

September 25, 2020

Shay Dodds
Manager, In Situ Surface
Alberta Energy Regulator
Suite 1000, 250 – 5th Street S.W.
Calgary, AB T2P 0R4

**Re: Christina Lake Thermal Project
Phase H Optimization Project
Application Under the *Oil Sands Conservation Act* and
*Environmental Protection and Enhancement Act***

Dear Mr. Dodds,

Cenovus Energy Inc. (Cenovus) has prepared the enclosed application for submission to the Alberta Energy Regulator (AER) for approvals to construct and operate the Christina Lake Thermal Project (CLTP) Phase H Optimization (the Project). More specifically, Cenovus is seeking approval from the AER for the following:

- amendment to Scheme Approval No. 8591QQQ to construct and operate the Project pursuant to Section 13 of the Oil Sands Conservation Act (OSCA), and Part 2 and Part 4 of the Oil Sands Conservation Rules; and
- amendment to Approval No. 48522-01-14, under Part 2, Division 2, Section 70 of the Environmental Protection and Enhancement Act (EPEA) to construct, operate and reclaim the Project, as proposed in the application contained herein.

This single application has been developed to combine all information required under the *OSCA* and *EPEA*. Other related applications under provincial statutes will be submitted separately to the agencies having jurisdiction.

The Project will be completed within the existing CLTP central processing facilities located at Sections 16 and 17, Township 76, Range 6, W4M, approximately 20 km southeast of the community of Conklin, Alberta. The Project is proposed to:

- increase the electrical generation capacity of the CLTP by approximately 96 MW (2 – 48 MW gas turbine generators);
- provide additional steam generation facilities through the installation of two new heat recovery steam generators (HRSGs); and
- update and optimize the Phase H water handling facilities

The Project will not result in a change to the approved CLTP Phase A to H production capacity of 49,284 m³/d (310,000 bbl/d), or the associated Project Area and Development Area boundaries.

Should you have any questions or concerns regarding the enclosed application, please contact the undersigned at (403) 766-7521, or brent.mitchell@cenovus.com.

Yours truly,

CENOVUS ENERGY INC.

A handwritten signature in dark ink, appearing to read "B. Mitchell", is positioned above the printed name.

Brent Mitchell
Sr. Specialist, Regulatory Applications

Enclosure



**Phase H Optimization Project
Integrated Application to the
Alberta Energy Regulator**

September 2020

Prepared for:

Cenovus Energy Inc.

Prepared by:

Stantec Consulting Ltd.
Calgary, Alberta

Project Number: 123513310

**PHASE H OPTIMIZATION PROJECT
INTEGRATED APPLICATION TO THE ALBERTA ENERGY REGULATOR**

Limitations and Sign-off

This document entitled Phase H Optimization Project Integrated Application to the Alberta Energy Regulator was prepared by Stantec Consulting Ltd. ("Stantec") for the account of Cenovus Energy Inc. (the "Client") to support the regulatory review process for its EPEA Approval Amendment and Scheme Approval Amendment (the "Application") for the Christina Lake Thermal Project (the "Project"). In connection therewith, this document may be reviewed and used by the Alberta Energy Regulator participating in the review process in the normal course of its duties. Except as set forth in the previous sentence, any reliance on this document by any other party or use of it for any other purpose is strictly prohibited. The material in it reflects Stantec's professional judgment in light of the scope, schedule and other limitations stated in the document and in the contract between Stantec and the Client. The information and conclusions in the document are based on the conditions existing at the time the document was published and does not take into account any subsequent changes. In preparing the document, Stantec did not verify information supplied to it by the Client or others, unless expressly stated otherwise in the document. Any use which another party makes of this document is the responsibility and risk of such party. Such party agrees that Stantec shall not be responsible for costs or damages of any kind, if any, suffered by it or any other party as a result of decisions made or actions taken based on this document.

**Elaine
Little**

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Project Manager _____
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Elaine Little, B.Sc.

**Hill,
Maureen**

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Project Director _____
(signature)

Maureen Hill, B.Sc, M.E.Des., P.Biol.



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Abbreviations

%	percent
°C	degrees Celsius
µg/m ³	micrograms per cubic metre
AAAQO	Alberta Ambient Air Quality Objective
ABMI	Alberta Biodiversity Monitoring Institute
ACO	Aboriginal Consultation Office
ACR	Alberta Chamber of Resources
AEP	Alberta Environmental Protection
AER	Alberta Energy Regulator
AQMG	Air Quality Modelling Guideline
m ASL	metres above sea level
m E	meters East
m N	meters North
AUC	Alberta Utilities Commission
bb/d	barrels per day
BFW	Boiler Feed Water
CaCO ₃	calcium carbonate
CAPP	Canadian Association of Petroleum Producers
Cenovus	Cenovus Energy Inc.
CFU	compact flotation unit
CLTP	Christina Lake Thermal Project
CO ₂	carbon dioxide
CH ₄	methane



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CO ₂ eq	carbon dioxide equivalent
COSIA	Canada's Oil Sands Innovation Alliance
CPF	central processing facility
CWE	Cold Water Equivalent
DA	Development Area
e ³ Sm ³ /d	thousand standard cubic metres per day
e ³ m ³ /d	thousand cubic metres per day
EIA	Environmental Impact Assessment
<i>EPEA</i>	<i>Alberta Environmental Protection and Enhancement Act</i>
ERCB	Alberta Energy Resources Conservation Board
ESRD	Alberta Environment and Sustainable Resource Development
EUB	Alberta Energy and Utilities Board
GHG	greenhouse gas
GOR	Gas to Oil Ratio
GTG	gas turbine generator
ha	hectare
HRSG	heat recovery steam generator
IGF	induced gas flotation
K	Kelvin
kg	kilogram
km	kilometre
kPa	kilopascal
LARP	Lower Athabasca Regional Plan
m	metre
m/s	metres per second



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m ³	cubic metre
m ³ /d	cubic metres per day
MMBtu/h	millions of international British thermal units per hour
MSL	Mineral Surface Lease
MW	megawatt
N ₂ O	nitrous oxide
NO	nitric oxide
NO ₂	nitrogen dioxide
NO _x	nitrogen oxides (oxides of nitrogen)
NRSU	Non-Regenerative Scavenger Unit
ORF	Oil Removal Filter Package
OSCA	Oil Sands Community Alliance
OSCA	<i>Oil Sands Conservation Act</i>
OSCR	<i>Oil Sands Conservation Rules</i>
OSDG	Oil Sands Developers Group
OSM	Oil Sands Monitoring
OTSG	Once through steam generator
PA	Project Area
PFD	Process flow diagram
ppm	parts per million
PW	Process water
PWSR	produced water to steam ratio
PVSV	Pressure vacuum safety valve
Q	quarter year
SAGD	Steam-assisted gravity drainage



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Sm ³ /d	standard cubic metres per day
SO ₂	sulphur dioxide
SOR	Steam to Oil Ratio
t/d	tonnes per day
the Guide	Guide to Content for Energy Project Applications
the Project	Phase H Optimization Project
W4M	West of the Fourth Meridian
WBEA	Wood Buffalo Environmental Association
WLS	Warm Lime Softener
yr	year



PHASE H OPTIMIZATION PROJECT INTEGRATED APPLICATION TO THE ALBERTA ENERGY REGULATOR

Introduction

Cenovus Energy Inc. (Cenovus) operates a commercial scheme for the recovery of crude bitumen at the Christina Lake Thermal Project (CLTP), located at Townships 75 and 76, Ranges 4, 5 and 6, West of the Fourth Meridian (W4M). Steam-assisted gravity drainage (SAGD) technology is utilized to extract bitumen from the McMurray Formation. The facility includes the central processing facilities (CPFs), SAGD well pairs, and supporting infrastructure and pipelines. The CLTP operates under Alberta Energy Regulator (AER) *Environmental Protection and Enhancement Act (EPEA)* Approval No. 48522-01-14 and *Oil Sands Conservation Act (OSCA)* Scheme Approval No. 8591QQQ.

As described in this application, Cenovus is requesting an EPEA approval amendment and scheme approval amendment for the proposed optimization of the CLTP approved Phase H CPF, or the Phase H Optimization Project (the Project). The Phase H and Eastern Expansion Application (Scheme Application No. 1758947, EPEA Application No. 019-48522) was previously approved in December 2015. The Project is proposed to:

- increase the electrical generation capacity of the CLTP by approximately 96 MW (2 – 48 MW gas turbine generators)
- provide additional steam generation facilities through the installation of two new heat recovery steam generators (HRSGs)
- update and optimize the Phase H water handling facilities

The Project will be completed within the existing CLTP CPF disturbance area at Section 16, Township 76, Range 6, W4M. No additional land disturbance is required to complete the Project. The CLTP is located approximately 20 km southeast of the community of Conklin, Alberta. Figure 18-1 provides the CLTP project location in association with the surrounding area. After regulatory and internal corporate approvals, site construction is expected to take up to three years with operations commencing the following year. The operational lifespan of the Project is expected to be approximately 25 years.

This document is Cenovus's integrated application to the AER for an amendment to Approval No. 48522-01 (as amended) under Division 2 of Part 2 and Section 70 of the *EPEA*, and amendment to Commercial Scheme Approval No. 8591 (as amended), pursuant to Section 13 of the *OSCA*, and Part 2 and Part 4 of the Oil Sands Conservation Rules (OSCR). It has been prepared in accordance with the Guide to Content for Energy Project Applications (AER, 2014) (the Guide) and the requirements listed in subsection 3(1) of the Approvals and Registrations Procedure Regulation (Alberta Regulation 113/93). It has also been prepared in accordance with draft Directive 023: Oil Sands Project Applications (AER, 2013). A concordance table relating to the requirements outlined in draft Directive 023 is provided in the AER Directive 023 Concordance Table (Appendix A). The format for this report follows the headings in the Guide, in bold text throughout this document.



**PHASE H OPTIMIZATION PROJECT
INTEGRATED APPLICATION TO THE ALBERTA ENERGY REGULATOR**

Confirm Applicant Identification
September 2020

Part 3: Amendments

17.0 CONFIRM APPLICANT IDENTIFICATION

17.1 CONFIRM APPLICANT NAME

Cenovus Energy Inc. (Cenovus). AER Business Associate Code: A5D4.

17.2 MAILING ADDRESS OF REGISTERED CORPORATION

Cenovus Energy Inc.
225 – 6 Avenue SW
P.O. Box 766 Calgary, AB
T2P 0M5

17.3 MAILING ADDRESS OF PLANT

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Lac La Biche, AB
T0A 2C0

17.4 APPLICANT CONTACTS

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Title Sr. Specialist, Regulatory Applications

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E-mail: brent.mitchell@cenovus.com

Christina Lake Thermal Project Operations

Telephone: (780) 559-8523
Facsimile: (780) 559-8401

See also: Appendix B Authorization of Application for Approval by Owner/Agent



PHASE H OPTIMIZATION PROJECT INTEGRATED APPLICATION TO THE ALBERTA ENERGY REGULATOR

Confirmation of Plant Identification
September 2020

18.0 CONFIRMATION OF PLANT IDENTIFICATION

18.1 PRIMARY ACTIVITIES AND CLASSIFICATION

The CLTP is designated as an enhanced recovery in-situ oil sands processing plant and oil production site under the *EPEA* Activities Designation Regulation (AR 276/2003), as approved under *EPEA* Approval No. 48522-01-14. In addition, the CLTP is designated as an in-situ operation under the *OSCA*, as approved through commercial Scheme Approval No. 8591QQQ. Bitumen resource for the Project is sourced from areas within the Cenovus scheme approved Project Area (PA) and Development Area (DA) boundaries. The total CLTP Phase A to H approved production capacity is 49,284 m³/d (310,000 bbl/d), as given in Condition 4 of the scheme approval.

As part of the Phase H Optimization Project, Cenovus is proposing to install a 96 megawatt (MW) cogeneration facility and complete associated plant modifications to the approved CLTP Phase H facilities. The Project will not result in a change to the approved production capacity, surface land requirements, or PA and DA boundaries. Pursuant to Division 2 Part 2 of *EPEA*, and pursuant to Section 13 of the *OSCA*, and Part 2 and Part 4 of the *OSCR*, amendments to the CLTP *EPEA* Approval No. 48522-01-14 and to Scheme No. 8591QQQ are required for the proposed modifications.

In consideration with Section 10 of the AER Directive 023: Oil Sands Project Applications (AER, May 2013), Cenovus requests that the scheme application be processed as a Category 2 amendment, based on the following rationale:

- the proposed Project is not expected to adversely and materially impact the rights of stakeholders, including other mineral right holders
- the proposed Project is not expected to materially affect resource conservation
- the proposed Project is not expected to adversely and materially alter the socioeconomic or environmental impacts previously predicted and assessed for the CLTP

18.2 PLANT LOCATION

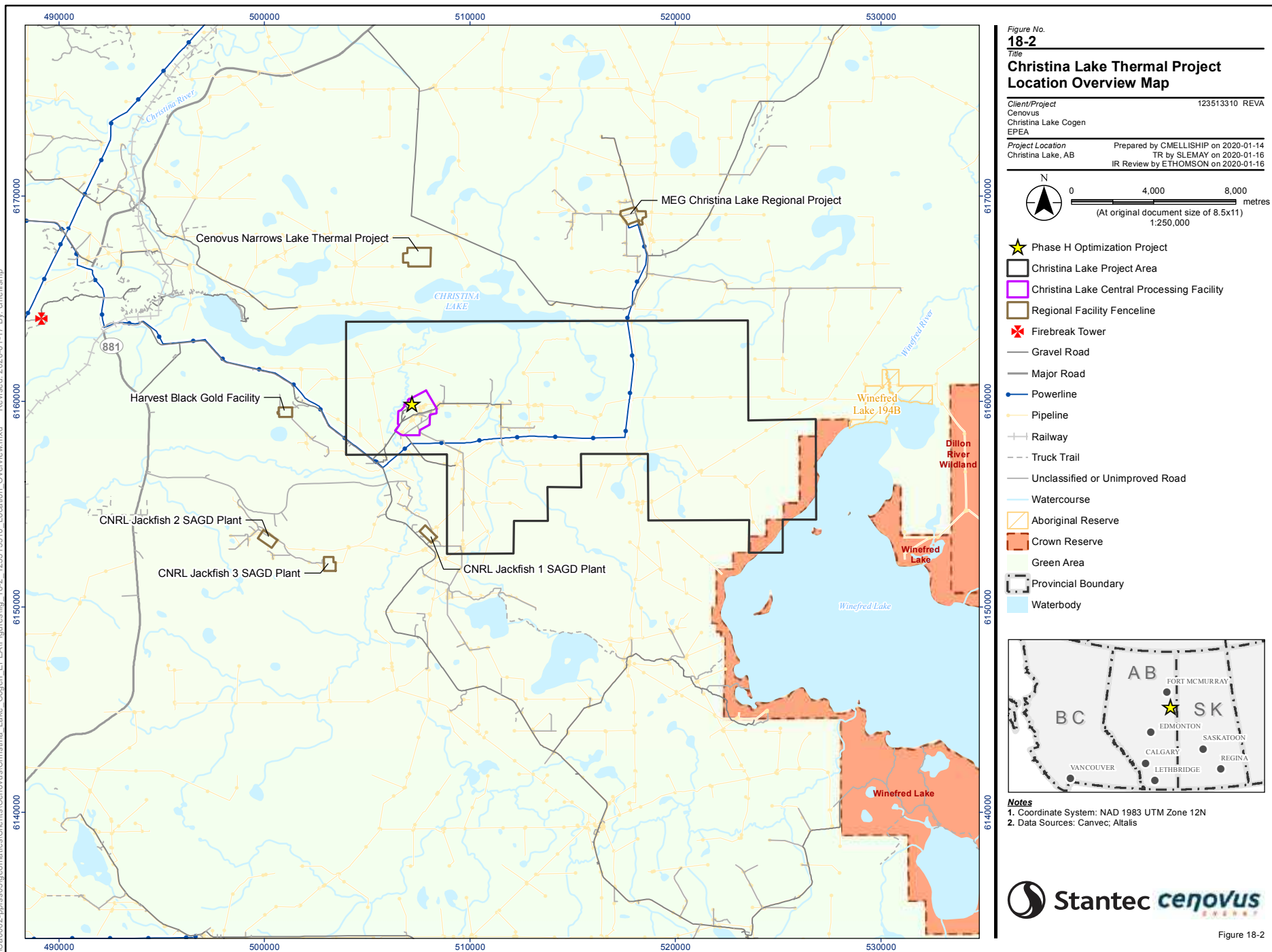
The CLTP is located in Townships 75 and 76, Ranges 4, 5 and 6, West of the Fourth Meridian (W4M). Within the CLTP PA, the Phase A to H CPF is located in Section 16 and 17, Township 76, Range 6, W4M. The proposed Project is located entirely within the existing/approved CLTP CPF footprint. The latitude and longitude of the CPF plant site is 55.58129 and -110.88765, respectively. The CLTP is located approximately 20 km southeast of the community of Conklin, Alberta.

18.3 REGIONAL MAP

A regional map of the area surrounding the CLTP is provided in Figure 18-1. A location overview map of the CLTP area is provided in Figure 18-2.



\\Ca0002-ppfss03\geomatics\Clients\Cenovus\Christina Lake_Cogen_EPEA\Figures\fig_18-2_123513310_Location_Overview.mxd Revised: 2020-01-17 By: cmelliship



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PHASE H OPTIMIZATION PROJECT INTEGRATED APPLICATION TO THE ALBERTA ENERGY REGULATOR

Confirmation of Plant Identification
September 2020

18.4 PROJECT AND PLANT SIZE

The CLTP has an approved Phase A to H bitumen production capacity of 49,284 m³/d (310,000 bbl/d), steam generation capacity of 89,696 m³/d (CWE) and electrical generating capacity of 88 MW. Through the addition of the Project, Cenovus is proposing to add 8,767 m³/d (Cold Water Equivalent [CWE]) of steam generation capacity and 96 MW of electrical generating capacity (see Section 21.1.1). Given the proposed Steam to Oil Ratio (SOR) for the Project, Cenovus is not anticipating an overall increase to the bitumen production capacity. The approved and proposed bitumen production, steam generation capacity, and power capacity for the CLTP are provided in Table 18-1.

Table 18-1 Christina Lake Thermal Project Central Plant Summary

	Approved Phase A-G	Approved Phase H	Proposed Phase H Optimization	Proposed Phase A-H (Total)
# of once-through steam generators (OTSGs)	24	5	0	29
# of gas turbine generator (GTG)/heat recovery steam generators (HRSGs)	2	0	2	4
Production Capacity (bbl/d)	260,000	50,000	0 ^(a)	310,000
Production Capacity (m ³ /d)	41,335	7,494	0 ^(a)	49,284
Power Generation Capacity ^(b) (MW)	88	0	96	184
NOTES: ^(a) The Project will not result in an overall Phase A to H production increase. ^(b) Power capacity based on an ambient temperature of 15 C.				

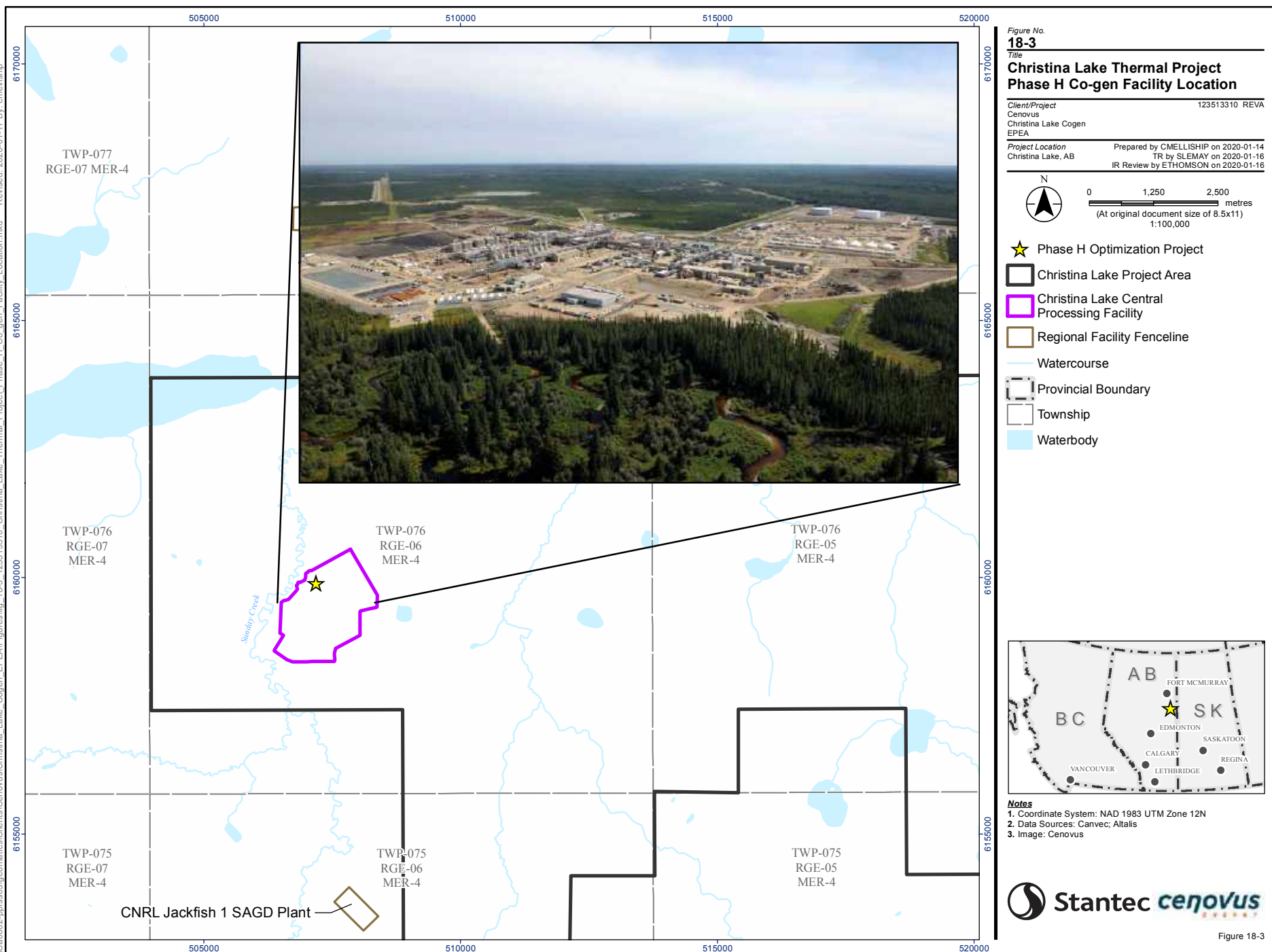
The Project will result in the addition and modification of the following equipment to the approved Phase H facilities:

- two new 48 MW gas turbine generators to increase the electrical generation capacity of the CLTP by approximately 96 MW
- two new 112 MW heat recovery steam generators (HRSGs) to provide additional steam generation facilities
- a compact flotation unit (CFU) to optimize the Phase H CPF water handling facilities
- additional utilities and tankage
- Sunday Creek substation modifications

The plot plan for the Phase H Optimization Project, which includes the major equipment to be added for the Project is provided in Appendix C. The Project will have a footprint of approximately 0.5 ha, and the cogeneration facility and associated plant modifications will be located entirely within the footprint of the existing Christina Lake CPF and approved Mineral Surface Lease (MSL) 002635 (see Figure 18-3).



\\Ca0002-ppfss03\geomatics\Clients\Cenovus\Christina Lake Thermal Project Phase H Co-gen Facility Location.mxd Revised: 2020-01-17 By: cmelliship



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PHASE H OPTIMIZATION PROJECT INTEGRATED APPLICATION TO THE ALBERTA ENERGY REGULATOR

Confirmation of Plant Identification
September 2020

As discussed above, the Project is proposed to optimize and expand the approved Phase H facilities. Given its location in relation to the existing and approved facilities, the Project can utilize a significant amount of the existing and approved site infrastructure, including the following:

- sales oil pipeline
- natural gas source pipeline
- site access roads and infrastructure
- work site camps and office/support buildings
- sulphur removal facilities
- steam/emulsion/produced gas pipeline corridors and well pads

The use of this existing/approved infrastructure significantly reduces the footprint requirements for the Project.

Water is required for steam generation to support SAGD production. The majority of the water used for steam generation is recycled produced water that is de-oiled and softened in the produced water treatment areas of the CPF. Brackish water is used to make up for water losses from boiler blowdown and regeneration waste streams that are sent to disposal wells. The current CLTP operation predominantly uses saline water from the Clearwater B Aquifer for steam generation water make-up, and a limited amount of fresh water from the Christina Channel (Empress Formation) for utility water purposes. The Project will primarily use make-up water from the McMurray Formation and will not require an increase to the freshwater allocations approved in the current CLTP *Water Act* licenses. Wastewater from the CLTP is injected (disposed of) into the saline Basal McMurray Aquifer.

Bitumen resource for the Project will be sourced from areas within the Cenovus scheme approved PA and DA boundaries. Well pad drainage pattern update scheme applications will be submitted separately, as required, as well pad development progresses within the approved DA. The Project will not result in a change to the scheme approved production capacity, or PA and DA boundaries.



PHASE H OPTIMIZATION PROJECT INTEGRATED APPLICATION TO THE ALBERTA ENERGY REGULATOR

Project Background for the Proposed Changes
September 2020

19.0 PROJECT BACKGROUND FOR THE PROPOSED CHANGES

19.1 RELEVANT REGIONAL INITIATIVES AND PLANS

Cenovus is committed to responsible resource development. Following sustainable development principles allows Cenovus to balance environmental integrity while enhancing social and economic opportunities. This section discusses Cenovus's efforts in working with others involved in the region to achieve these goals.

19.1.1 Co-Operative Efforts

Cenovus works together with industry and communities to improve our environmental footprint while providing economic opportunity and stability. These activities include:

- regional environmental monitoring
- working co-operatively in environmental research
- stakeholder consultation

Cenovus participates in co-operative efforts to address industry issues where it determines that such endeavors are effective. Cenovus re-visits its participation in such co-operative effort on an ongoing basis. Cenovus is currently a participant in the following:

Canada's Oil Sands Innovation Alliance (COSIA) – Formed in March of 2012, COSIA consists of a consortium of Canadian oil sands producers focused on accelerating the pace of improving environmental performance in the oil sands region. The commitments put forward in the charter focus on collaboration and transparent exchange, by setting environmental performance goals and reporting publicly on progress towards those goals.

The guiding principle for COSIA is that all members will have greater success by collaborating on environmental innovation than by their own individual efforts. Four environmental priority areas that will allow COSIA to achieve these objectives are tailings, water, land, and greenhouse gases. Cenovus's President and Chief Executive Officer stated:

"As a company with a deep-rooted respect for the environment, and a culture that fosters new ideas and new approaches in all aspects of our business, we are excited to be a charter member of COSIA."



PHASE H OPTIMIZATION PROJECT INTEGRATED APPLICATION TO THE ALBERTA ENERGY REGULATOR

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Oil Sands Monitoring (OSM) Program – The OSM Program mandate is to implement an ambient environmental monitoring program for the oil sands that integrates air, water, land and biodiversity. The program strives to improve the characterization of the state of the environment and enhance understanding of the cumulative effects of oil sands development in the oil sands area. Cenovus currently provides logistical support, technical information and funding, contributing to the \$50 million industry allocation as specified in the funding formula for the OSM Program.

Wood Buffalo Environmental Association (WBEA) - WBEA monitors the environment of the Regional Municipality of Wood Buffalo in northeastern Alberta. WBEA is committed to reporting accurate and timely high-quality data from its air, terrestrial and human exposure monitoring programs to ensure regional stakeholders have the information needed to make informed environmental decisions. Cenovus is a funding industry member of WBEA.

Oil Sands Community Alliance (OSCA) – This organization was formerly called the Oil Sands Developers Group (OSDG). The OSCA is a Canadian Association of Petroleum Producers (CAPP) directed program funded through industry members that works with various other organizations to address socio-economic issues of oil sands developments. Cenovus participates as a member of OSCA.

Alberta Chamber of Resources (ACR) – Cenovus is a financial supporter and an active participant in the ACR, as well as participating in its Integrated Landscape Management program. As stated by ACR, (ACR 2010):

“The Integrated Landscape Management program represents the first large scale Canadian effort to proactively address the cumulative impacts of resource-based land use.”

Alberta Biodiversity Monitoring Institute (ABMI) – Cenovus is a financial supporter and an active participant in the ABMI. This organization is establishing a province-wide biodiversity monitoring program. As stated by ABMI (ABMI 2010):

“The Alberta Biodiversity Monitoring Institute (ABMI) conducts world-class monitoring of the changing state of Alberta’s species, habitats and ecosystems. The goal of the ABMI is to support natural resource decision-making by providing relevant, timely, and credible scientific knowledge on the state of provincial biodiversity.”

19.1.2 Lower Athabasca Regional Plan

The Lower Athabasca Regional Plan (LARP) sets out several objectives for long term land-use planning. It touches on management and conservation for topics such as air quality, ecosystem function and biodiversity, groundwater and surface water quality and tailings management framework (GOA 2012).

Development of the oil sands is in keeping with the principles of the LARP which states “The economic potential of the oil sands is optimized” as one of its Regional Outcomes (GOA 2012). Cenovus is actively engaged in ensuring consistency with the LARP as it relates to CLTP development.



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19.2 RELATED HEARING RESULTS AND DECISIONS

The original joint application and Environmental Impact Assessment (EIA) for the CLTP was submitted to the Alberta Energy and Utilities Board (EUB) and Alberta Environmental Protection (AEP) in March 1998. In 2000, the Order in Council was issued, and the scheme and *EPEA* application was approved by the EUB and AEP for the production of 70,000 bbl/d (11,200 m³/d) of bitumen over three phases of development (Phases I, II and III), each with a separate CPF site. Subsequent to this, Cenovus amended the original application to the current Phase A/B development and then further amended the application to incorporate Phases C and D, giving a Phase A to D cumulative bitumen production capacity of 98,800 bbl/d (15,700 m³/d).

The CLTP Phase E, F and G joint application and EIA was filed on October 2, 2009 to the Alberta Energy Resources Conservation Board (ERCB) and Alberta Environment and Sustainable Resource Development (ESRD). This application included three additional 40,000 bbl/d (6,360 m³/d) phases, bringing the cumulative production capacity to 218,800 bbl/d (34,789 m³/d). This joint application and *EPEA* amendment were approved by the ERCB in April 2011 and ESRD in July 2011. Subsequent to this, Cenovus submitted the Phase CDE Debottleneck and Phase F/G Amendment to further optimize the CLTP Phase A to G facilities and increase the total cumulative bitumen production rate to 260,000 bbl/d (41,335 m³/d).

In March 2013, Cenovus filed the CLTP Phase H and Eastern Expansion joint application and EIA (the Phase H Application), which proposed to expand the existing and approved CLTP Phase A to G facilities to increase bitumen production by 50,000 bbl/d (7,949 m³/d), bringing the total production capacity to 310,000 bbl/d (49,284 m³/d). The Phase H and Eastern Expansion joint application was approved in December 2015 (*EPEA* Approval No. 48522-01-06; and Scheme Approval No. 8591QQ). Cenovus completed construction of Phase G in 2019 and the current Phase A to G CPF has a production capacity of approximately 260,000 bbl/d (41,335 m³/d).

The CLTP phased development history and associated regulatory approval dates are provided in Table 19-1.

Table 19-1 Christina Lake Thermal Project Phased Expansion Approval Chronology

Phase	Application Description	Approved Cumulative Capacity	Scheme Approval	EPEA Approval
Phase I, II, III	Initial Project Application - three phase development	11,200 m ³ /d	8591 (April 2000)	48522-00-00 (August 2000)
A	First Commercial Phase of CLTP	1,590 m ³ /d (10,000 bbl/d)	8591C (March 2005)	48522-00-00 (August 2000)
B	Phase B Amendment	2,989 m ³ /d (18,800 bbl/d)	8591E (December 2005)	48522-00-07 (December 2005)
C/D	Phase C/D plant expansion	15,709 m ³ /d (98,800 bbl/d)	8591I (July 2008)	48522-00-09 (July 2008)



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Table 19-1 Christina Lake Thermal Project Phased Expansion Approval Chronology

Phase	Application Description	Approved Cumulative Capacity	Scheme Approval	EPEA Approval
E/F/G	Phase E/F/G plant expansion	34,789 m ³ /d (218,800 bbl/d)	8591Q (April 2011)	48522-00-12 (July 2011)
F/G Amendment	Phase F/G plant optimization	37,969 m ³ /d (238,800 bbl/d)	8591Y (December 2012)	48522-01-03 (December 2012)
C/D/E Amendment	Phase C/D/E plant optimization	41,335 m ³ /d (260,000 bbl/d)	8591DD (September 2013)	48522-01-04 (January 2014)
H	Phase H plant expansion	49,284 m ³ /d (310,000 bbl/d)	8591QQ (December 2015)	48522-01-06 (December 2015)

A hearing was conducted as part of the original CLTP application (Application No. 1023589) in 1999. Issues reviewed during the hearing included need for the project, public consultation, socioeconomic issues, bitumen recovery process, land use, environmental issues and cumulative effects of oil sands development. EUB Decision 2000-7 was issued in February 2000 regarding the hearing conducted. No additional regulatory hearings have occurred related to the CLTP.

19.3 ENVIRONMENTAL IMPACT ASSESSMENT ACCEPTANCE DATE

As discussed in Section 19.2, Cenovus (and its predecessor companies) completed three EIAs for the CLTP. The EIA acceptance dates for these applications are provided below:

- Original Application and EIA submitted in March 1998 – EIA accepted 1999
- Phase EFG Application and EIA (Encana FCCL, 2009) – EIA accepted 2011
- Phase H Application and EIA (Cenovus FCCL, 2013) – EIA accepted 2015

To determine if the Project required an EIA, Cenovus provided a Project Summary Table and Project Map to the AER on October 3, 2019. Following review of the provided documentation, the AER determined on October 21, 2019 that an EIA was not required for the Project (see Appendix D).

19.4 RELATED AUTHORIZATIONS

Other related applications or guidelines under provincial and federal statutes may be pertinent to the Project. Any supplemental applications required for the development of the Project will be submitted separately to agencies having jurisdiction. Potential pertinent approvals or guidelines may include but are not necessarily limited to the following:

- Provincial:
 - *Historical Resources Act*, for clearance to construct surface facilities
 - MSL002635, *Public Lands Act*, for surface rights



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- Directive 017: Measurement Requirements for Upstream Oil and Gas Operations (AER 2018)
- Directive 042: Measurement, Accounting and Reporting Plan (MARPs) Requirement for Thermal Bitumen Schemes (AER 2006)
- Directive 055: Storage Requirements for the Upstream Petroleum Industry (AER 2001)
- Directive 056: Energy Development Applications and Schedules (AER 2019a)
- Directive 081: Water Disposal Limits and Reporting Requirements for Thermal In Situ Oil Sands Schemes (AER 2019b)
- *Municipal Government Act*, Part 17 for development permits
- Application to Alberta Utilities Commission (AUC) under Rule 007 (AUC 2019) and Rule 012 (AUC 2013) of the *Hydro and Electric Energy Act*.
- Federal:
 - The Project as proposed is not expected to require Federal approval (see Appendix D).

19.5 FINANCIAL SECURITY

No changes to financial security are required due to the Project.

19.6 PROJECT TIMELINE AND MILESTONES

After regulatory and internal corporate approvals, site construction is expected to take up to three years with operations commencing the following year. The operational lifespan of the Project is expected to be approximately 25 years.

19.7 PUBLIC CONSULTATION AND STAKEHOLDER ENGAGEMENT

Cenovus submitted a pre-consultation assessment request to the Government of Alberta Aboriginal Consultation Office (ACO) for the Project on May 24, 2019. Given that the Project is located wholly within MSL002635, does not require additional surface disturbance, and will meet current emission standards and the Alberta Ambient Air Quality Objectives (AAAQOs), the ACO adequacy assessment determined that consultation is not required for the Project (FNC 201903720). Cenovus maintains ongoing community and local engagement with its stakeholders. No stakeholder engagement activities outside of the regulatory approval amendment process are currently planned for the Project; however, stakeholder engagement will continue as required. To date, no environmental concerns have been identified. Cenovus will continue to work with stakeholders to address concerns raised through the application process and public notice of application.



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20.0 UPDATE APPLICABLE ELEMENTS OF THE CURRENT SETTING AND ITS ENVIRONMENTAL CONDITION

20.1 SCOPE OF UPDATES

The Project will result in changes to air quality in the vicinity of the Project and will require approximately 0.5 ha of land within the existing CLTP CPF footprint. The Project includes a change to saline groundwater withdrawal and disposal plans.

The land to be used is currently brownfield (i.e., within the active facility footprint), located to the south of the existing storm water pond and north of the de-oiling buildings, tanks and facilities. The Project's predicted air emission contributions have been calculated in support of this application (see Section 21.18).

The Project will not adversely alter the socioeconomic impacts previously assessed and approved for the CLTP.

20.2 CURRENT SETTING AND ENVIRONMENTAL CONDITIONS

The proposed changes due to the Project have the potential to affect environmental aspects related to air quality as further described below. Cenovus also updated the regional hydrogeology model as provided in Appendix E to assess changes to saline water use and subsequent disposal volumes into the McMurray Formation. Cenovus is not proposing to increase its approved freshwater allocation for the Project

20.2.1 Existing Conditions

Development of the Project will not require additional or new disturbance of the natural environment and will be entirely within the existing development of the CLTP. The area that has been identified for the Project (see Figure 18-3) is currently stripped of vegetation and soils and does not have any natural waterbodies; therefore, no environmental effects on vegetation, soil, wildlife, hydrology, fish and fish habitat will occur.

20.2.2 Ambient Air Quality

Topography within a 22 km by 22 km study area was assessed for the air quality assessment, provided in Appendix F. The Project is situated at a base elevation of approximately 565 m above sea level (ASL). Terrain elevations decrease to the northwest towards Christina Lake. Terrain generally rises gently to the southwest. The maximum elevation within the study area is 690 m.

As per the Air Quality Modelling Guideline (AQMG), representative regional ambient background concentrations were determined for the study area (Appendix F). Wood Buffalo Environmental Association (WBEA) Conklin station monitoring data were selected to provide background sulphur dioxide



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(SO₂), nitrogen dioxide (NO₂) and nitrogen oxides (NO_x) concentrations for the area because the station is located approximately 13 km west-northwest of the Project site, and is the closest continuous monitoring station in the local area outside the Project boundary. Ambient data for SO₂, NO₂ and NO_x for the most recent year (2018) were analyzed using the AQMG (ESRD 2013) methodology to calculate background concentrations. Background concentrations are presented in Table 20-1.

Table 20-1 Estimated Ambient Background Concentrations

Substance	Averaging Period	Background Concentration ^a (µg/m ³)	AAAQO ^b (µg/m ³)	Comparison of Background to AAAQO (%)
SO ₂	One-hour	2.62	450	0.6
	24-hour	2.62	125	2
	30-day	0.65	30	2
	Annual	0.35	20	2
NO _x	One-hour	12.2	-	
	Annual	3.89	-	
NO ₂	One-hour	10.0	300	4
	Annual	3.31	45	9

NOTES:

^a Background concentration was calculated as per Section 4.2 of the Air Quality Modelling Guideline (ESRD 2013). The hourly average background concentration is the 90th percentile value calculated from the complete data set. For averaging periods greater than one-hour, the maximum calculated value, for each averaging period, was based on a reduced hourly data set with the hourly values above the 90th percentile value removed.

^b Concentrations given (µg/m³) at 25°C and 101.325 kPa. See Table 2-2 in Appendix F.

20.3 CHANGES TO ENVIRONMENTAL ASPECTS DUE TO REGIONAL INITIATIVES AND PLANS

Cenovus works together with industry and communities to improve its environmental footprint while providing economic opportunity and stability. These activities include:

- regional environmental monitoring
- working co-operatively in environmental research
- stakeholder consultation

Cenovus participates in co-operative efforts to address industry issues where it determines that such endeavors are effective. Cenovus re-visits its participation in such co-operative effort on an ongoing basis. More information on Cenovus's approaches to regional initiatives is located in Section 19.1.1.

The CLTP has established environmental management frameworks for air and surface water quality that include environmental limits, and abide by the conditions in EPEA Approval 48522-01-14, as amended.



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20.4 CHANGES TO PLANT OBLIGATIONS

Not applicable. There are no changes proposed for CLTP obligations as a result of the Project. All monitoring and other requirements will be completed in accordance with the CLTP *EPEA* and Scheme approvals.



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21.0 PROPOSED CHANGES TO DESIGN AND OPERATION

21.1 PROPOSED CHANGES TO PLANT PROCESSES

The Phase H facilities were originally proposed in, and approved as part of, the March 2013 CLTP Phase H and Eastern Expansion joint application and EIA (the Phase H Application). Phase H included the addition of five OTSGs, with a total of 29 OTSGs and 2 GTG/HRSGs for the Phase A to H CPFs. The Phase H and Eastern Expansion application was approved in December 2015 (the Phase H Approval).

As described in this application, Cenovus is proposing to optimize the previously approved CLTP Phase H project through the addition and modification of the following surface facilities:

- Addition of two 48 MW GTGs
- Addition of two 112 MW HRSGs
- Addition of a CFU within the produced water de-oiling system

The proposed cogeneration facility will supply additional electrical power generating capacity to further balance on-site power needs, import power requirements and provide additional efficient steam generation capacity for use in the SAGD operations. In addition, the incorporation of a CFU will optimize the produced water de-oiling system and replace the previously planned induced gas flotation (IGF) unit. The proposed changes will not increase the approved CLTP Phase A to H approved bitumen production capacity of 310,000 bbl/d (49,284 m³/d).

The following sections further discuss the additions and modifications proposed for the approved Phase H facilities that were previously described in the Phase H and Eastern Expansion Application (Scheme Application No. 1758947). For ease of review, the Facilities section follows the same format as the original Phase H application document. If the sections are unchanged due to this amendment, the sections are denoted as “No changes required to this section”. The material balances, block flow diagrams, and energy balances associated with this section are provided in Appendix G, process flow diagrams are provided in Appendix H, and the equipment list and plot plan have been provided in Appendix C. An assessment of environmental noise as a result of the additions and modifications discussed in the following sections has been included as Appendix I.

21.1.1 Central Processing Facility Overview

The currently approved CLTP Phase H facilities are proposed to be expanded to increase steam generation capacity and sustain oil production. The updated steam and bitumen capacities for all phases of the CPF are summarized in Table 21-1.



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Table 21-1 Injection Steam Capacity and Bitumen Production Capacity

Phase	Status	Dry Steam Capacity	Bitumen Production Capacity	
		m ³ /d Cold Water Equivalent (CWE) ^(a)	(bbl/d)	(m ³ /d) ^(a)
Phases A and B	Operating	5,347 ^(b)	18,800	2,989 ^(b)
Phase C	Operating	11,392 ^(b)	40,000	6,359 ^(b)
Phase D	Operating	11,392 ^(b)	40,000	6,359 ^(b)
Phase E	Operating	11,392 ^(b)	40,200	6,359 ^(b)
Phase F	Operating	14,612 ^(b)	40,200	6,391 ^(b)
Phase G	Operating	14,610 ^(b)	40,000	6,391 ^(b)
Phases A to G (Sub-total)	See Above	68,745	219,200	34,850
CDE 2 nd Stage OTSGs	Operating	6,695 ^(b)	21,200	3,371
Phases A to G, includes CDE 2nd Stage OTSGs (Sub-total)	See Above	75,440	240,400	38,221
Phase H	Approved	17,178 ^(b)	46,100	7,329 ^(b)
Phase H Amendment (the Project)	Proposed	8,767 ^(b)	23,500	3,736 ^(b)
Phases A to H, includes CDE 2nd Stage OTSGs and the Project (Total)	See Above	102,135	310,000	49,286
NOTES:				
^(a) Totals may not add due to rounding.				
^(b) Refer to Block Flow Diagram CL1-42-BFD-00-143-03.				

A summary of the Project equipment and the associated subsections in which equipment is referenced is provided in Table 21-2. Equipment lists are also provided in Appendix C.

21.1.1.1 Steam Generation

Two HRSGs will be installed to increase the Phase H steam capacity. The placement of these HRSGs is within the CPF plot plan as shown in Appendix C. The CPF will have a fixed maximum steam rate based on the number of steam generators available, while the bitumen production rate will depend on the SOR achieved. The average forecast SOR for Phases A to H is 2.0.

The dry steam rates for Phases C through H has been upgraded to 82% based on CPF performance to date. As per previous amendments, emission modelling for all steam generators is based on the burner limitations.

Overall CPF block flow diagrams for a produced water to steam ratio (PWSR) of 1.0, an overall energy balance, development profile with the Directive 081 water usage formulas, and a simplified water balance are included in Appendix G.



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Table 21-2 Central Processing Facility Equipment for the Project

Equipment Description	Equipment Identification Number	Sub-Section Reference	Associated Process Flow Diagrams ^(a)
Produced Water/Glycol Exchangers	E-4650F, E-4450F, E-4550F	21.1.3.1 (Production Processing)	CL1H-42-PFD-04-0140-001 CL1H-42-PFD-04-0150-001 CL1H-42-PFD-04-0160-001
Glycol Air Coolers	AC-7351A-J	21.1.4.3 (CPF Glycol System)	CL1H-42-PFD-07-0142-002
Produced Water Transfer Pumps	P-0510A-C	21.1.5.2 (Produced Water Deoiling System)	CL1H-42-PFD-01-0151-001
Produced Water Surge Tank	T-0515	21.1.5.2 (Produced Water Deoiling System)	CL11H-42-PFD-01-0151-001 CL1H-42-PFD-01-0161-001 CL1H-42-PFD-01-0161-002
CFU Feed Pumps	P-0520A-C		
CFU Package	PK-0525		
Oil Removal Filter Packages (ORFs)	PK-0540D		
Deoiled Water Pumps	P-0558D		
Oil Recycle Tanks	T-0545B		
Deoiling Flocculant Polymer Injection Package	PK-0779, T-0778	21.1.1.1 (Steam Generation)	CL1H-42-PFD-02-0140-001 CL1H-42-PFD-02-0161-001 CL1H-42-PFD-02-0161-002 CL1H-42-PFD-02-0161-004 CL1H-42-PFD-02-0161-005
HRSBs	B-5600/5650		
HP Natural Gas Filters/Separators	F-5495A/B		
HP Natural Gas Heater	EH-5494		
Gas Turbines	GT-5500/5550		
Steam Separators	V-5700		
BFW / Blowdown Exchangers	E-5705		
Blowdown/Glycol Exchanger	E-5710		
2 nd Stage BFW Charge Pumps	P-2880		
Boiler Feed Water (BFW) Booster Pumps	P-3010H		
BFW Charge Pumps	P-3015H		
Vapour Recovery Unit (VRU) Compressor Package	PK-7670	21.1.9 (Vapour Recovery System)	CL1H-42-PFD-07-0140-002
NOTE: ^(a) Associated process flow diagrams provided in Appendix H.			



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21.1.1.2 Make-Up Water Treatment

The Project has made no change to the scope of this system since the original Phase H application, although the anticipated make-up water requirements have changed as a result of the Project.

21.1.1.3 Water Re-use and Disposal

The Project has made no change to the scope of the water re-use and disposal water systems since the original Phase H application; however, the anticipated wastewater disposal volumes have changed as a result of the Project.

Five OTSGs are proposed for Phase H, as described in the original application, with one designated for 2nd stage operation. Two HRSGs added for the Project allow the 2nd stage OTSG to operate at rated capacity. Refer to Figure 21-1 for a sketch of the proposed steam generation configuration.

Development profiles indicating anticipated production and water usage are included in Appendix G. In these models it is assumed that all steam generators will operate at 82% steam quality. The PWSR equal to 1.0 cases yield the maximum make-up water requirements. The predicted high PWSR cases yield the maximum blowdown disposal requirements.

21.1.1.4 Produced Gas Treatment

The Project has made no change to the scope of this system since the original Phase H application.



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21.1.1.5 Bitumen Production Treatment

Heat and material balances for the Project are included in Appendix G.

21.1.2 Flow Rates

The anticipated cumulative flow rates for the expanded CPF are listed in Table 21-3.

Table 21-3 CPF Cumulative Flow Rates

Parameter	Units	Phases A to H
Saturated steam from steam generators	m ³ /d CWE	102,135 ^(a)
Saturated steam to injection wells	m ³ /d CWE	101,015 ^(a)
Oil from production wells	Sm ³ /d	49,283 ^(a)
Produced water from wells	m ³ /d CWE	101,015 ^(a)
Produced gas from wells (dry basis)	e ³ Sm ³ /d	908.8 ^(a) 1,792.0 (Sensitivity) ^(e)
Coinjection/Blowdown Produced Gas	e ³ Sm ³ /d	366.7 ^(a) 1,304.8 (Sensitivity) ^(e)
Fresh water consumption	Sm ³ /d	229 ^(a) 5,000 (Upset) ^(d)
Brackish make-up water consumption	Sm ³ /d	11,166 ^(a) 23,650 (Upset) ^(b)
Steam blowdown to disposal	Sm ³ /d	9,803 ^(a) 22,247 (Upset) ^(b)
Regeneration/neutralization waste to disposal ^(c)	Sm ³ /d	1,029 ^(a) 1,119 (Upset) ^(b)

NOTES:

- (a) Refer to the Block Flow Diagrams and Simplified Water Balances in Appendix G.
- (b) Upset conditions indicated are based on a blowdown recycle rate of 0% and a PWSR of 1.0. For simplicity, it is assumed that all OTSGs operate at a steam quality of 82% in the upset case. Note that the Block Flow Diagrams and Simplified Water Balances (Appendix G) assume an 82% steam quality for all the OTSGs, except the Phase CDE 2nd Stage OTSGs, which use a steam quality of 75%.
- (c) Regen waste quantities are based on assumed water quality. Design assumes 20 ppm total hardness as CaCO₃ for the produced water, 140 ppm as CaCO₃ for the Clearwater B (Phases A to E) and 352 ppm as CaCO₃ for the Basal McMurray (Phases F to H). Operating capacities for the Strong Acid Cation (SAC) and Weak Acid Cation (WAC) resins are based on vendor recommendations. Blowdown recycle and total dissolved solids influence sodium interference and reduce the operating capacity of SAC resin. This may contribute to more frequent regenerations and result in increased regeneration waste. Use of higher hardness water will similarly require more frequent regeneration and result in increased regeneration waste. Regen waste quantities are also including the Phase A-E Brackish Water Regen Waste.
- (d) Fresh water consumption will normally be minimized. Fresh water rates up to the permanent non-saline license (5,600 Sm³/d) may be used to blend with high hardness brackish water.
- (e) Sensitivity condition based on timing of well pad co-injection and blowdown and recycle ratio of co-injection/blowdown injected gas. Produced gas from wells (dry basis) is reported including co-injection/blowdown produced gas.



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21.1.2.1 Bitumen Rates

Bitumen production rates are presented in Table 21-4.

Table 21-4 Bitumen Production Capacity

Phase(s)	Bitumen Production Capacity ^(a)	
	(bbl/d)	(m ³ /d)
A to E	138,800	22,067
CDE 2 nd Stage OTSGs	21,200	3,371
F and G	80,400	12,783
H	46,100	7,329
H Amendment (the Project)	23,500	3,736
A to H	310,000	49,286
NOTE:		
^(a) Totals may not add due to rounding.		

21.1.2.2 Water Rates

Development profiles indicating anticipated production and water usage are included in Appendix G. Based on the development profile, CLTP is anticipating compliance with Directive 081 disposal limits during all years included in the development profile (2024 – 2054).

For the three cases provided in this section, it is assumed that all steam generators will operate at 82% steam quality. This assumption was made to simplify the model and may be slightly different than the block flow diagram numbers provided in Appendix G, which use 82% steam quality for Phases A to H, and 75% for the CDE 2nd Stage OTSGs.

The ideal blowdown recycle case is based on a PWSR equal to 1.0 (Table 21-5).

The maximum make-up water requirement is based on a PWSR equal to 1.0 with 0% blowdown recycle (Table 21-6).

The maximum disposal requirement is based on a PWSR equal to 1.23 (Table 21-7). This is the highest daily PWSR predicted from reservoir forecasts.

Under normal operating conditions, the make-up water and disposal rates may increase due to the addition of the two HRSGs; however, the maximum make-up water and disposal rates are forecasted to range between the values listed in Tables 21-6 and 21-7.



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Table 21-5 Water Balance Summary, Ideal Blowdown Recycle Case

Phase(s)	PWSR	Steam Quality (%)	Blowdown Recycle (%)	Brackish Make-up (t/d)	Water Treating Regen Loss (t/d)	WLS Sludge Water (t/d)	Blowdown Disposal (t/d)
A to E	1.00	82	50	5,029	555	29	4,317
A to E, plus CDE 2 nd Stage OTSG's	1.00	82	75	5,138	588	34	4,390
F and G	1.00	82	50	4,995	270	37	3,594
H	1.00	82	50	2,497	160	18	3,209
A-H	1.00	82	57	12,630	1,029	89	11,193

Table 21-6 Water Balance Summary, Maximum Make-Up Water Case

Phase(s)	PWSR	Steam Quality (%)	Blowdown Recycle (%)	Brackish Make-up (t/d)	Water Treating Regen Loss (t/d)	WLS Sludge Water (t/d)	Blowdown Disposal (t/d)
A to E	1.00	82	0	9,281	438	34	8,705
A to E, plus CDE 2 nd Stage OTSG's	1.00	82	0	10,857	512	40	10,179
F and G	1.00	82	0	6,900	324	25	6,436
H	1.00	82	0	6,032	283	22	5,632
A-H	1.00	82	0	23,650	1,118	87	22,247



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Table 21-7 Water Balance Summary, Maximum Disposal Case

Phase(s)	PWSR	Steam Quality (%)	Blowdown Recycle (%)	Brackish Make-up (t/d)	Water Treating Regen Loss (t/d)	WLS Sludge Water (t/d)	Blowdown Disposal (t/d)	Produced Water Disposal (t/d)
A to E	1.23	82	0	2,733	444	36	8,705	2,898
A to E, plus CDE 2 nd Stage OTSG's	1.23	82	0	2,850	515	42	10,179	2,606
F and G	1.23	82	0	0	308	25	6,436	0
H	1.23	82	0	0	270	22	5,632	0
A-H	1.23	82	0	2,850	1,090	89	22,247	1,888



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21.1.2.3 Produced Water Rates

The produced water flow rates are presented in Table 21-8.

Table 21-8 Produced Water Rates

Phase(s)	Produced Water Rates (Sm ³ /d)
A to E	39,524
CDE 2 nd Stage OTSGs	6,695
F and G	29,224
H	25,572
A to H	101,015

These design values are based on a PWSR equal to 1.0 and an updated SOR of approximately 2.0. Higher water rates may occur as a result of a PWSR greater than one, or optimization of steam rates.

21.1.2.4 Produced Gas Rates

The most recent forecasts for the Christina Lake facility show a continuing upward trend in produced gas rates and Gas to Oil Ratio (GOR), peaking in Q1 2022 before declining through to Q1 2027.

Increases in produced gas rates are tied to the timing of well pad co-injection and blowdown programs that are forecasted for the Project. Co-injection and blowdown are crucial strategies for Christina Lake reservoir and SOR management.

At the planned first oil date for the Project, forecast data shows a GOR of 11 and 23 Sm³ of dry produced gas per m³ of bitumen on the Phase FG trunk, and full field, respectively. The estimated GOR includes produced gas from the reservoir, as well as recycled gas from the co-injection and blowdown operations.

Forecast produced gas flow rates are provided in Table 21-9.

Table 21-9 Produced Gas Rates

Phase(s)	Produced Gas Rates Design Case ^(a) (e ³ Sm ³ /d)	Produced Gas Rates Sensitivity Case ^(b) (e ³ Sm ³ /d)
A to E	406.9	802.4
CDE 2 nd Stage OTSGs	62.1	122.5
F and G	293.2	578.1
H	146.6	289.0
A to H	908.8	1,792.0
NOTES: (a) Design case is based on a GOR of 18 (b) Sensitivity case is based on a GOR of 36		



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21.1.2.5 Lift Gas Rates

The CLTP no longer utilizes gas lift for SAGD production.

21.1.3 Central Processing Facility Production Description

21.1.3.1 Production Processing

The Project has made limited change to the scope of this system since the Phase H application. Changes include the addition of several produced water/glycol heater exchangers.

Reference process flow diagrams are found in Appendix H:

- CL1H-42-PFD-04-0140-001
- CL1H-42-PFD-04-0141-001
- CL1H-42-PFD-04-0142-001
- CL1H-42-PFD-04-0150-001
- CL1H-42-PFD-04-0152-001
- CL1H-42-PFD-04-0160-001
- CL1H-42-PFD-04-0162-001

New production processing equipment required for the Project is listed in Table 21-10.

Table 21-10 Project Production Processing Equipment

Equipment Description	Equipment Identification Number
Produced Water/Glycol Exchangers	E-4450F E-4550F E-4650A-F

21.1.3.2 Desanding System

No changes required to this section.

21.1.4 Heat Recovery Integration

Other than Boiler Feed Water Heating equipment, the Project has made no change to the scope of this system since the Phase H application.

Reference process flow diagrams (PFDs) are found in Appendix H:

- CL1H-42-PFD-02-0140-001
- CL1H-42-PFD-02-0161-001
- CL1H-42-PFD-02-0161-002



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- CL1H-42-PFD-02-0161-005
- CL1H-42-PFD-04-0160-001
- CL1H-42-PFD-05-0140-001
- CL1H-42-PFD-06-0140-001

21.1.4.1 Boiler Feed Water Heating

The Project has provided additional BFW booster and charge pumps, and BFW/Blowdown Exchanger as listed in Section 21.1.8 below.

Reference PFDs are found in Appendix H:

- CL1H-42-PFD-02-0140-01
- CL1H-42-PFD-02-0161-001
- CL1H-42-PFD-02-0161-002
- CL1H-42-PFD-02-0161-005

21.1.4.2 Sales Oil/Diluent Heat Exchange

No changes required to this section.

21.1.4.3 Glycol System

The Project has made limited change to the scope of this system since the Phase H application. Changes include several glycol air coolers to increase cooling capacity.

Reference PFDs are found in Appendix H:

- CL1H-42-PFD-07-0142-001
- CL1H-42-PFD-07-0142-002

New glycol system equipment required for the Project is listed in Table 21-11.

Table 21-11 Project Glycol System Equipment

Equipment Description	Equipment Identification Number
Glycol Air Coolers	AC-7351A-J

21.1.5 Make-up Water and Produced Water Treatment

21.1.5.1 Make-up Water Treatment

There are no changes required to this system as a result of the Project.



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21.1.5.2 Produced Water Treatment

The Project proposes the implementation of a CFU to replace the IGF equipment proposed in the Phase H application. Changes to the produced water de-oiling system are further discussed below.

Reference PFDs for Phase H are found in Appendix H:

- CL1H-42-PFD-01-0161-001
- CL1H-42-PFD-01-0161-002
- CL1H-42-PFD-01-0162-001
- CL1H-42-PFD-01-0163-001
- CL1H-42-PFD-01-0164-001
- CL1H-42-PFD-01-0166-001
- CL1H-42-PFD-01-0166-002

Producing Water De-Oiling

In the Project, the de-oiling train consists of a process water (PW) Surge Tank, CFU, and Oil Removal Filter (ORF). The PW Surge Tank gathers produced water from Phases F, G, and H. Produced water is pumped to the CFU which is designed for 99% bulk oil removal. From the CFU, produced water is routed to a set of ORFs for final oil removal.

The ORFs, which are hydromotion filters common to the heavy oil industry, capture residual traces of dispersed oil from the produced water. Hydromotion filters can remove about 90% of finely dispersed oil droplets from a produced water stream. The filter feed stream is expected to contain between 10 to 20 ppm of finely dispersed oil. The de-oiled water from the filters will normally contain less than 2 ppm residual oil and is acceptable for the Warm Lime Softeners (WLSs).

Produced water from the ORFs is routed to the De-oiled Water Tank. The tank provides surge capacity and reserve water to accommodate minor upsets and normal flow fluctuations.

Skim oil from the PW Surge Tank is routed to an Oil Recycle Tank where water is separated from the oil. Separated oil is recovered to the free water knock-out drum via the off-spec oil header. Separated water is recycled back to the PW Surge Tank.

New produced water de-oiling system equipment required for the Project is listed in Table 21-12.

Table 21-12 Project Produced Water De-oiling System Equipment

Equipment Description	Equipment Identification Number
PW Surge Tank	T-0515
CFU Feed Pumps	P-0520A/B/C
CFU Package	PK-0525
Skim Vessels	V-0522A/B/C



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Table 21-12 Project Produced Water De-oiling System Equipment

Equipment Description	Equipment Identification Number
Compact Flotation Units (CFU)	V-0525A/B/C
Reject Vessel	V-0527
Oil Removal Filter Packages (ORFs)	PK-0540D
De-oiled Water Pumps	P-0558D
Oil Recycle Tanks	T-0545B
Oil Recycle Pumps	P-0548A/B
Water Recycle Pumps	P-0550A/B
De-oiling Polymer Injection Package	PK-0779, T-0778

Water Softening System

No changes required to this system as a result of the Project.

21.1.5.3 Boiler Blowdown Recycle

No changes required to this section.

21.1.5.4 Water Disposal – Blowdown and Regeneration Waste

No changes required to this section.

21.1.5.5 Produced Water Disposal

No changes required to this section.

21.1.6 Utilities

With the exception of electricity/cogeneration, the Project will not significantly change any of the other Phase H utilities equipment.

21.1.6.1 Cogeneration

The Project includes two 48 MW GTGs for electricity and steam cogeneration. Electricity from the cogeneration units in Phases F and H (as well as the grid for back-up) will be used to supply power to the CPF, including Phase H. The existing Sunday Creek substation with a possible bus expansion will accommodate the Phase H Cogeneration feeds.

Reference energy balances are found in Appendix G.

Reference PFDs for utilities are found in Appendix H:

- CL1H-42-PFD-07-0141-001



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- CL1H-42-PFD-07-0142-001
- CL1H-42-PFD-07-0142-002
- CL1H-42-PFD-07-0143-001
- CL1H-42-PFD-07-0144-001
- CL1H-42-PFD-07-0145-001
- CL1H-42-PFD-07-0145-003
- CL1H-42-PFD-07-0147-001
- CL1H-42-PFD-07-0148-001

21.1.7 Fluid Storage

The Project has made limited change to the scope of this system since the original Phase H application. Changes include the addition of two diluent/glycol exchangers.

Reference PFDs are found in Appendix H:

- CL1H-42-PFD-06-0140-001
- CL1H-42-PFD-06-0141-001
- CL1H-42-PFD-06-0141-002

New Diluent System equipment required for the Project is listed in Table 21-13.

Table 21-13 Project Diluent System Equipment

Equipment Description	Equipment Identification Number
Diluent/Glycol Exchangers	E-4065C1/C2

21.1.8 Steam Generation

The Project is proposing to increase steam generation capacity through the addition of two 112 MW HRSGs. The Project will also include additional boiler feedwater/blowdown/glycol heat exchange to increase heat integration.

Reference PFDs for the steam generation system are found in Appendix H:

- CL1H-42-PFD-02-0140-001
- CL1H-42-PFD-02-0161-001
- CL1H-42-PFD-02-0161-002
- CL1H-42-PFD-02-0161-004
- CL1H-42-PFD-02-0162-005

New steam generation equipment required for the Project is listed in Table 21-14.



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Table 21-14 Project Steam Generation Equipment

Equipment Description	Equipment Identification Number
HRSs	B-5600/5650
Gas Turbines	GT-5500/5550
HP Natural Gas Filters/Separators	F-5495A/B
HP Natural Gas Heater	EH-5494
Steam Separators	V-5700
BFW / Blowdown Exchangers	E-5705
Blowdown/Glycol Exchangers	E-5710
BFW Booster Pumps	P-3010H
BFW Charge Pumps	P-3015H

21.1.9 Vapour Recovery System

The Project has made limited change to the scope of this system since the Phase H application. Changes include the addition of a PW Surge Tank and Oil Recycle Tank.

Reference PFDs for the vapour recovery system are found in Appendix H:

- CL1H-42-PFD-07-0140-001
- CL1H-42-PFD-07-0140-002

New waste gas sources tied into vapour recovery equipment are detailed in Table 21-15.

Table 21-15 Project Equipment with Vapour Recovery

Equipment Description	Equipment Identification Number
PW Surge Tank	T-0515
Oil Recycle Tank	T-0545B

21.1.10 Sulphur Removal Facility

The produced gas handling facilities at the Phase A-E and F-H CPFs include dedicated Non-Regenerative Scavenger Unit (NRSU) trains that utilize a triazine-based chemical to remove sulphur from the produced gas streams. The current Phase A-E and F-H NRSU design configuration is provided in Figure 21-2, below.

The NRSU design is based on a GOR of 11 Sm³ gas per m³ of bitumen and a Sulphur to Bitumen Ratio of 0.2 kg S per m³ of bitumen.

As given in Section 21.1.2.4, the forecast GOR for the CLTP ranges from 18 to 36 and is significantly higher than the design GOR for the Phase A-E and F-H NRSU trains. Based on the forecast GOR, Cenovus anticipates a produced gas rate of up to 1,792 e³m³/d, and due to hydraulic limitations, a partial



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bypass of the NRSUs is required. Given this, Cenovus proposes to maintain the current SO₂ limit of 7.0 t/d issued under EPEA Approval No. 48522-01-14 for the Project. An ambient air quality assessment has been completed for the proposed emission limit and the modeled ground level SO₂ concentrations are predicted to be within the Alberta Ambient Air Quality Objectives (see Appendix F).

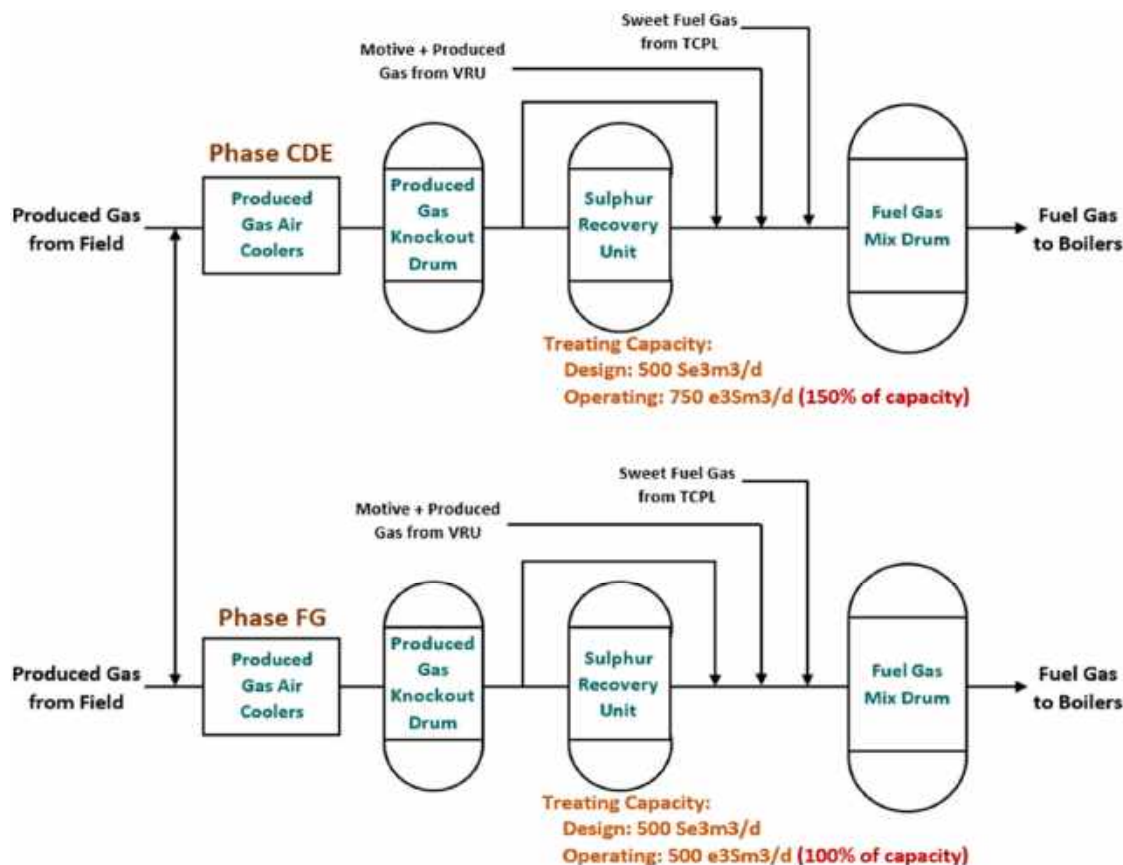


Figure 21-2 CLTP NRSU Design Configuration

21.1.11 Flare System

No changes required to this section.

21.1.12 Blend and Diluent Storage Terminal

No changes required to this section.

21.1.13 Offsites Process Description

No changes required to this section.



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21.1.14 Roads and Infrastructure

No changes required to this section.

21.1.15 Design Standards

The Project will apply the same design standards as the original Phase H application.

21.2 PROPOSED CHANGES TO GENERATED SUBSTANCES

Refer to Section 21.15 to 21.18 for details on emission streams to air resulting from the combustion of fuel gas.

The Project's waste streams will be integrated into the existing CLTP waste management system. The Project will generate solid and liquid waste streams associated with the cooling system's heat medium (coolant), lubrication oil and filters, wash water, and domestic waste from operations. Under normal operating conditions the cooling system's heat medium is fully contained within the system. Demineralized wash water will be used to clean the gas-turbine during maintenance operations.

21.3 EFFICIENCY OPTIMIZATION, SUBSTANCE RELEASE REDUCTION, AND WASTE MINIMIZATION

The concept of total recycle of produced water will be maintained in Phase H, except for the 2nd stage blowdown which cannot be recycled. Make-up water is currently drawn from the Basal McMurray source wells. Christina Lake facilities are designed to recycle between 0 and 75% of the steam generator blowdown, excluding the 2nd stage steam generator blowdown. Recycling blowdown acts to reduce water requirements for make-up and minimize water consumption and disposal rates. The make-up water treatment system is designed to satisfy the water make-up requirements assuming no boiler blowdown recycle. Blowdown recycle will be maximized; however, short-term upsets in blowdown recycle may occur intermittently during plant upsets or start-up scenarios.

21.4 FOOTPRINT MINIMIZATION

The Project will be located entirely within the existing footprint of the CLTP CPF, thereby not requiring development of any previously undisturbed land. Water and wastewater systems will be integrated into the existing facilities and the general operations of the CLTP.

21.5 SCALED DIAGRAMS OF THE PLANT

Scale diagrams of the Project (plot plans) are provided in Appendix C.

21.6 PROPOSED CHANGES TO MATERIAL STORAGES

A list of new tanks to be installed for the Project are provided in Table 21-16.



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Table 21-16 Storage Tanks

Tank Status	Tank ID	Description of Tank	Location	Contents	Capacity (m³)	Placement	Material of Primary Container	Corrosion Control	Secondary Containment	Method of Leak Detection	Maximum True Vapour Pressure	Type of Vents	Fugitive Emissions Controls
Proposed	T-0515	Produced Water Surge Tank	Outside	Produced Water		Above Grade	Carbon Steel	Devchem 256	Liner and Berm	API 650 Annex 1	95 kPaa @90C	PVSV	Vapour Control Unit
Proposed	T-0545B	Oil Recycle Tank	Outside	Produced Water/Oil	590	Above Grade	Carbon Steel	Enviroline 405HTR/ Devchem 256	Liner and Berm	API 650 Annex 1	95 kPaa @90C	PVSV	Vapour Control Unit



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**21.7 PROPOSED CHANGES TO COLLECTION AND STORAGE
PERFORMANCE MONITORING**

There are no proposed changes to collection or storage performance monitoring. All new required tanks will meet Secondary Containment guidelines and be included in existing regular maintenance activities at the CLTP. All chemicals stored in the new tanks are considered non-hazardous.

21.8 PROPOSED CHANGES TO TREATMENT AND CONTROL SYSTEMS

Not applicable. The Project does not require changes to the existing treatment and control systems. The Project will be integrated into the existing CLTP CPF wastewater treatment and release control systems. The project does result in an increase to anticipated disposal water volumes, and an updated hydrogeological assessment for the Project is included as Appendix E.

**21.9 PROPOSED CHANGES TO SUITABILITY AND CAPACITY OF
WASTEWATER TREATMENT AND RELEASE CONTROL**

Not applicable. The Project will be integrated into the existing CLTP CPF wastewater treatment and release control systems.

**21.10 SCALED DIAGRAM OF PROPOSED CHANGES TO TREATMENT
FACILITIES AND DISPOSAL LOCATIONS**

Not applicable. There are no changes to the CLTP CPF treatment and disposal locations.

**21.11 PROPOSED CHANGES TO MONITORING FOR PERFORMANCE
EVALUATION**

Not applicable. There are no changes to the CLTP CPF performance monitoring and evaluation

**21.12 CHANGES IN LOCATION AND TO RELEASE OF TREATED
WASTEWATER**

Not applicable. There are no proposed changes to the location and release of treated wastewater. The Project does result in an increase to anticipated disposal water volumes, and an updated hydrogeological assessment for the Project is included as Appendix E.



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21.13 PROPOSED CHANGES TO AMBIENT MONITORING FOR WASTEWATER RELEASE

Not applicable. No changes are proposed to the monitoring and reporting programs that are conducted as per *EPEA* Approval 48522-01-14 (as amended).

21.14 PROPOSED CHANGES TO WASTEWATER RELEASE AND DISPOSAL DETAILS

Not applicable. There are no proposed changes to the release and disposal of treated wastewater.

21.15 PROPOSED CHANGES TO SUBSTANCES RELEASED TO AIR

The primary substances of interest associated with the Project are SO₂ and NO_x. Oxides of nitrogen are produced in most combustion processes and are almost entirely made up of nitric oxide (NO) and NO₂. Together they are often referred to as NO_x.

21.16 PROPOSED CHANGES TO NATURE OF AIR EMISSIONS

The emission rates and substances released to the air for the new cogeneration units are provided in Table 21-17 in Section 21.18. An air quality assessment, including the specifications and emission data for the new cogeneration units and the approved CLTP emission sources, is provided in Appendix F.

The addition of the two cogeneration units are anticipated to increase the CLTP NO_x emissions by 11%. The total SO₂ emissions from the CLTP remain the same at 7 t/d after the addition of the cogeneration units (see Appendix F).

21.17 AIR EMISSIONS MINIMIZATIONS

An air quality assessment, including the specifications and emission data for the two new cogeneration units is provided in Appendix F. The Project is predicted to decrease the maximum concentrations within the air quality study area in the range of 0 to 3% (see Section 21.22). The predicted decrease is due to updated NO_x and SO₂ emission rates after the Project addition.

21.18 AIR EMISSION DETAILS

Approved air emission sources at the CLTP includes 29 steam generators, 6 glycol heaters, 4 flash treaters, and 2 cogeneration units. The Project consists of two proposed cogeneration units that burn natural gas in the turbines and mixed fuel gas in the HRSGs.



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An air quality assessment, including the specifications and emission data for the two new cogeneration units is provided in Appendix F. The emission rates for the two new cogeneration units are presented in Table 21-30 below. A simplified plot plan with emission source stack locations is provided as Figure 21-3. The emission rates for the 41 approved sources are provided in Table 4-2 of the Appendix F.

Table 21-17 Stack and Emission Parameters Associated with the Two New Cogeneration Units at the CLTP

Source identification No.		GT-5500 Turbine	GT-5500 HRSG Boiler	GT-5550 Turbine	GT-5550 HRSG Boiler
Unit Name / Description		Cogeneration Unit ^a		Cogeneration Unit ^a	
Temporal Variation		Continuous	Continuous	Continuous	Continuous
Capacity - Heat Input (HHV)	MW	135	81.3	135	81.3
	MMBtu/h	461	277	461	277
Efficiency (HHV)	%	73.7		73.7	
Fuel Type	-	Sweet fuel gas (natural gas)	Mixed fuel gas	Sweet fuel gas (natural gas)	Mixed fuel gas
Fuel Consumption	10 ³ Sm ³ /d ^b	287	179	287	179
Stack Location					
UTM NAD 83	m E	507181		507197	
UTM NAD 83	m N	6159898		6159870	
Base Elevation of Stack	m ASL	564		564	
Stack Dimensions					
Height Above Base Elevation	m	32		32	
Inside Tip Diameter	m	3.34		3.34	
Exhaust Parameters					
Exit Velocity	m/s	22.7		22.7	
Exit Temperature	C	204		204	
	K	474		474	
Emission Rate					
NO _x ^c	t/d	0.961		0.961	
SO ₂	t/d	0.167		0.167	
NOTES:					
^a The power output of the turbine of each cogeneration unit is 47.5 MW.					
^b Sm ³ /d: referenced to 15 C and 101.325 kPa.					
^c NOx emission rates are calculated based on ECCC 2017 Guideline (ECCC 2017) (see Appendix F).					



\\Ca0002-ppfs03\geomatics\Clients\Cenovus\Christina Lake Cogen EPEA\Figures\Fig_21-3_123513310_Simplified_Plot_Plan.mxd Revised: 2020-01-20 By: cmelliship



Figure No.

21-3

Title

Simplified Plot Plan

Client/Project
Cenovus
Christina Lake Cogen
EPEA

123513310 REVA

Project Location
Christina Lake, AB

Prepared by CMELLISHIP on 2019-12-18

TR by SLEMAY on 2020-01-16

IR Review by ETHOMSON on 2020-01-16



0 150 300 metres
(At original document size of 8.5x11)
1:12,000

● New Stack - Phase H
Optimization Project

● Stack

■ Building

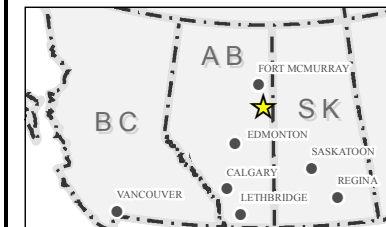
■ Christina Lake Central
Processing Facility

■ Tank

— Watercourse

□ Quarter Section

□ Waterbody



Notes

1. Coordinate System: NAD 1983 UTM Zone 12N
2. Data Sources: Canvec; Altalis
3. Background: Source: Esri, DigitalGlobe, GeoEye, Earthstar Geographics, CNES/Airbus DS, USDA, USGS, AeroGRID, IGN, and the GIS User Community



Figure 21.3

Disclaimer: This document has been prepared based on information provided by others as cited in the Notes section. Stantec has not verified the accuracy and/or completeness of this information and shall not be responsible for any errors or omissions which may be incorporated herein as a result. Stantec assumes no responsibility for data supplied in electronic format, and the recipient accepts full responsibility for verifying the accuracy and completeness of the data.

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21.18.1 Greenhouse Gas Emissions

Cenovus's corporate strategy for greenhouse gas (GHG) management is to reduce GHG emissions intensity from its operating facilities. The corporate goal is to reduce per-barrel GHG emissions by 30 percent by the end of 2030, and to achieve net-zero emissions by 2050.

GHG emissions for the Project have been calculated and are presented in Table 21-18. The Project does not offset any emissions from previously approved OTSGs at the CLTP; however, the additional power that will be produced by the Project does offset GHGs from the Alberta Power generation pool, as CLTP will require less power from the grid as a result of the Project. No offsets have been factored into the GHG estimate as presented.

Table 21-18 GHG Emissions for the Project

Parameters	Units	Cogeneration Unit GT-5500/GT-5550		Cogeneration Unit GT-5500/GT-5550	
		Turbine	HRSG	Turbine	HRSG
CO ₂ Emission	tonnes/yr	211,828	131,926	211,828	131,926
CH ₄ Emission	tonnes/yr	3.88	2.42	3.88	2.42
N ₂ O Emission	tonnes/yr	3.46	2.16	3.46	2.16
CO ₂ eq	tonnes/yr	212,957	132,629	212,957	132,629

21.19 PROPOSED CHANGES TO FLARE PIT DETAILS

Not applicable. The Project's components do not require flare pits.

21.20 PROPOSED CHANGES TO FUGITIVE EMISSIONS

Not applicable. Fugitive emissions associated with the Project are expected to be consistent with those assessed in the Phase H and Eastern Expansion Application.

21.21 PROPOSED CHANGES TO NON-POINT EMISSION SOURCES

Not applicable. There are no non-point emission sources associated with the Project.

21.22 DISPERSION MODELLING OF TREATMENT AND CONTROL SYSTEMS

Potential effects on ambient air quality were evaluated using the CALPUFF dispersion model in accordance with the AEP Air Quality Model Guideline, and are presented in Appendix F. Dispersion modelling for the Application Case includes emissions from the existing regional emission sources, in combination with the CLTP existing and approved emission sources and the two proposed cogeneration



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units. The maximum predicted concentrations, are summarized in Table 21-19, including the background concentrations.

The maximum predicted 1-hour, 24-hour, 30-day and annual average ground-level SO₂ concentrations associated with the Application Case are 299, 113, 14.5, and 8.17 µg/m³, respectively. These values include ambient background and are less than the corresponding AAAQO.

Using the Ozone Limiting Method (OLM), The maximum predicted 1-hour and annual average ground-level NO₂ concentrations associated with the Application Case are 128 and 13.9 µg/m³, respectively. These values include ambient background and are also less than the corresponding AAAQO.

Compared to the Base Case, the Project is predicted to decrease the maximum concentrations within the study area in the range of 0 to 3% (see Appendix F). The predicted decrease is due to updated NO_x and SO₂ emission rates after the Project addition. The addition of the two cogeneration units is predicted to have a minimal impact on ambient air quality.

Table 21-19 Maximum Predicted Ground-level Concentrations (µg/m³) Associated with the Application Case

Substance	Averaging Period	Maximum Predicted Ground-Level Concentrations (µg/m ³)	Ambient Background Concentration (µg/m ³)	Maximum Predicted Concentration Including Background (µg/m ³)	AAAQO (µg/m ³)	Comparison of Predictions to AAAQO (%)
SO ₂	1-hour ^b	297	2.62	299	450	66
	24-hour	110	2.62	113	125	90
	30-day	13.8	0.65	14.5	30	48
	Annual	7.82	0.35	8.17	20	41
NO ₂ ^a	1-hour ^b	118	10.0	128	300	43
	Annual	10.6	3.31	13.9	45	31

NOTES:

^a NO_x was converted to NO₂ using the Ozone Limiting Method (OLM).

^b 9th highest predictions (ESRD 2013).

21.23 PLANT AIR EMISSION DIAGRAM

See Figure 21-3 for the simplified plot plan showing the stack locations of all the CLTP emission sources.

21.24 PROPOSED CHANGES TO MONITORING FOR PERFORMANCE EVALUATION OF TREATMENT AND CONTROL SECTIONS

Not applicable. There are no proposed changes to the monitoring or performance evaluations for the CLTP.



**PHASE H OPTIMIZATION PROJECT
INTEGRATED APPLICATION TO THE ALBERTA ENERGY REGULATOR**

Proposed Changes to Design and Operation
September 2020

**21.25 PROPOSED CHANGES TO LOCATION AND MONITORING OF
AMBIENT AIR QUALITY**

CLTP currently conducts ambient air quality monitoring as per the requirements of *EPEA* Approval 48522-01-14, as amended. There are no proposed changes to ambient air quality monitoring as a result of the Project.

21.26 AIR EMISSIONS RELEASE AND DISPOSAL METHODS

Air emissions for the Project are presented in Section 21.18 and Appendix F.

**21.27 PROPOSED CHANGES TO EXISTING OPERATIONAL AND
MANAGEMENT SYSTEMS**

Not applicable. There are no proposed changes to existing operational and management systems as the Project will be an addition to the current processes at the CLTP CPF.

**21.28 EVALUATION OF NEW OPERATIONAL AND MANAGEMENT
SYSTEMS**

Not applicable. There are no proposed changes to existing operational and management systems as the Project will be an addition to the current processes at the CLTP CPF.



**PHASE H OPTIMIZATION PROJECT
INTEGRATED APPLICATION TO THE ALBERTA ENERGY REGULATOR**

Amended or Final Reclamation Plan
September 2020

22.0 AMENDED OR FINAL RECLAMATION PLAN

The Project is located within the existing CLTP CPF disturbance area. There are no changes to the reclamation plan completed for the CLTP as a result of the Project. However, as required by the existing *EPEA* approval, within six months of the CLTP ceasing operation, Cenovus will prepare and submit a Decommissioning and Land Reclamation Plan to the AER.



PHASE H OPTIMIZATION PROJECT INTEGRATED APPLICATION TO THE ALBERTA ENERGY REGULATOR

References
September 2020

23.0 REFERENCES

23.1 LITERATURE CITED

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PHASE H OPTIMIZATION PROJECT INTEGRATED APPLICATION TO THE ALBERTA ENERGY REGULATOR

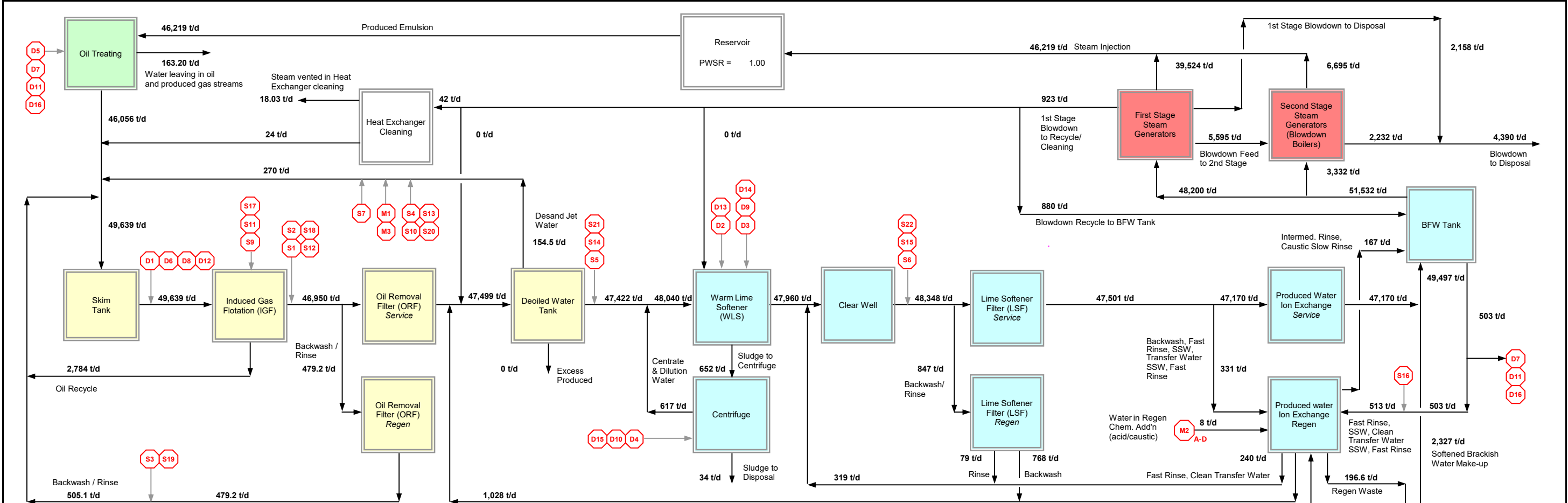
References
September 2020

- Encana FCCL Ltd. (Encana FCCL). 2009. Environmental Impact Assessment Application for Amendment to Christina Lake Thermal Expansion Project, Phases 1E, 1F, and 1G. October 2009. Available online: <ftp://ftp.gov.ab.ca/env/fs/EIA/2009-10-CenovusFCCLChristinaLakeThermalProjectPhases1E1F1GIn-situ/EIA%20Main%20Menu.pdf>
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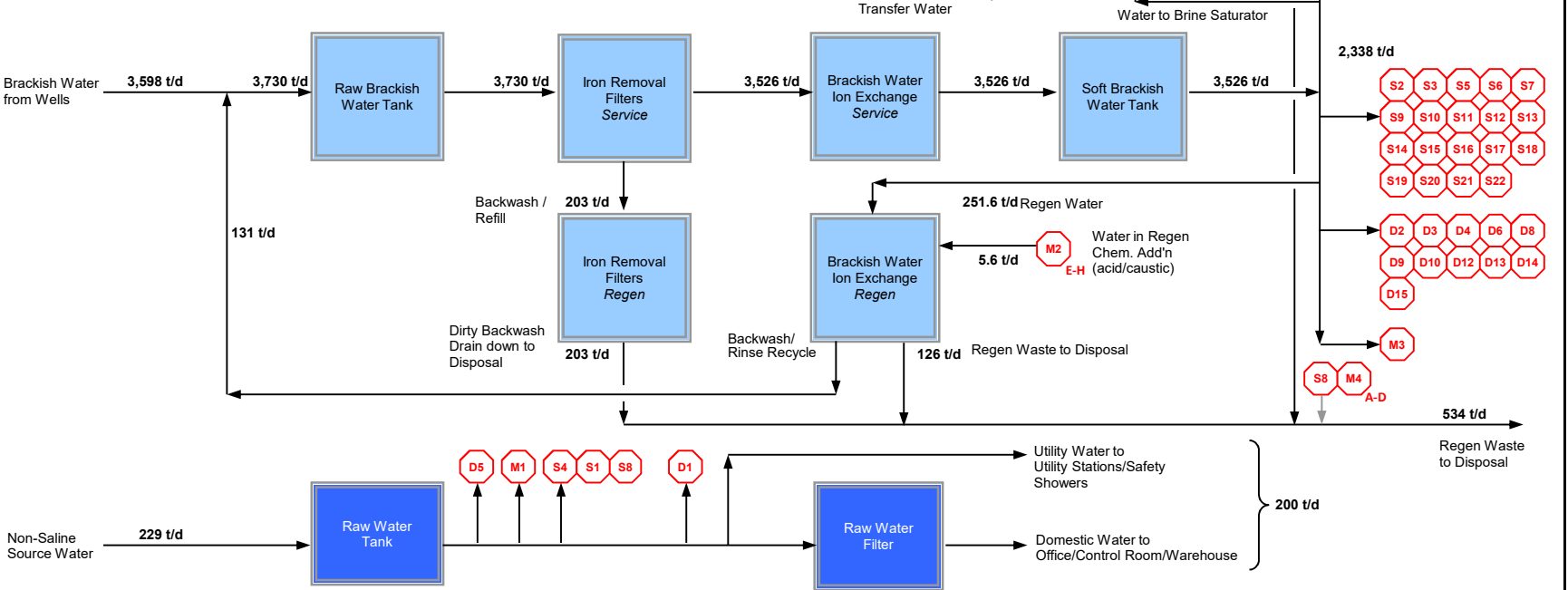


APPENDIX G

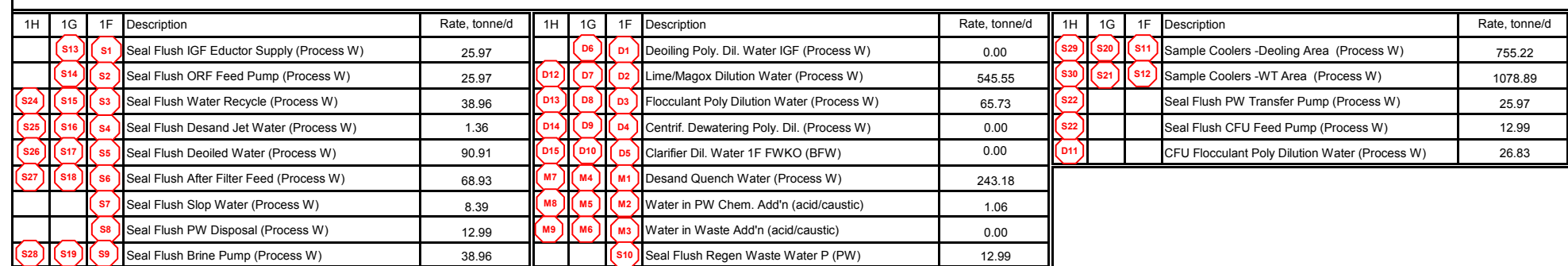
Heat and Material Balance, Energy Balance, Water Balance



Description			Description		
S1	Seal Flush IGF Pumps (Non-Saline)	16.78	S22	Seal Flush After Filter Feed Pumps (SB) 1E	22.98
S2	Seal Flush ORF Feed Pump (Soft Brack)	12.99	D1	Deoiling Poly. Dil. Water IGF (Non-Saline)	0.00
S3	Seal Flush Water Recycle (Soft Brackish)	12.99	D2	Lime/Magox Dilution Water (Soft Brackish)	221.83
S4	Seal Flush Desand Jet Water (Non-saline)	0.35	D3	WLS Poly Dilution Water (Soft Brackish)	80.86
S5	Seal Flush Deoiled Water (Soft Brackish)	25.97	D4	Centrif. Dewatering Poly. Dil. (Soft Brack)	0.00
S6	Seal Flush After Filter Feed (Soft Brack.) 1C	22.98	D5	Clarifier Dil. Wtr 1A/B FWKO (Non-saline)	0.00
S7	Seal Flush Slop Water (Soft Brackish)	8.39	D6	Deoiling Poly. Dil. Water IGF (Soft Brackish)	0.00
S8	Seal Flush Neut. Waste (Non-Saline)	0.01	D7	Clarifier Dil. Water 1C FWKO (BFW)	0.00
S9	Seal Flush IGF Eductor Supply (Soft Brack)	12.99	D8	Deoiling Poly. Dil. Wat. IGF 1D(Soft Brack.)	0.00
S10	Seal Flush Desand Jet Water (Soft Brack)	0.45	D9	WLS Poly Dil. Water 1D (Soft Brackish)	79.66
S11	Seal Flush IGF Eductor Supply (Soft Brack)	12.99	D10	Centrif. Dewatering Poly. Dil. 1D (Soft Brack)	0.00
S12	Seal Flush ORF Feed Pump (Soft Brack)	12.99	D11	Clarifier Dil. Water 1D FWKO (BFW)	0.00
S13	Seal Flush Desand Jet Water (Soft Brack)	0.34	D12	Deoiling Poly. Dil. Wat. IGF 1E(SB)	0.00
S14	Seal Flush Deoiled Water (Soft Brack.) 1D	25.97	D13	Lime/Magox Dilution Water (Soft Brack.) 1E	110.34
S15	Seal Flush After Filter Feed (Soft Brack) 1D	22.98	D14	WLS Poly. Dil. Water 1E (Soft Brackish)	79.66
S16	Seal Flush Regen. Water Feed Pumps (SB)	10.59	D15	Centrifuge Dewatering C-XXXX 1E	0.00
S17	Seal Flush IGF Educt. Supply 1E (SB)	12.99	D16	Clarifier Dil. Water 1E FWKO (BFW)	0.00
S18	Seal Flush ORF Feed Pumps 1E (SB)	12.99	M1	Desand Quench Water (Non-saline)	12.16
S19	Seal Flush Water Recycle Pumps (SB)	12.99	M2	Water in Regen Chem. Add'n (acid/caustic)	13.85
S20	Seal Flush Desand Jet Water Pump (SB) 1E	0.34	M3	Desand Quench Water (Soft Brackish)	93.87
S21	Seal Flush Deoiled Water Pumps 1E (SB)	25.97	M4	Water created in acid/caustic neut. reaction	8.74



										
									Cenovus FCCL Partnership	
									TITLE	
									CHRISTINA LAKE COMMERCIAL PLANT	
B	29-Nov-2019	Re-Issued for Regulatory Approval	SRP						Overall Water Plant Block Diagram Phase 1A-E Debottleneck	
A	20-Aug-2012	Issued for Regulatory Approval	CJG	MDE					Phase 1A-E Debottleneck	
REV	DATE	DESCRIPTION	BY	CHKD	APPD	APPD	PROJECT Christina Lake Phase 1A-E	PROJ. NO -	DOCUMENT NUMBER CL1-42-WTR-00-300-01	REV B



Water Reporting		
	Result	Max/Limit
Fresh Make-Up	0.0%	10%
Brackish Make-Up	11.8%	25.0%
PW Use	88.2%	75.0%

							CONSULTANT LOGO 	 Cenovus FCCL Partnership		
								TITLE		
								CHRISTINA LAKE COMMERCIAL PLANT		
								Overall Water Plant Block Diagram Phase 1F and Phase 1G and Phase 1H PWSR = 1.0, 100% BFW Feed, 50% of BD Recycle		
A	10/Jul/2019	Issued for Regulatory Application	BJZ	RVG	KUL					
REV	DATE	DESCRIPTION	BY	CHKD	APPD	APPD	PROJECT	PROJ. NO	DOCUMENT NUMBER	REV
							Christina Lake Phase 1H	CL1H	CL1-42-WTR-00-400-01-REG	A

Facility Overall Energy Balance	
Energy in	Energy out
Produced Gas + Purchased Gas278,581 GJ/d	Bitumen Energy2,108,701 GJ/d
Electrical8,973 GJ/d	Energy Diluent in Product1,895,545 GJ/d
Bitumen Energy2,108,701 GJ/d	Energy From Turbines16,416 GJ/d
Diluent Feed Energy1,914,692 GJ/d	
Total4,310,947 GJ/d	Total4,020,662 GJ/d

Facility Overall Energy Efficiency (Total Energy OUT / Total Energy IN)*100 (Note1)	
Energy Efficiency	93.3 %

Note:

$$(1) \quad \text{Energy Efficiency} = \frac{(\text{Total Energy OUT} / \text{Total Energy IN}) * 100}{(\text{Total Energy in Dilbit Product Out} + \text{Energy from Turbines}) / (\text{Total Energy in Feed and Purchased Offlease} + \text{Energy from Turbines})}$$

Where

Diluent Product = Diluent Feed - losses to fuel gas system etc.
 Bitumen Product = Bitumen Feed (no losses)

CL1H-42-CAL-00-007

DRAWING NUMBER	REFERENCE DRAWING	STAMPS	REV NO	REVISION	DATE	DRN	CKD	CKD	DES	LDE	PE	DESIGNED BY	CONSULTANT LOGO	 TITLE CHRISTINA LAKE COMMERCIAL PLANT ENERGY BALANCE PHASE 1A-H + CLCDE-BB DRAWING CL1-42-BFD-00-241-01 REVISION 6	
			6	Issued for Regulatory Approval(CL1H)	19.06.27	ICS	BUZ		ICS	KUL			DRAWN BY		 CADD FILE NAME PROJECT NO CL 1H
			2	Issued for Regulatory Approval(CLBB)	12.07.25	MX	APC		MX				CHECKED BY		
			3	Issued for Regulatory Approval(CL1H)	12.07.26	MX	APC		MX				LEAD ENG		
			4	Issued for Regulatory Approval(CLCDE-BB)	12.09.27	MX	APC		MX				PROJ ENG		
			5	Issued for Regulatory Approval(CL1H)	12.10.2	MX	APC		MX				WORK PKG		

APPENDIX H

Process Flow Diagrams

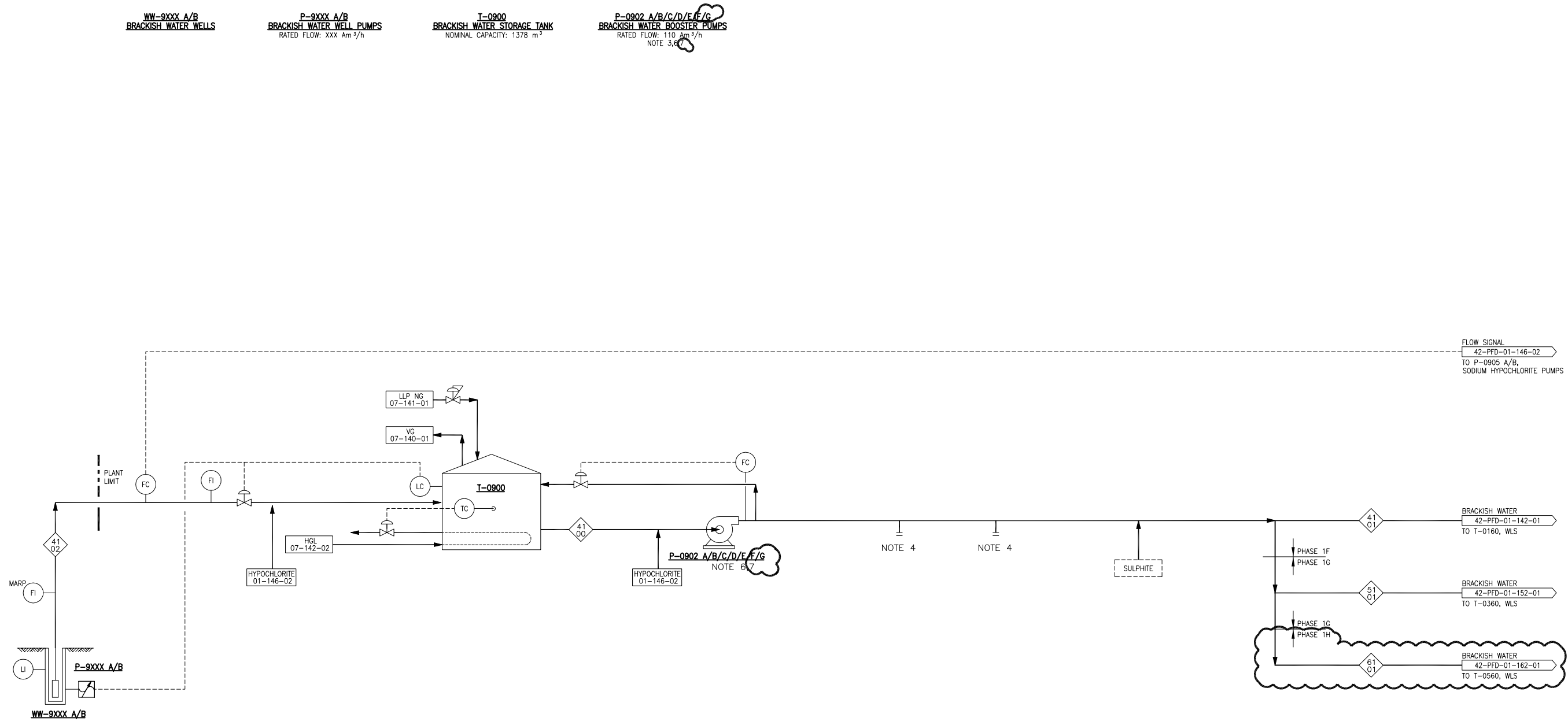


CHRISTINA LAKE COMMERCIAL PLANT
PHASE 1H EXPANSION
ALL AREAS
PROJECT #2195
PROCESS FLOW DIAGRAMS
FOR REGULATORY APPLICATION AMENDMENT



Note: Red clouds denote major equipment changes on Phase H since the previous regulatory application.

CL1-42-PFD-01-0140-001_3.A.0

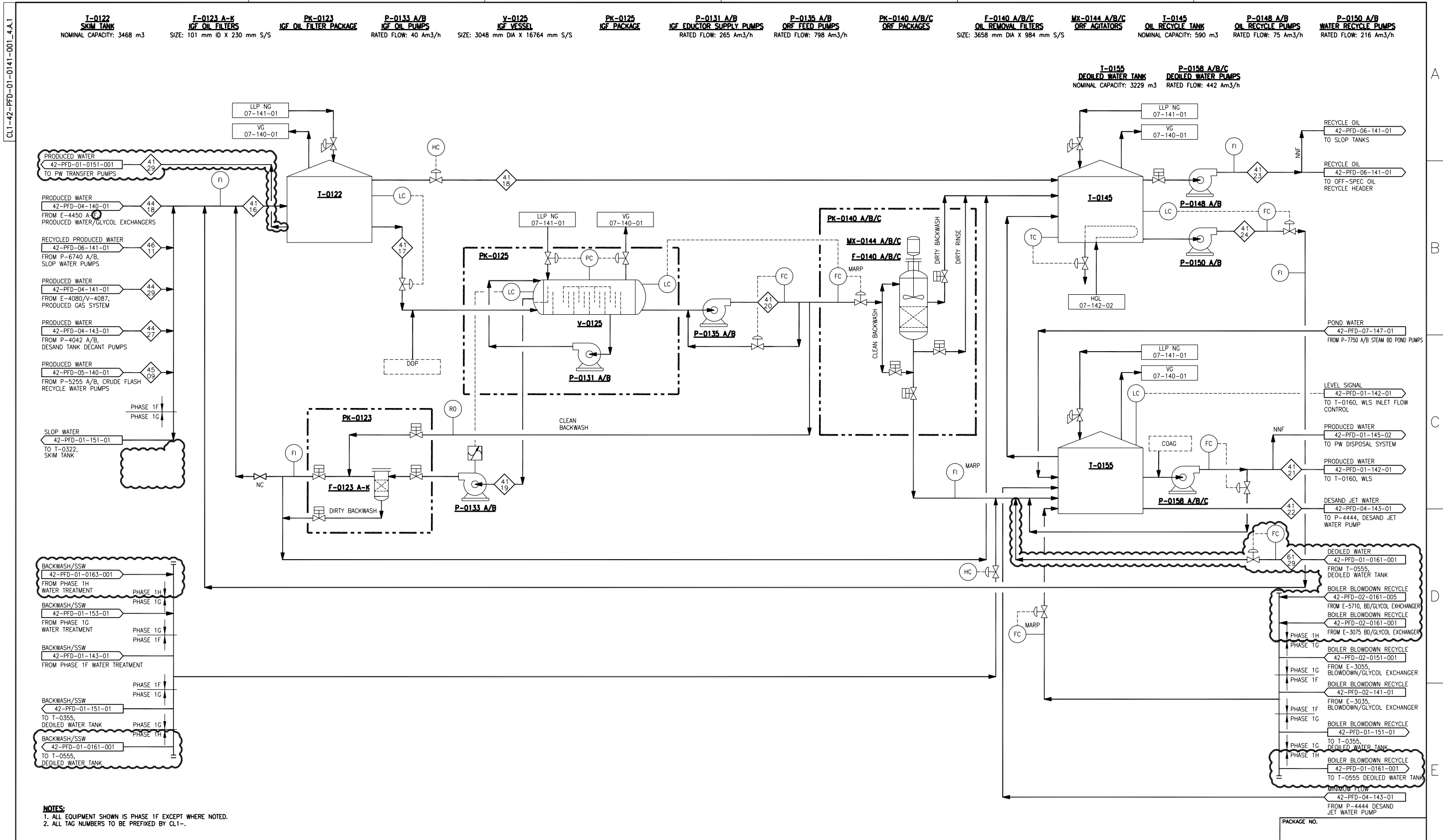


NOTES:

1. ALL EQUIPMENT SHOWN IS PHASE 1F, EXCEPT WHERE NOTED.
2. ALL TAG NUMBERS TO BE PREFIXED BY CL1-
3. TWO PUMPS OPERATING DURING NORMAL SERVICE WITH THREE PUMPS OPERATING DURING BACKWASH WHEN PWSR=0.95 WITH 0% BD RECYCLE
4. FUTURE TIE-IN POINTS FOR IRON REMOVAL FILTERS.
5. DELETED.
6. P-0902D/E ARE INSTALLED AS PART OF PHASE 1G.
7. P-0902F/G ARE INSTALLED AS PART OF PHASE 1H.

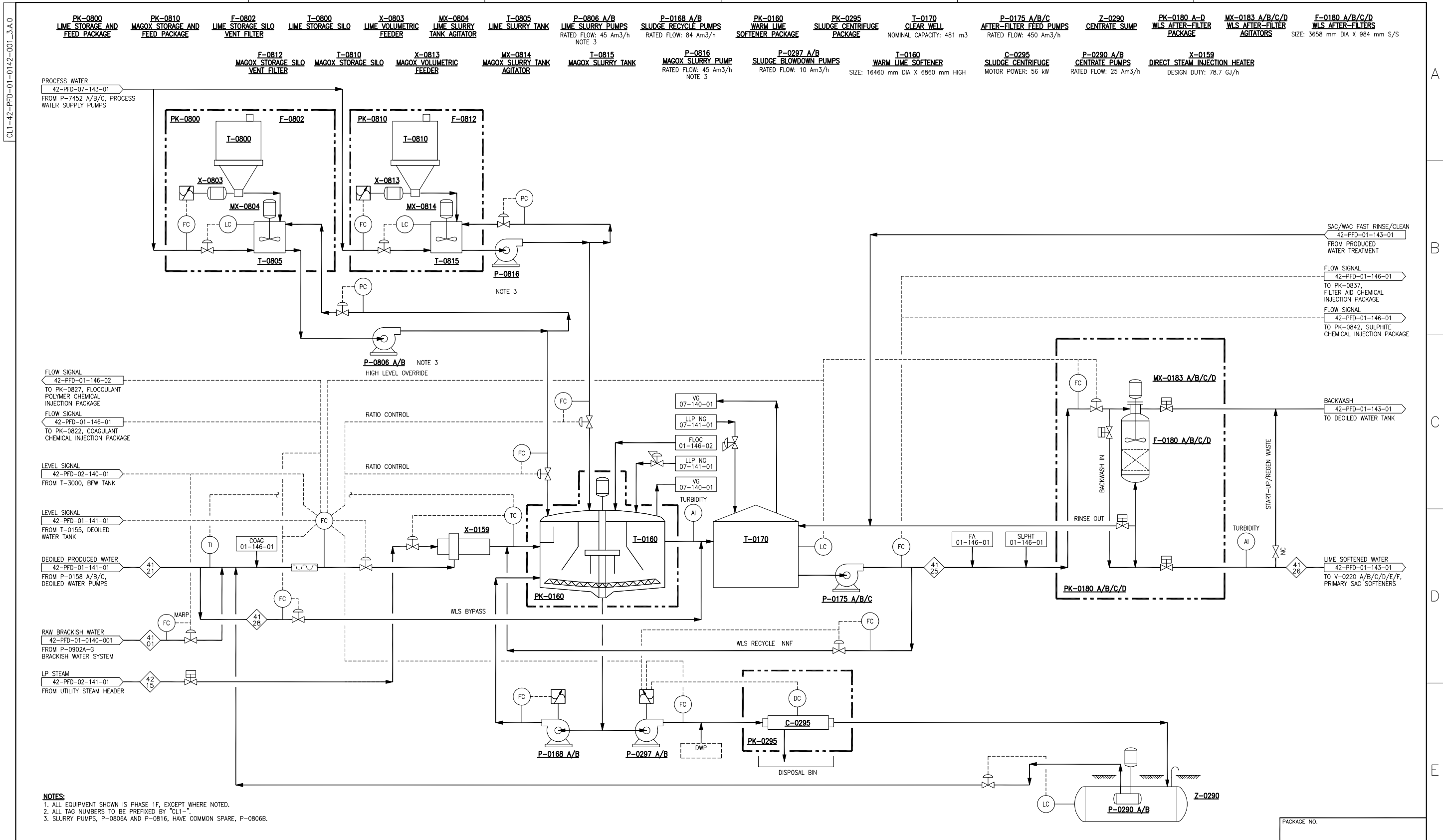
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				04/04/2019												REVISION DESCRIPTION ISSUED FOR DESIGN										PROCESS FLOW DIAGRAM			
																PROJECT NO. CL1H										BRACKISH WATER SYSTEM			
																LSD S.E. 1/4, Sec. 17, TWP 76, RG 6, W4M										PHASE 1F/1G/1H			
																ISSUE DATE 2019/04/05					SCALE					DRAWING NO. CL1-42-PFD-01-0140-001		REVISION NO. 3.A.0	

CL1-42-PFD-01-0141-001_4.A.1



- NOTES:**
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 - ALL TAG NUMBERS TO BE PREFIXED BY CL1-.

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			1V	PHASE 1G EXPANSION - REISSUED FOR DESIGN	2013/07/23	JM	RVG	LY	KU	MC		
			2V	PHASE 1G EXPANSION - ISSUED FOR PROJECT TURNOVER	2015/06/08	DL	RVG	LY	RVG	FY		
			4.A.0	PHASE 1H EXPANSION - ISSUED FOR DESIGN	2019/04/05	KSO	RVG	ZGA	KUL	JEG		
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											PROJECT NO. CL1H	
											LSD S.E. 1/4, Sec. 17, TWP 76, RG 6, W4M	
											ISSUE DATE 2019/06/11	
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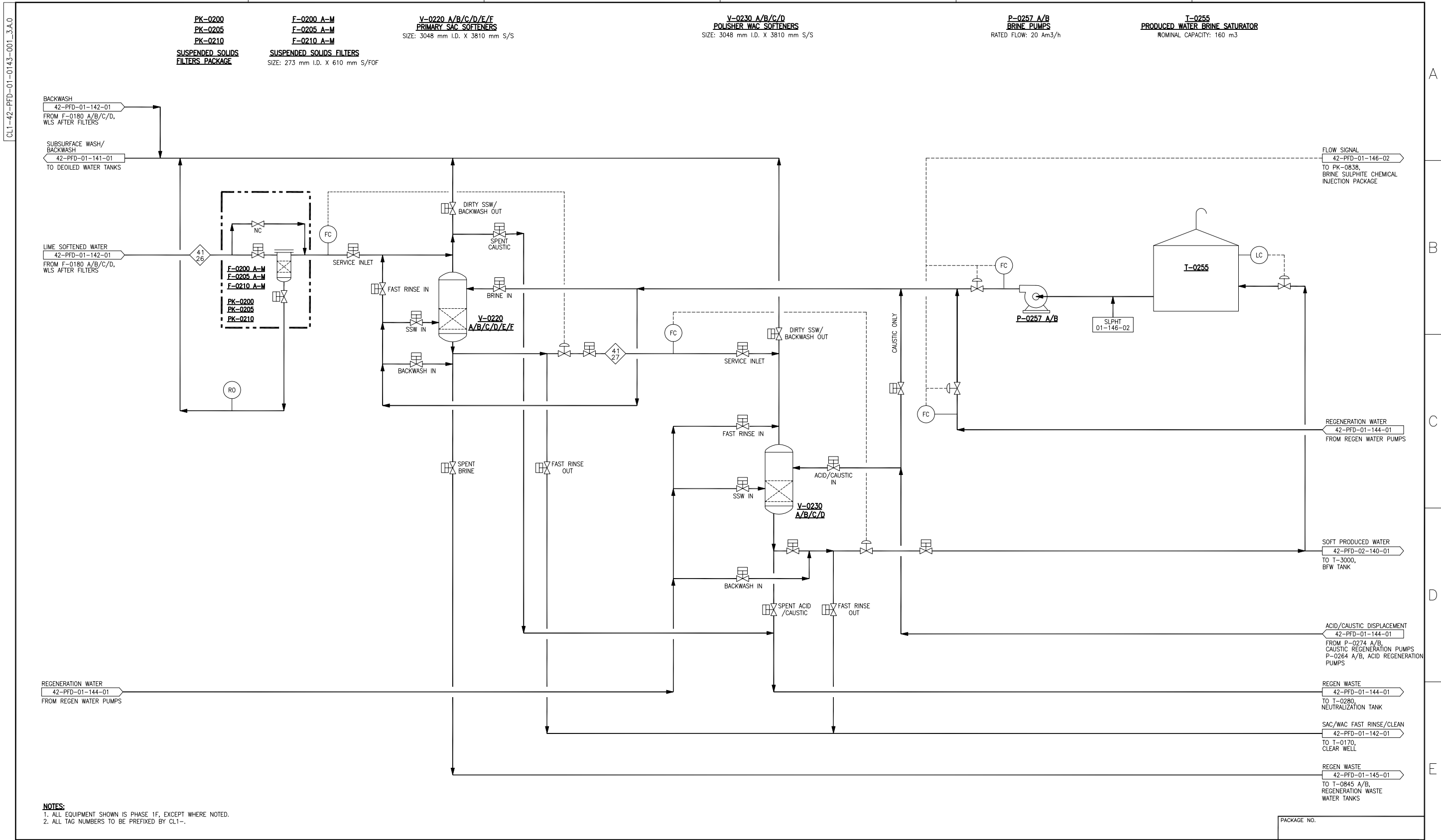


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			1V	PHASE 1G EXPANSION - REISSUED FOR DESIGN	2013/07/23	JM	RVG	LY	KU	MC		
			2V	PHASE 1G EXPANSION - ISSUED FOR PROJECT TURNOVER	2015/06/08	GP	RVG	LY	RVG	FY		
			3.A.0	PHASE 1H EXPANSION - ISSUED FOR DESIGN	2019/04/05	DSH	RVG	ZGA	KUL	JEG		
											REVISION DESCRIPTION ISSUED FOR DESIGN	
											PROJECT NO. CL1H	
											LSD S.E. 1/4, Sec. 17, TWP 76, RG 6, W4M	
											ISSUE DATE 2019/04/05	SCALE NONE
											DRAWING NO. CL1-42-PFD-01-0142-001	REVISION NO. 3.A.0

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cenovus
ENERGY



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			0V	PHASE 1G EXPANSION - ISSUED FOR DESIGN	2013/01/15	KJS	RVG	LY	KU	GP		CHRISTINA LAKE COMMERCIAL PLANT PROCESS FLOW DIAGRAM WATER TREATMENT (ION EXCHANGE) SYSTEM PHASE 1F	CL1-42-PFD-01-0143-001	3.A.0
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											REVISION DESCRIPTION ISSUED FOR DESIGN			
											PROJECT NO. CL1H			
											LSD S.E. 1/4, Sec. 17, TWP 76, RG 6, W4M			
											ISSUE DATE 2019/04/05	SCALE NONE		

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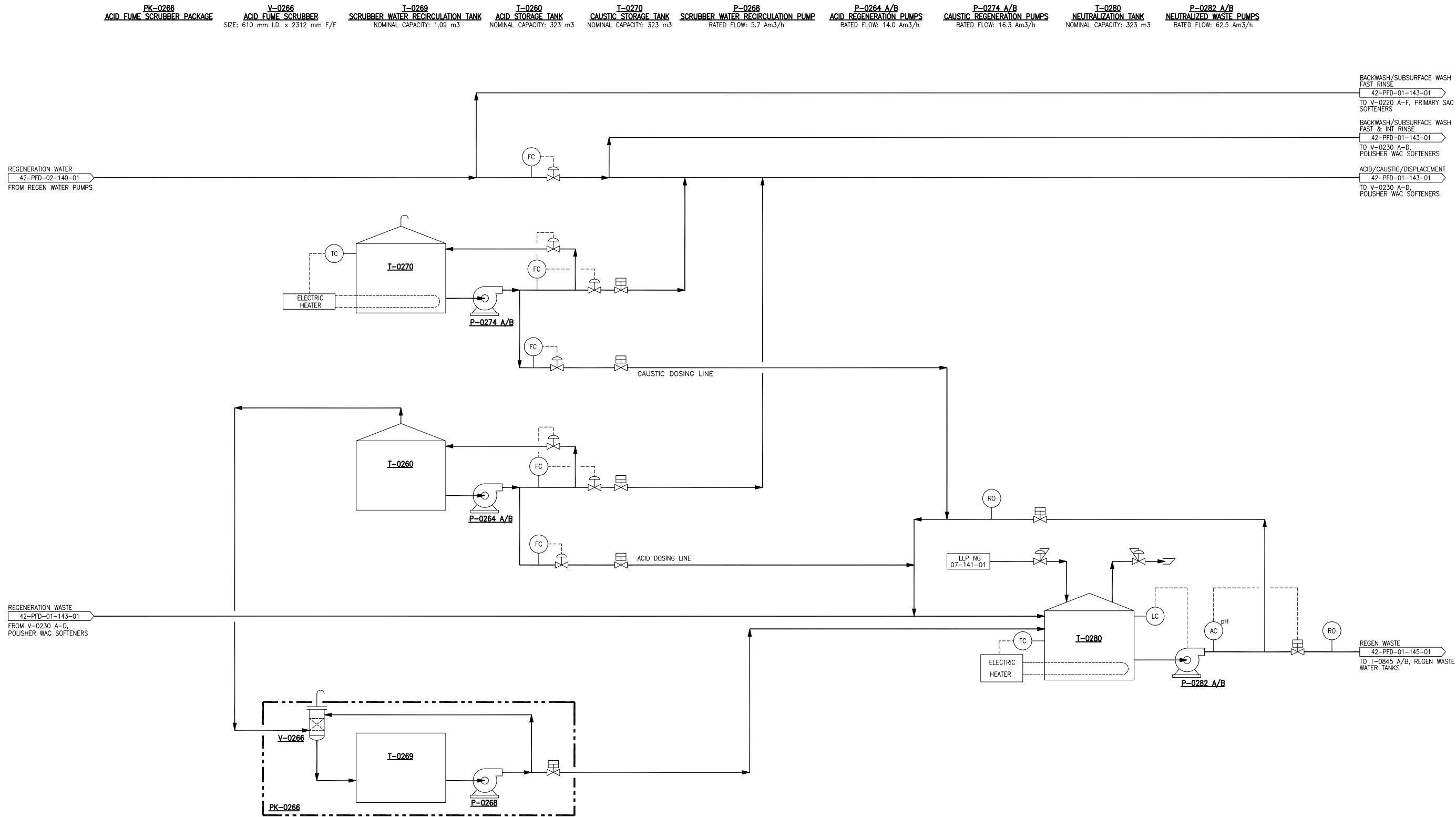
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04/04/2019



04/04/2019

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NOTES:
1. ALL EQUIPMENT SHOWN IS PHASE 1F, EXCEPT WHERE NOTED.
2. ALL TAG NUMBERS TO BE PREFIXED BY CL1-.

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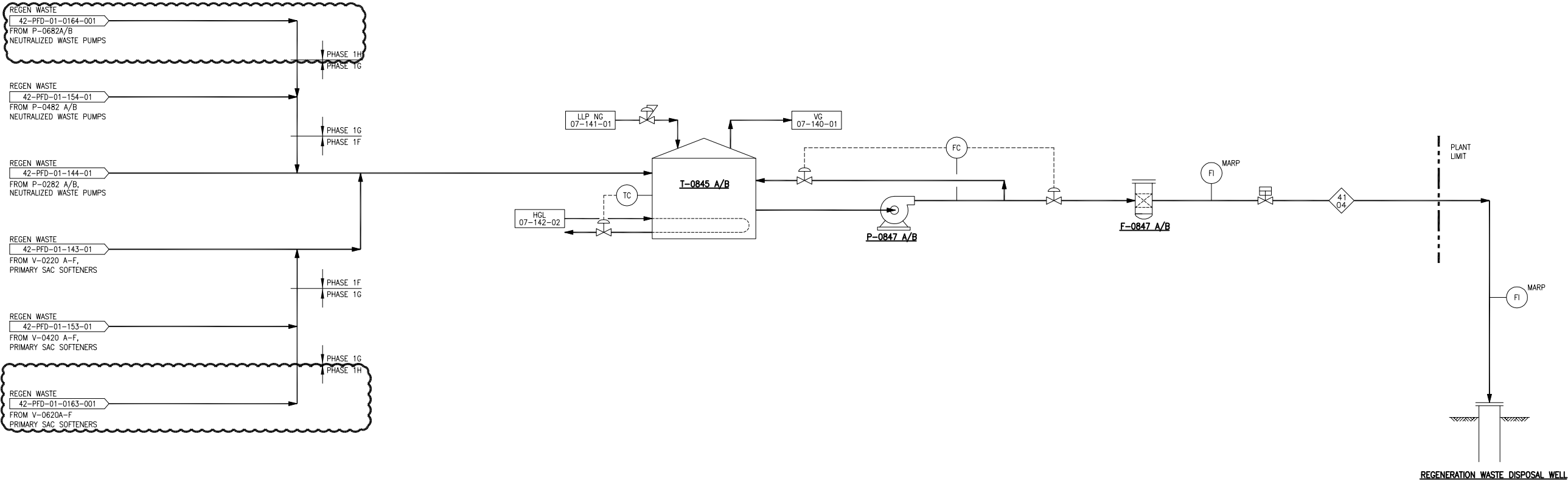
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											LSD S.E. 1/4, Sec. 17, TWP 76, RG 6, W4M	
											ISSUE DATE 2019/04/05	SCALE NONE
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CL1-42-PFD-01-0145-01_3.A.0



NOTES:
1. EQUIPMENT SHOWN IS PHASE 1F, EXCEPT WHERE NOTED.
2. ALL TAG NUMBERS TO BE PREFIXED BY CL1-.

PACKAGE NO.

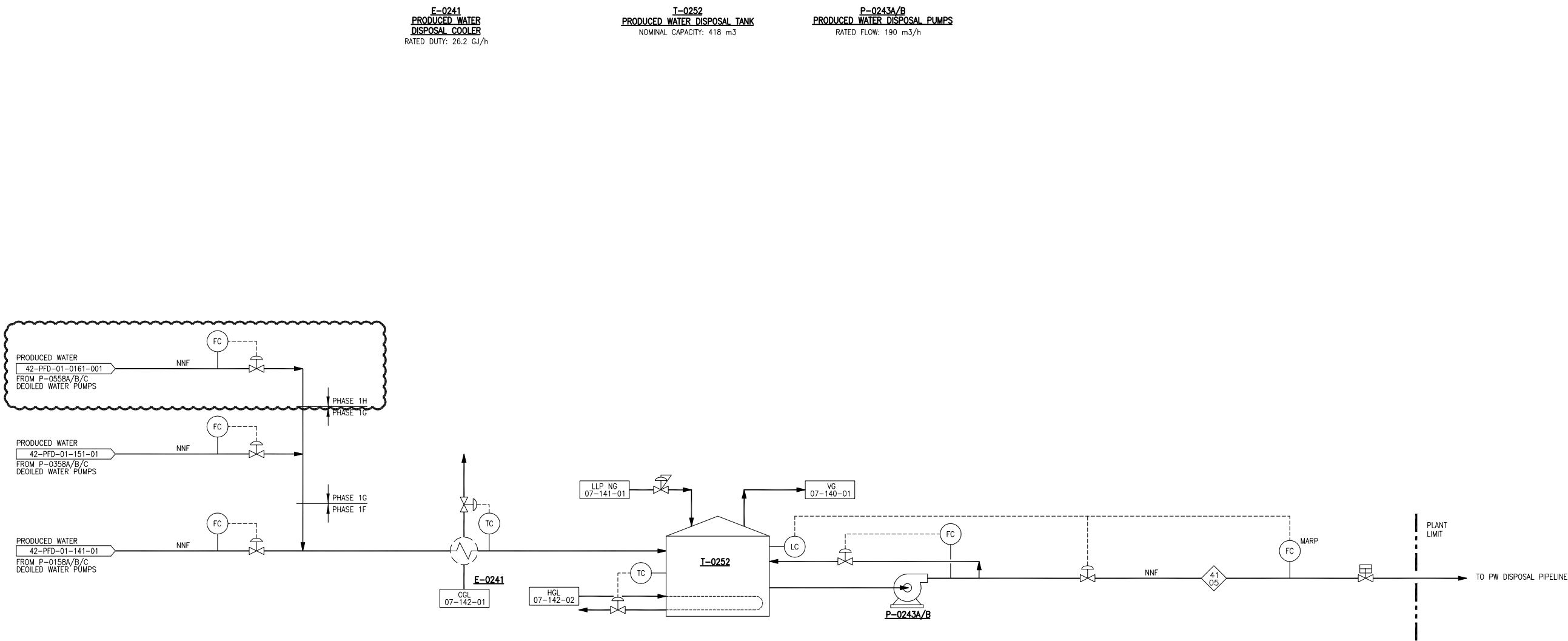
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			1V	PHASE 1G EXPANSION – REISSUED FOR DESIGN	2013/07/23	JM	RVG	LY	KU	MC				
			2V	PHASE 1G EXPANSION – ISSUED FOR PROJECT TURNOVER	2015/06/08	GP	RVG	LY	RVG	FY				
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											REVISION DESCRIPTION ISSUED FOR DESIGN			
											PROJECT NO. CL1H			
											LSD S.E. 1/4, Sec. 17, TWP 76, RG 6, W4M			
											ISSUE DATE 2019/04/05	SCALE NONE		



04/04/2019

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NOTES:
1. EQUIPMENT SHOWN IS PHASE 1F, EXCEPT WHERE NOTED.
2. ALL TAG NUMBERS TO BE PREFIXED BY CL1-.

PACKAGE NO.

REFERENCE NUMBER	REFERENCE TITLE

STAMPS

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REV NO	REVISION	DATE	DRN	CKD	DES	LDE	PE
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1V	PHASE 1G EXPANSION – REISSUED FOR DESIGN	2013/07/23	JM	RVG	LY	KU	MC
2V	PHASE 1G EXPANSION – ISSUED FOR PROJECT TURNOVER	2015/06/08	GP	RVG	LY	RVG	FY
2.A.0	PHASE 1H EXPANSION – ISSUED FOR DESIGN	2019/04/05	DSH	PVC	ZGA	KUL	JEG

CONSULTANT NAME AND LOGO

REVISION DESCRIPTION
ISSUED FOR DESIGN

PROJECT NO.
CL1H

LSD
S.E. 1/4, Sec. 17, TWP 76, RG 6, W4M

ISSUE DATE
2019/04/05

SCALE
NONE

TITLE
CHRISTINA LAKE COMMERCIAL PLANT
PROCESS FLOW DIAGRAM
PRODUCED WATER DISPOSAL SYSTEM
PHASE 1F/1G/1H

DRAWING NO.
CL1-42-PFD-01-0145-002

REVISION NO.
2.A.0

CL1-42-PFD-01-0146-001_3.A.0

T-0820
COAGULANT BULK
STORAGE TANK
NOMINAL CAPACITY: 27.8 m3

PK-0822
COAGULANT CHEMICAL
INJECTION SKID PACKAGE

P-0822 A/B
COAGULANT PUMPS
RATED FLOW: 0.042 Am3/h

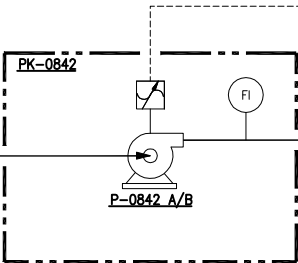
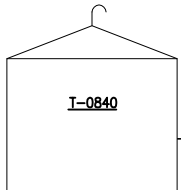
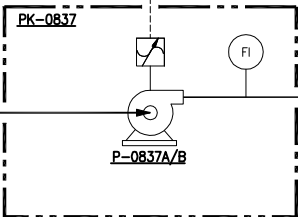
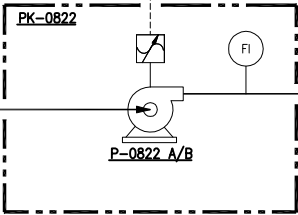
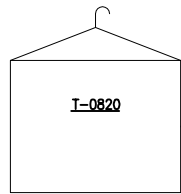
PK-0837
FILTER AID CHEMICAL
INJECTION SKID PACKAGE

P-0837A/B
FILTER AID PUMPS
RATED FLOW: 0.042 Am3/h

T-0840
SULPHITE BULK
STORAGE TANK
NOMINAL CAPACITY: 24 m3

PK-0842
SULPHITE CHEMICAL
INJECTION PACKAGE

P-0842 A/B
SULPHITE PUMP
RATED FLOW: 0.1 Am3/h



FLOW SIGNAL
42-PFD-01-142-01
FROM T-0160,
WLS FLOW CONTROL

COAGULANT
NOTE 3
TO INJECTION

FLOW SIGNAL
42-PFD-01-142-01
FROM P-0175 A/B/C,
AFTER-FILTER FEED PUMPS

FILTER AID
NOTE 3
TO INJECTION

FLOW SIGNAL
42-PFD-01-142-01
FROM P-0175A/B/C,
AFTER-FILTER FEED PUMPS

SULPHITE
NOTE 3
TO INJECTION

- NOTES:
1. ALL EQUIPMENT SHOWN IS PHASE 1F, EXCEPT WHERE NOTED.
 2. ALL TAG NUMBERS TO BE PREFIXED BY "CL1-".
 3. INJECTION POINT LOCATED ON DWG. CL1G-42-PFD-01-142-01.

PACKAGE NO.

REFERENCE NUMBER	REFERENCE TITLE

STAMPS



04/04/2019

PERMIT TO PRACTICE
VISTA PROJECTS LIMITED
APEGA PERMIT No.
P 04559
The Association of Professional Engineers,
and Geoscientists of Alberta

REV NO	REVISION	DATE	DRN	CKD	DES	LDE	PE
0V	PHASE 1G EXPANSION – ISSUED FOR DESIGN	2013/01/15	KJS	RVG	LY	KU	GP
1V	PHASE 1G EXPANSION – REISSUED FOR DESIGN	2013/07/23	JM	RVG	LY	KU	MC
2V	PHASE 1G EXPANSION – ISSUED FOR PROJECT TURNOVER	2015/06/08	GP	RVG	LY	RVG	FY
3.A.0	PHASE 1H EXPANSION – ISSUED FOR DESIGN	2019/04/05	DSH	ZGA	KUL	JEG	

CONSULTANT NAME AND LOGO	
REVISION DESCRIPTION ISSUED FOR DESIGN	
PROJECT NO. CL1H	
LSD S.E. 1/4, Sec. 17, TWP 76, RG 6, W4M	
ISSUE DATE 2019/04/05	SCALE NONE

cenovus ENERGY	
TITLE CHRISTINA LAKE COMMERCIAL PLANT PROCESS FLOW DIAGRAM CHEMICAL INJECTION – AREA 01 PHASE 1F	
DRAWING NO. CL1-42-PFD-01-0146-001	REVISION NO. 3.A.0

CL1-42-PFD-01-0146-002_3.A.0

T-0825
FLOCCULANT POLYMER TOTE
CAPACITY: 1 m3

PK-0827
FLOCCULANT POLYMER
CHEMICAL INJECTION
SKID PACKAGE

P-0827 A/B
FLOCCULANT POLYMER PUMPS
RATED FLOW: 0.002 Am3/h

T-0838
BRINE SULPHITE TOTE TANK
CAPACITY: 1 m3

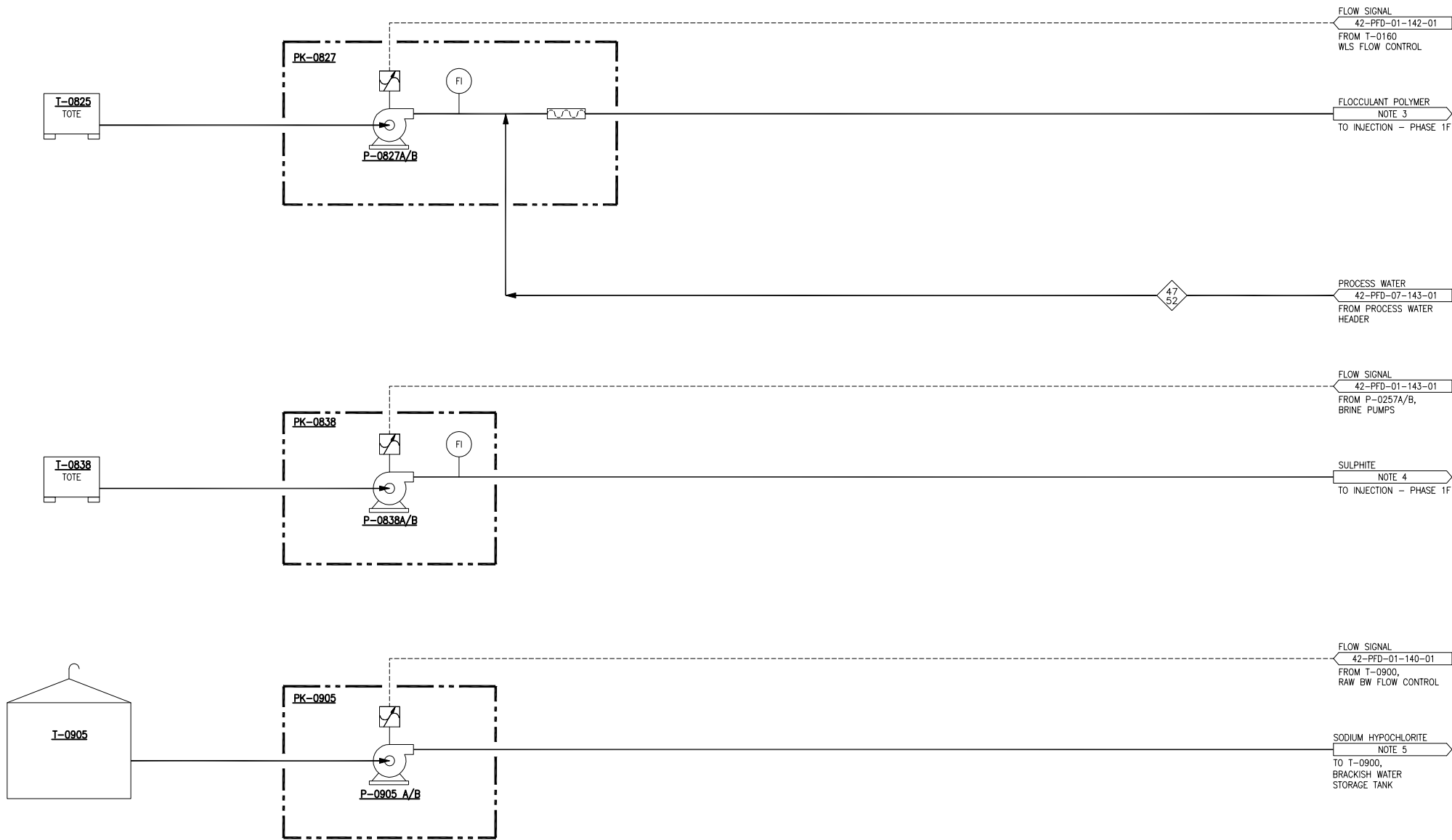
PK-0838
BRINE SULPHITE CHEMICAL
INJECTION PACKAGE

P-0838A/B
BRINE SULFITE PUMPS
RATED FLOW: 0.02 Am3/h

T-0905
SODIUM HYPOCHLORITE TANK
NOMINAL CAPACITY: 5.7 m3

P-0905 A/B
SODIUM HYPOCHLORITE PUMPS
RATED FLOW: 0.027 Am3/h

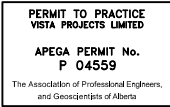
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SODIUM HYPOCHLORITE
INJECTION PACKAGE

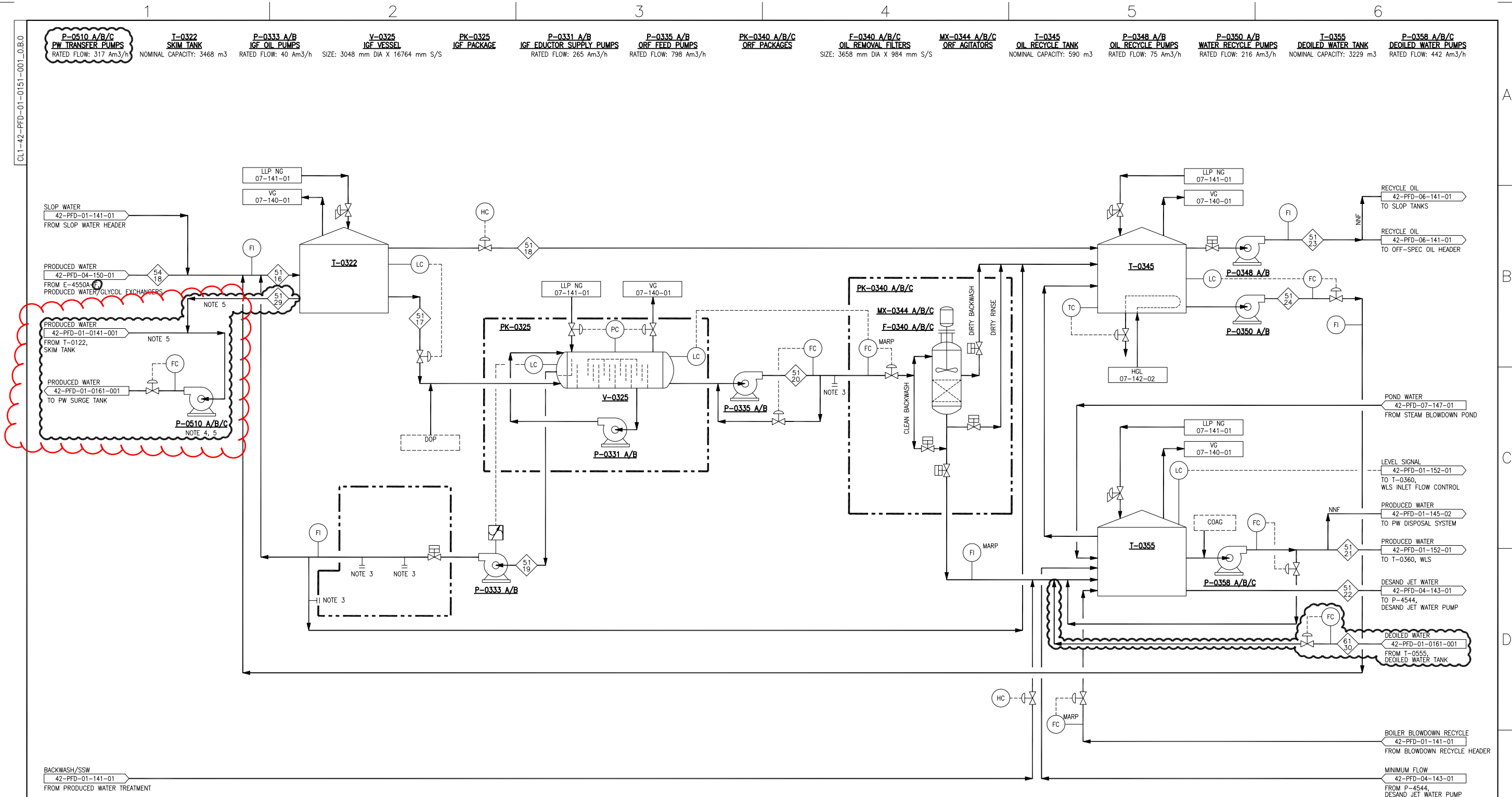


NOTES:

1. ALL EQUIPMENT SHOWN IS PHASE 1F, EXCEPT WHERE NOTED.
2. ALL TAG NUMBERS TO BE PREFIXED BY "CL1-".
3. INJECTION POINT LOCATED ON DWG. CL1G-42-PFD-01-142-01.
4. INJECTION POINT LOCATED ON DWG. CL1G-42-PFD-01-143-01.
5. INJECTION POINT LOCATED ON DWG. CL1G-42-PFD-01-140-01.

PACKAGE NO.

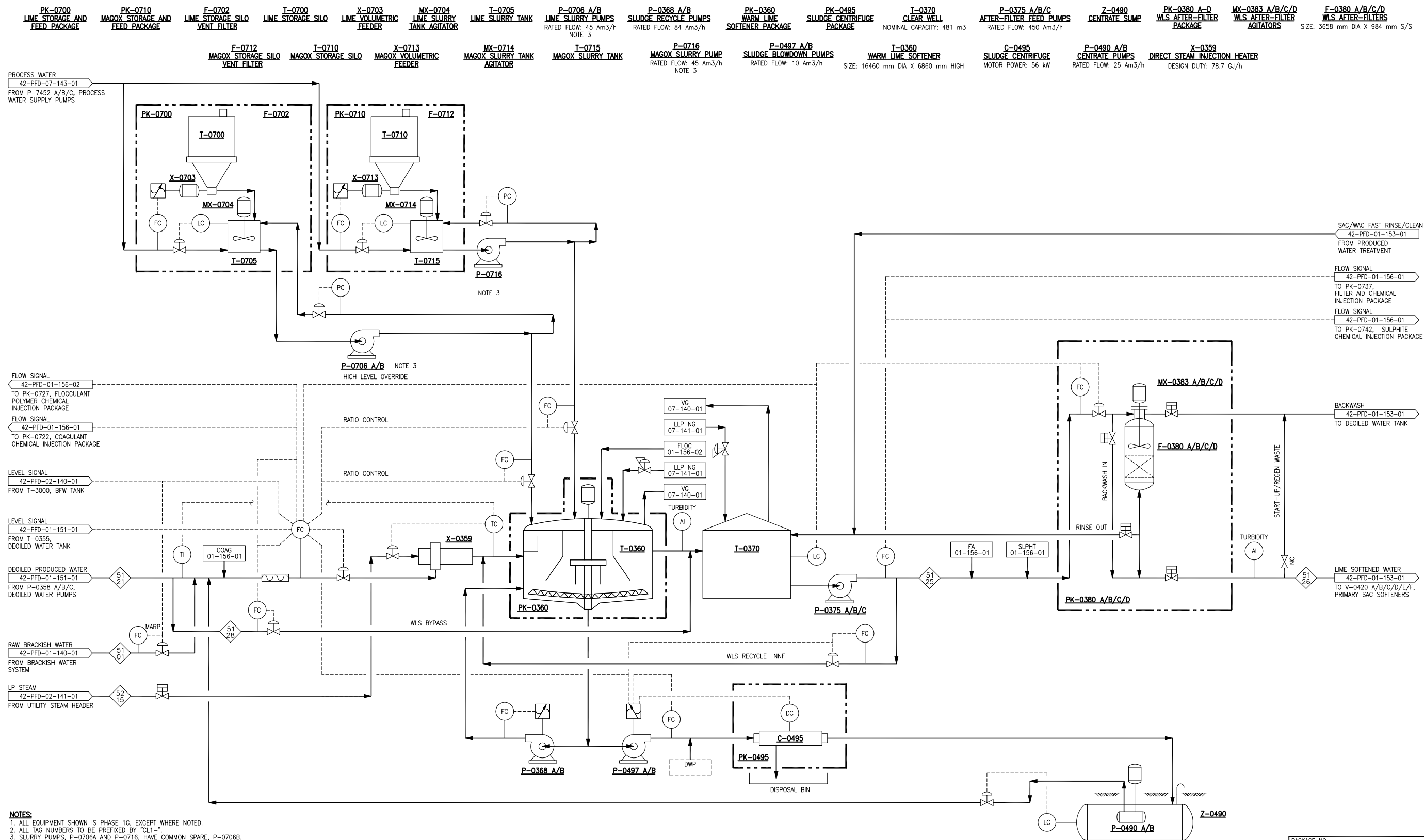
REFERENCE NUMBER	REFERENCE TITLE	STAMPS	REV NO	REVISION	DATE	DRN	CKD	DES	LDE	PE	CONSULTANT NAME AND LOGO	TITLE
		 04/04/2019 	0V	PHASE 1G EXPANSION - ISSUED FOR DESIGN	2013/01/15	KJS	RVG	LY	KU	GP	 REVISION DESCRIPTION ISSUED FOR DESIGN PROJECT NO. CL1H LSD S.E. 1/4, Sec. 17, TWP 76, RG 6, W4M ISSUE DATE 2019/04/05 SCALE NONE	 CHRISTINA LAKE COMMERCIAL PLANT PROCESS FLOW DIAGRAM CHEMICAL INJECTION - AREA 01 PHASE 1F
			1V	PHASE 1G EXPANSION - REISSUED FOR DESIGN	2013/07/23	JM	RVG	LY	KU	MC		
			2V	PHASE 1G EXPANSION - ISSUED FOR PROJECT TURNOVER	2015/06/08	GP	RVG	LY	RVG	FY		
			3.A.0	PHASE 1H EXPANSION - ISSUED FOR DESIGN	2019/04/05	DSH		ZGA	KUL	JEG		
											DRAWING NO.	REVISION NO.
											CL1-42-PFD-01-0146-002	3.A.0



- NOTES:**
1. ALL EQUIPMENT SHOWN IS PHASE 1G EXCEPT WHERE NOTED.
 2. ALL TAG NUMBERS TO BE PREFIXED BY CL1-.
 3. FUTURE TIE-IN POINTS FOR IGF OIL FILTERS.
 4. P-0510A IS DEDICATED TO CL1G SKIM TANK AT SUCTION AND P-0510B IS DEDICATED TO CL1G SKIM TANK AT DISCHARGE. BOTH PUMPS ARE INSTALLED IN PHASE 1G.
 5. P-0510C IS THE COMMON SPARE. PUMP IS INSTALLED IN PHASE 1G.

REFERENCE NUMBER	REFERENCE TITLE	STAMPS	REV NO	REVISION	DATE	DRN	CKD	DES	LDE	PE	CONSULTANT NAME AND LOGO	TITLE
			0V	PHASE 1G EXPANSION - ISSUED FOR DESIGN	2013/01/15	KJS	RVG	LY	KU	GP	Vista Projects	CHRISTINA LAKE COMMERCIAL PLANT
			1V	PHASE 1G EXPANSION - REISSUED FOR DESIGN	2013/07/23	JM	RVG	LY	KU	MC		PROCESS FLOW DIAGRAM
			2V	PHASE 1G EXPANSION - ISSUED FOR PROJECT TURNOVER	2015/06/08	GP	RVG	LY	RVG	FY		PRODUCED WATER DEOILING SYSTEM
			O.B.D	PHASE 1H EXPANSION - ISSUED FOR DESIGN	2019/04/05	DSH	RVG	ZGA	KUL	JEG		PHASE 1G
											REVISION DESCRIPTION ISSUED FOR DESIGN	
											PROJECT NO. CL1H	
											LSD S.E. 1/4, Sec. 17, TWP 76, RG 6, W4M	
											ISSUE DATE 2019/04/05	
											SCALE NONE	
											DRAWING NO. CL1-42-PFD-01-0151-001	
											REVISION NO. O.B.O	

CL1-42-PFD-01-0152-001_O.B.O



REFERENCE NUMBER	REFERENCE TITLE

STAMPS


04/04/2019

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VISTA PROJECTS LIMITED
APEGA PERMIT No.
P 04559
The Association of Professional Engineers,
and Geoscientists of Alberta

REV NO	REVISION	DATE	DRN	CKD	DES	LDE	PE
0V	PHASE 1G EXPANSION - ISSUED FOR DESIGN	2013/01/15	KJS	RVG	LY	KU	GP
1V	PHASE 1G EXPANSION - REISSUED FOR DESIGN	2013/07/23	JM	RVG	LY	KU	MC
2V	PHASE 1G EXPANSION - ISSUED FOR PROJECT TURNOVER	2015/06/08	GP	RVG	LY	RVG	FY
0.B.O	PHASE 1H EXPANSION - ISSUED FOR DESIGN	2019/04/05	DSH	RVG	ZGA	KUL	JEG

CONSULTANT NAME AND LOGO



REVISION DESCRIPTION
ISSUED FOR DESIGN

PROJECT NO.
CL1H

LSD
S.E. 1/4, Sec. 17, TWP 76, RG 6, W4M

ISSUE DATE
2019/04/05

SCALE
NONE

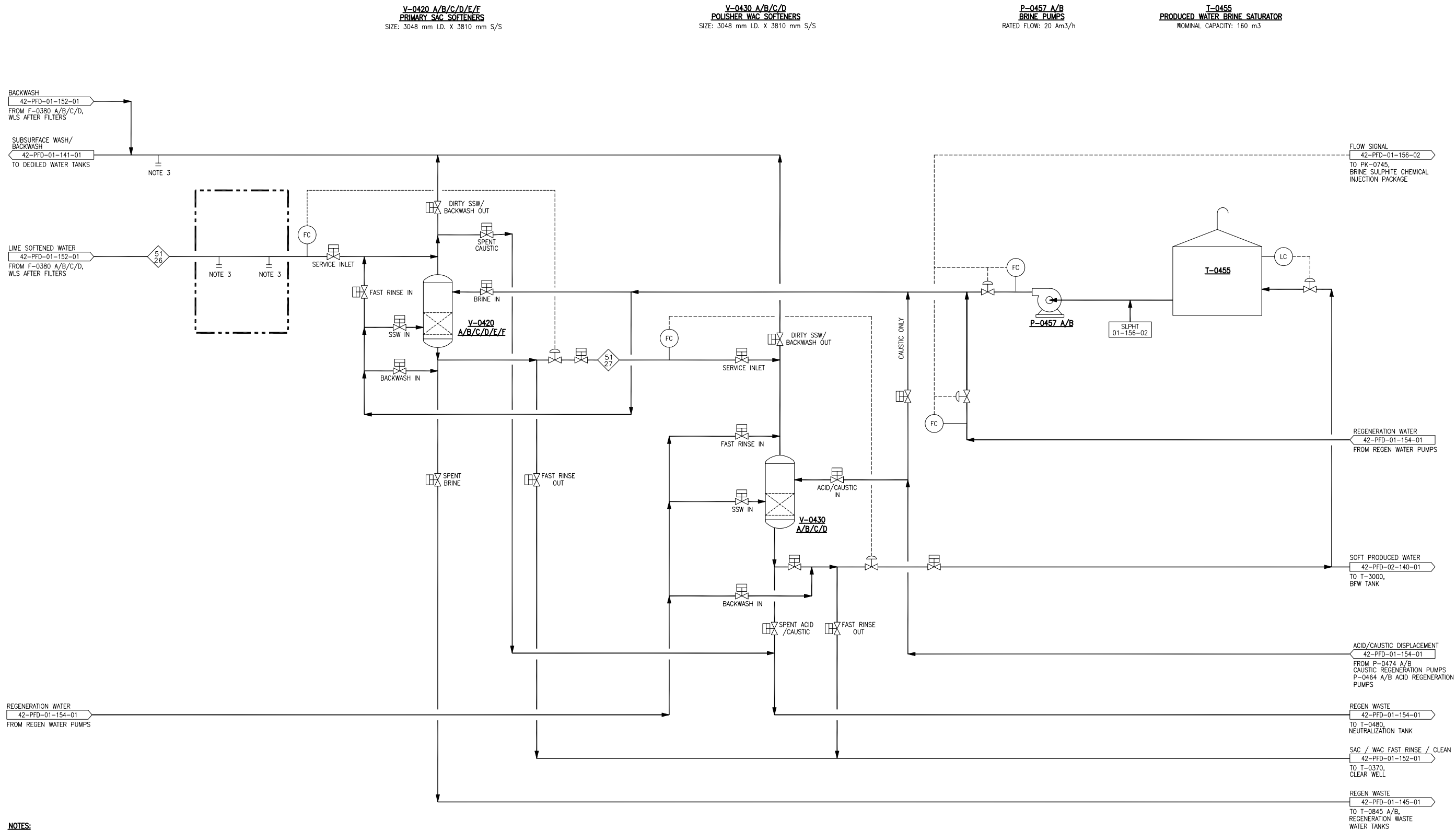
cenovus ENERGY

TITLE
CHRISTINA LAKE COMMERCIAL PLANT
PROCESS FLOW DIAGRAM
WARM LIME SOFTENER SYSTEM
PHASE 1G

DRAWING NO.
CL1-42-PFD-01-0152-001

REVISION NO.
0.B.O

CL1-42-PFD-01-0153-001_O.B.O



- NOTES:
1. ALL EQUIPMENT SHOWN IS PHASE 1G, EXCEPT WHERE NOTED.
 2. ALL TAG NUMBERS TO BE PREFIXED BY CL1-.
 3. FUTURE TIE-IN POINTS FOR SUSPENDED SOLIDS FILTERS.

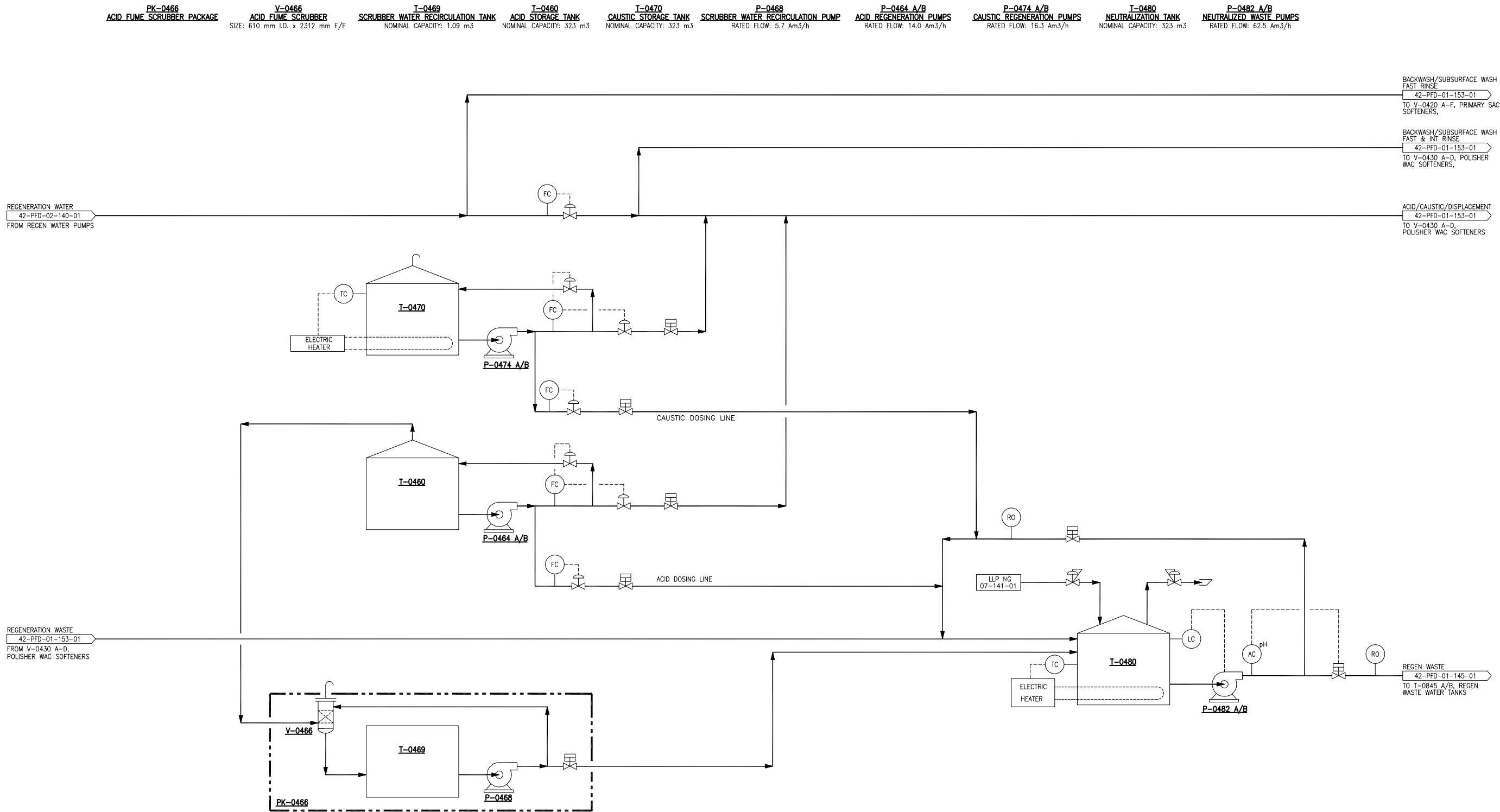
PACKAGE NO.

REFERENCE NUMBER	REFERENCE TITLE	STAMPS	REV. NO	REVISION	DATE	DRN	CKD	DES	LDE	PE	CONSULTANT NAME AND LOGO	TITLE	
		 04/04/2019 PERMIT TO PRACTICE VISTA PROJECTS LIMITED APEGA PERMIT No. P 04559 The Association of Professional Engineers, and Geoscientists of Alberta	0V	PHASE 1G EXPANSION – ISSUED FOR DESIGN	2013/01/15	KJS	RVG	LY	KU	GP	 REVISION DESCRIPTION ISSUED FOR DESIGN PROJECT NO. CL1H LSD S.E. 1/4, Sec. 17, TWP 76, RG 6, W4M ISSUE DATE 2019/04/05 SCALE NONE	cenovus ENERGY CHRISTINA LAKE COMMERCIAL PLANT PROCESS FLOW DIAGRAM WATER TREATMENT (ION EXCHANGE) SYSTEM PHASE 1G DRAWING NO. CL1–42–PFD–01–0153–001 REVISION NO. O.B.O	
			1V	PHASE 1G EXPANSION – REISSUED FOR DESIGN	2013/07/23	JM	RVG	LY	KU	MC			
			2V	PHASE 1G EXPANSION – ISSUED FOR PROJECT TURNOVER	2015/06/08	GP	RVG	LY	RVG	FY			
			O.B.O	PHASE 1H EXPANSION – ISSUED FOR DESIGN	2019/04/05	DSH	RVG	ZGA	KUL	JEG			
				</									



PERMIT TO PRACTICE
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APEGA PERMIT No.
P 04559
The Association of Professional Engineers,
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CL1-42-PFD-01-0154-001_O.B.O



NOTES:
1. ALL EQUIPMENT SHOWN IS PHASE 1G, EXCEPT WHERE NOTED.
2. ALL TAG NUMBERS TO BE PREFIXED BY CL1-.

PACKAGE NO.

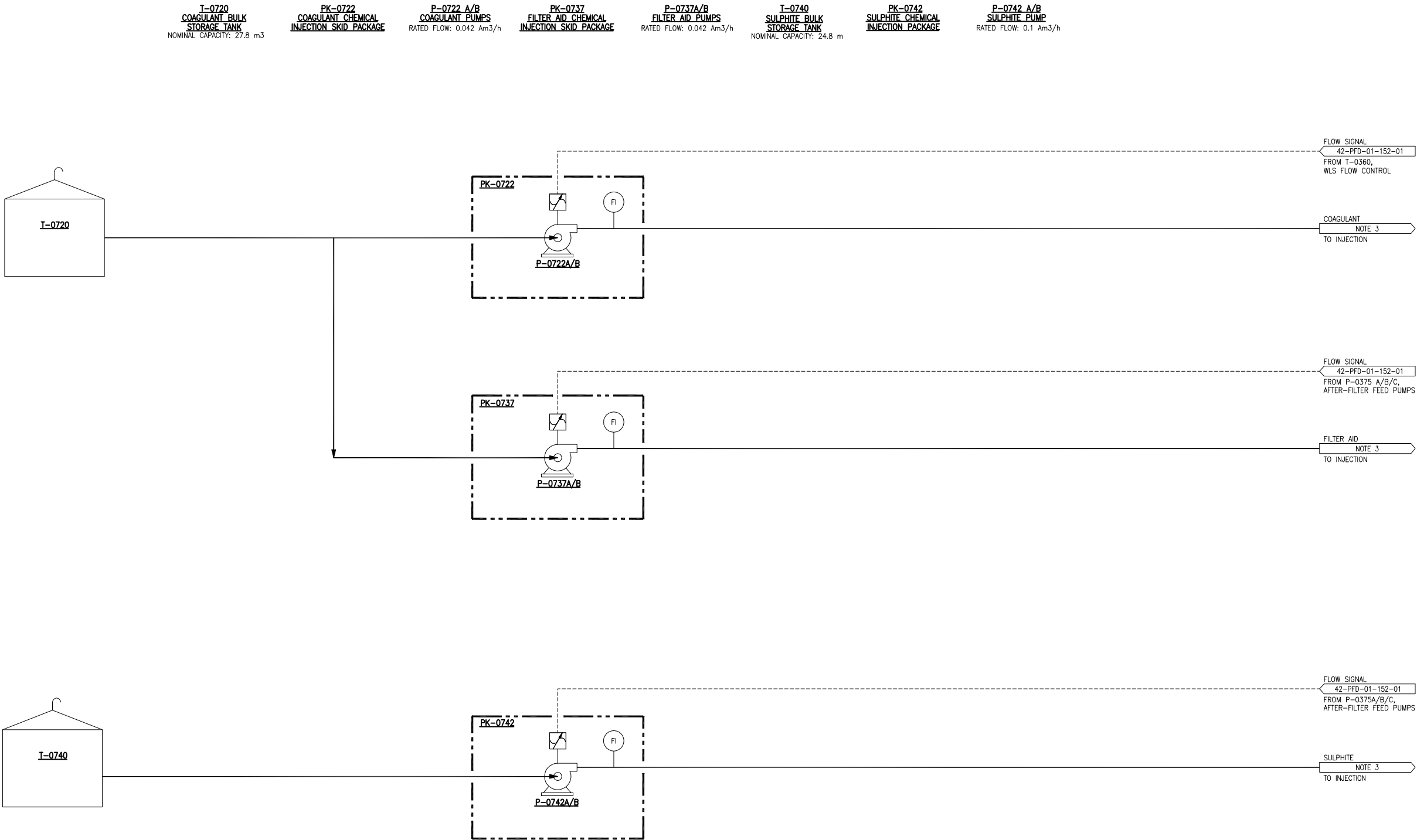
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			1V	PHASE 1G EXPANSION - REISSUED FOR DESIGN	2013/07/23	JM	RVG	LY	KU	MC		
			2V	PHASE 1G EXPANSION - ISSUED FOR PROJECT TURNOVER	2015/06/08	GP	RVG	LY	RVG	FY		
			O.B.O	PHASE 1H EXPANSION - ISSUED FOR DESIGN	2019/04/05	DSH	ZGA	KUL	JEG			
											REVISION DESCRIPTION ISSUED FOR DESIGN	
											PROJECT NO. CL1H	
											LSD S.E. 1/4, Sec. 17, TWP 76, RG 6, W4M	
											ISSUE DATE 2019/04/05	
											SCALE NONE	
											DRAWING NO. CL1-42-PFD-01-0154-001	REVISION NO. O.B.O



04/04/2019

PERMIT TO PRACTICE
VISTA PROJECTS LIMITED
APEGA PERMIT No.
P 04559
The Association of Professional Engineers,
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CL1-42-PFD-01-0156-001_O.B.O



- NOTES:**
1. ALL EQUIPMENT SHOWN IS PHASE 1G, EXCEPT WHERE NOTED.
 2. ALL TAG NUMBERS TO BE PREFIXED BY "CL1-".
 3. INJECTION POINT LOCATED ON DWG. CL1G-42-PFD-01-152-01.

PACKAGE NO.

REFERENCE NUMBER	REFERENCE TITLE	STAMPS	REV NO	REVISION	DATE	DRN	CKD	DES	LDE	PE	CONSULTANT NAME AND LOGO	TITLE
		 04/04/2019	0V	PHASE 1G EXPANSION - ISSUED FOR DESIGN	2013/01/15	KJS	RVG	LY	KU	GP		CHRISTINA LAKE COMMERCIAL PLANT PROCESS FLOW DIAGRAM CHEMICAL INJECTION - AREA 01 PHASE 1G
			1V	PHASE 1G EXPANSION - REISSUED FOR DESIGN	2013/07/23	JM	RVG	LY	KU	MC		
			2V	PHASE 1G EXPANSION - ISSUED FOR PROJECT TURNOVER	2015/06/08	GP	RVG	LY	RVG	FY		
			0.B.O	PHASE 1H EXPANSION - ISSUED FOR DESIGN	2019/04/05	DSH	ZGA	KUL	JEG			
		PERMIT TO PRACTICE VISTA PROJECTS LIMITED APEGA PERMIT No. P 04559 The Association of Professional Engineers and Geoscientists of Alberta									REVISION DESCRIPTION ISSUED FOR DESIGN	DRAWING NO. CL1-42-PFD-01-0156-001 REVISION NO. 0.B.O
											PROJECT NO. CL1H	
											LSD S.E. 1/4, Sec. 17, TWP 76, RG 6, W4M	
											ISSUE DATE 2019/04/05	
											SCALE NONE	

CL1-42-PFD-01-0156-002_O.B.0

T-0725
FLOCCULANT POLYMER TOTE
CAPACITY: 1 m3

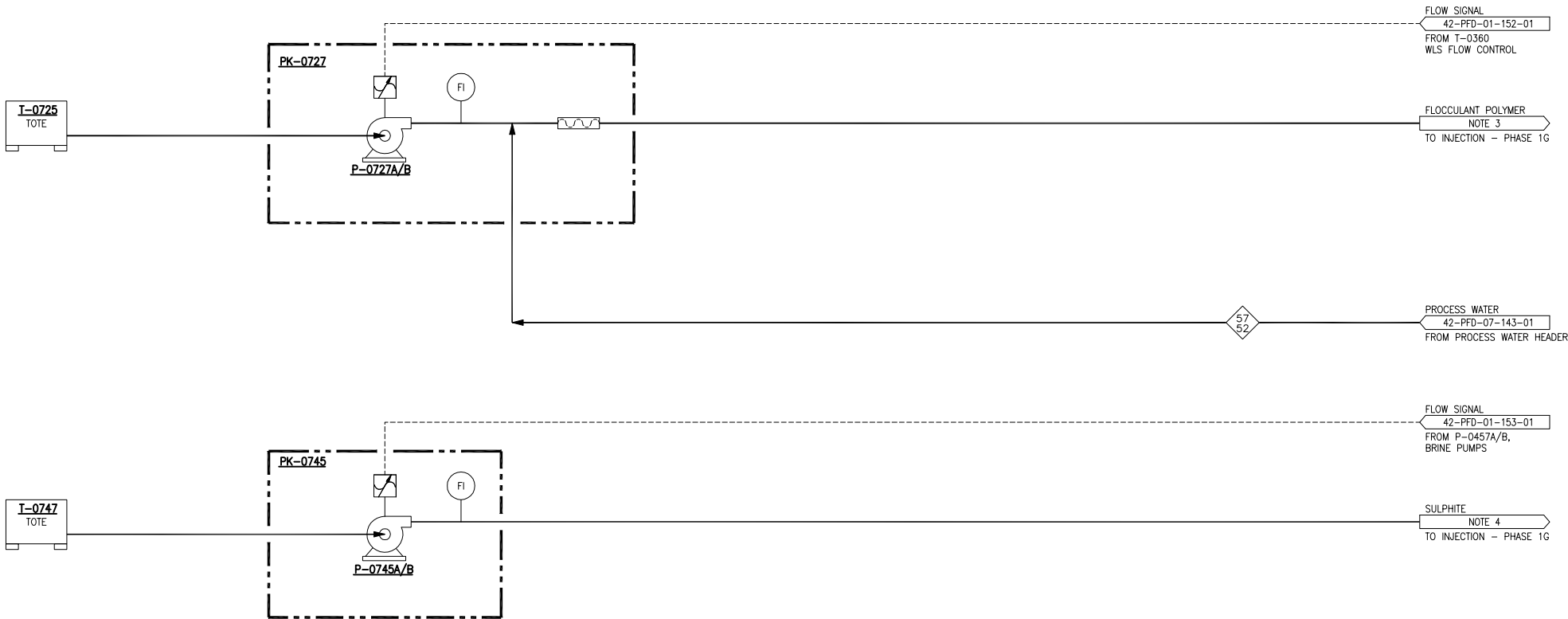
PK-0727
FLOCCULANT POLYMER
CHEMICAL INJECTION
SKID PACKAGE

P-0727A/B
FOCCULANT POLYMER PUMPS
RATED FLOW: 0.002 Am3/h

T-0747
BRINE SULPHITE TOTE TANK
CAPACITY: 1 m3

PK-0745
BRINE SULPHITE CHEMICAL
INJECTION PACKAGE

P-0745A/B
BRINE SULPHITE PUMPS
RATED FLOW: 0.02 Am3/h



NOTES:

1. ALL EQUIPMENT SHOWN IS PHASE 1G, EXCEPT WHERE NOTED.
2. ALL TAG NUMBERS TO BE PREFIXED BY "CL1-".
3. INJECTION POINT LOCATED ON DWG. CL1G-42-PFD-01-152-01.
4. INJECTION POINT LOCATED ON DWG. CL1G-42-PFD-01-153-01.

PACKAGE NO.

REFERENCE NUMBER	REFERENCE TITLE

STAMPS



04/04/2019

PERMIT TO PRACTICE
VISTA PROJECTS LIMITED

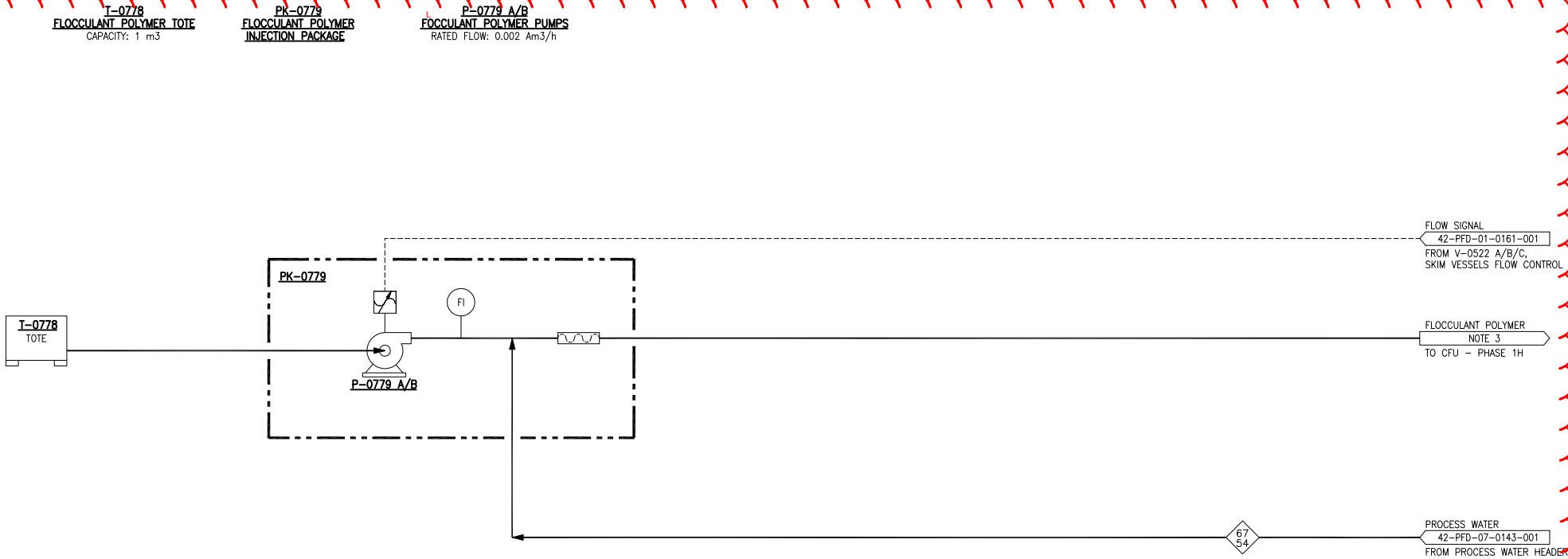
APEGA PERMIT No.
P 04559
The Association of Professional Engineers,
and Geoscientists of Alberta

REV NO	REVISION	DATE	DRN	CKD	DES	LDE	PE
0V	PHASE 1G EXPANSION - ISSUED FOR DESIGN	2013/01/15	KJS	RVG	LY	KU	GP
1V	PHASE 1G EXPANSION - REISSUED FOR DESIGN	2013/07/23	JM	RVG	LY	KU	MC
2V	PHASE 1G EXPANSION - ISSUED FOR PROJECT TURNOVER	2015/06/08	GP	RVG	LY	RVG	FY
0.B.0	PHASE 1H EXPANSION - ISSUED FOR DESIGN	2019/04/05	DSH	ZGA	KUL	JEG	

CONSULTANT NAME AND LOGO	
REVISION DESCRIPTION ISSUED FOR DESIGN	
PROJECT NO. CL1H	
LSD S.E. 1/4, Sec. 17, TWP 76, RG 6, W4M	
ISSUE DATE 2019/04/05	SCALE NONE

cenovus ENERGY	
TITLE CHRISTINA LAKE COMMERCIAL PLANT PROCESS FLOW DIAGRAM CHEMICAL INJECTION - AREA 01 PHASE 1G	
DRAWING NO. CL1-42-PFD-01-0156-002	REVISION NO. 0.B.0

CL1-42-PFD-01-0161-002_O.A.0



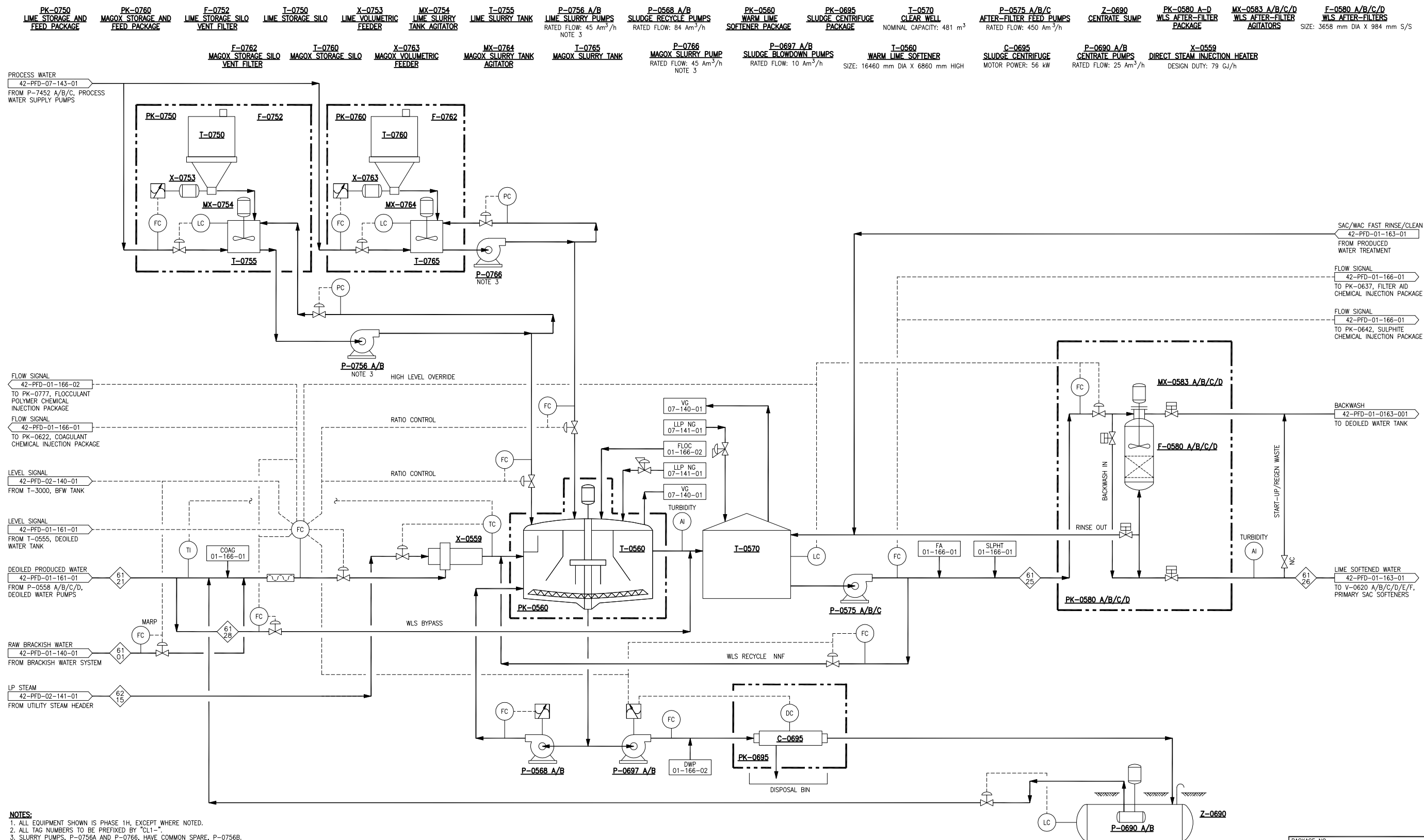
NOTES:

- 1. ALL EQUIPMENT SHOWN IS PHASE 1H, EXCEPT WHERE NOTED.
- 2. ALL TAG NUMBERS TO BE PREFIXED BY "CL1-".
- 3. INJECTION POINT LOCATED ON DWG. CL1-42-PFD-01-0161-001.

PACKAGE NO.

REFERENCE NUMBER	REFERENCE TITLE	STAMPS	REV NO	REVISION	DATE	DRN	CKD	DES	LDE	PE	CONSULTANT NAME AND LOGO	TITLE	
		 04/04/2019 PERMIT TO PRACTICE VISTA PROJECTS LIMITED APEGA PERMIT No. P 04559 The Association of Professional Engineers, and Geoscientists of Alberta	O.A.O	PHASE 1H EXPANSION – ISSUED FOR DESIGN	2019/04/05	DSH	PVC	ZGA	KUL	JEG		CHRISTINA LAKE COMMERCIAL PLANT PROCESS FLOW DIAGRAM CHEMICAL INJECTION – CFU PHASE 1H	
											</		

CL1-42-PFD-01-0162-001_O.A.O



REFERENCE NUMBER	REFERENCE TITLE

STAMPS



04/04/2019

PERMIT TO PRACTICE
VISTA PROJECTS LIMITED
APEGA PERMIT No.
P 04559
The Association of Professional Engineers,
and Geoscientists of Alberta

REV NO	REVISION	DATE	DRN	CKD	DES	LDE	PE
VB	PHASE 1H EXPANSION - REISSUED FOR REGULATORY APPROVAL	2012/07/25	IS	APC	LY	KUL	BZS
O.A.O	PHASE 1H EXPANSION - ISSUED FOR DESIGN	2019/04/05	DSH	ZGA	KUL	JEG	JEG

CONSULTANT NAME AND LOGO



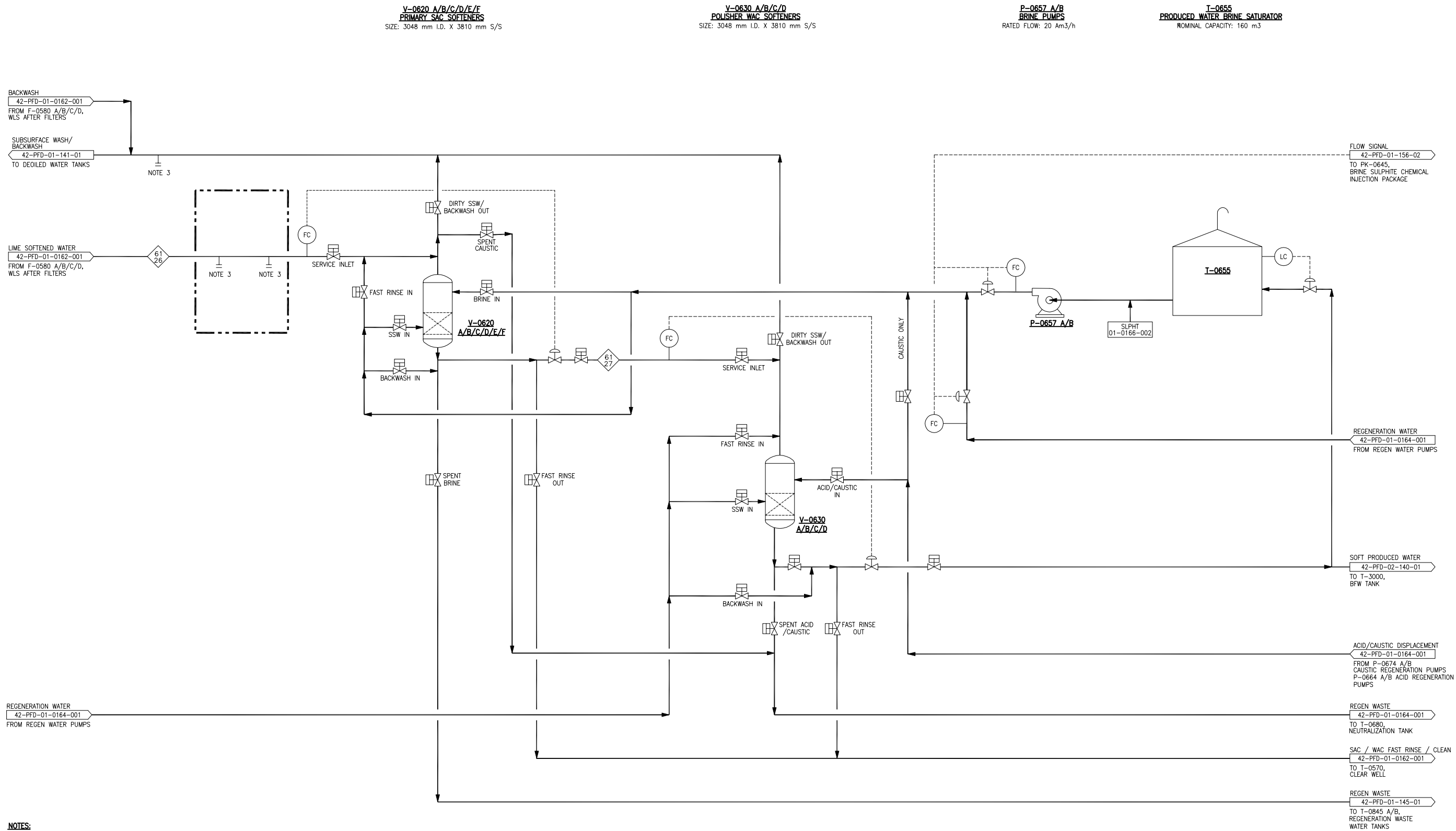
REVISION DESCRIPTION
ISSUED FOR DESIGN
PROJECT NO.
CL1H
LSD
S.E. 1/4, Sec. 17, TWP 76, RG 6, W4M
ISSUE DATE
2019/04/05
SCALE
NONE

cenovus ENERGY

TITLE
CHRISTINA LAKE COMMERCIAL PLANT
PROCESS FLOW DIAGRAM
WARM LIME SOFTENER SYSTEM
PHASE 1H

DRAWING NO.
CL1-42-PFD-01-0162-001
REVISION NO.
O.A.O

CL1-42-PFD-01-0163-001_O.A.0



- NOTES:**
1. ALL EQUIPMENT SHOWN IS PHASE 1H, EXCEPT WHERE NOTED.
 2. ALL TAG NUMBERS TO BE PREFIXED BY CL1-.
 3. FUTURE TIE-IN POINTS FOR SUSPENDED SOLIDS FILTERS.

PACKAGE NO.

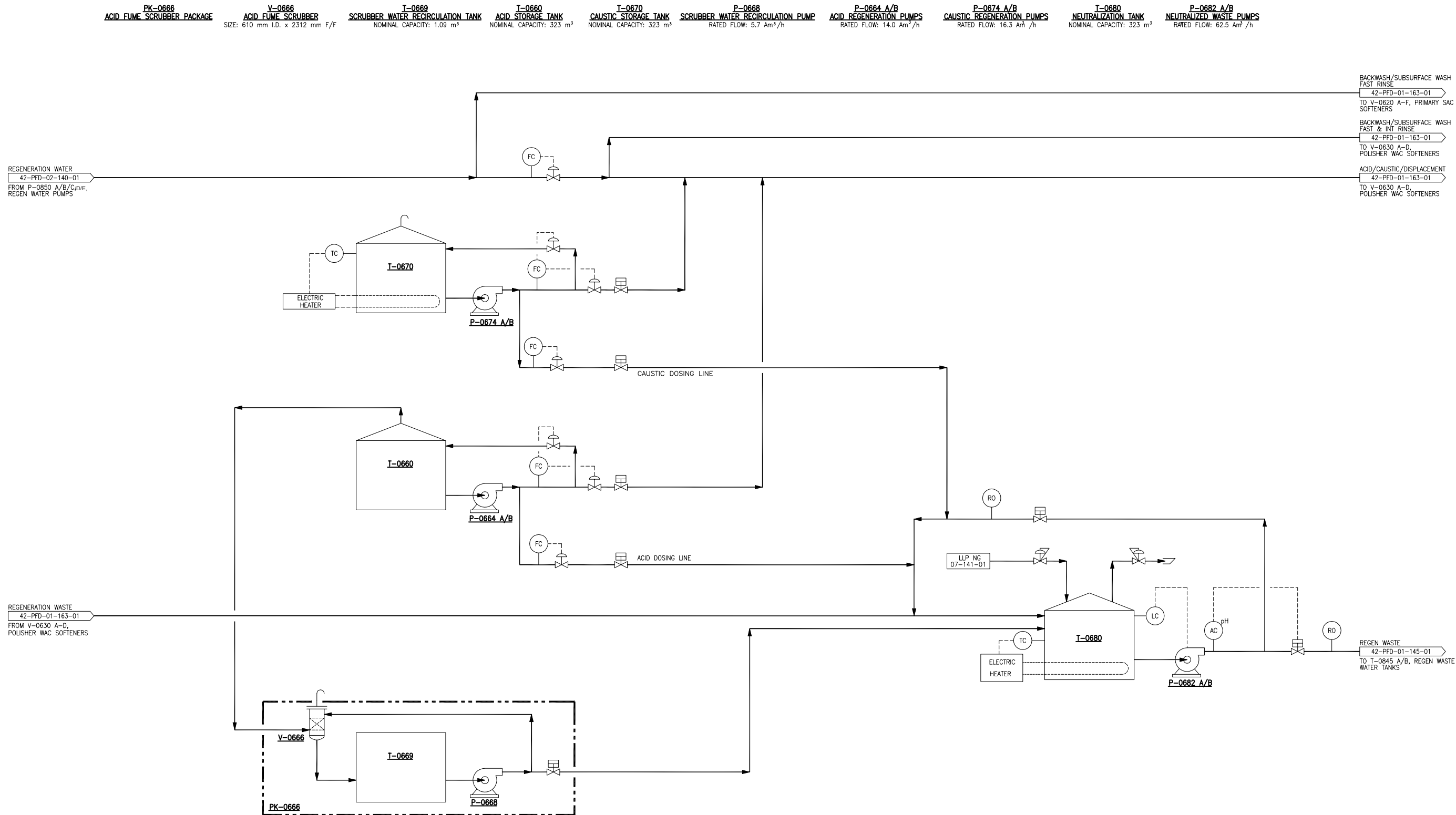
REFERENCE NUMBER	REFERENCE TITLE	STAMPS	REV NO	REVISION	DATE	DRN	CKD	DES	LDE	PE	CONSULTANT NAME AND LOGO	TITLE	
		 04/04/2019	VB	PHASE 1H EXPANSION – REISSUED FOR REGULATORY APPROVAL		IS						CHRISTINA LAKE COMMERCIAL PLANT PROCESS FLOW DIAGRAM WATER TREATMENT (ION EXCHANGE) SYSTEM PHASE 1H	
			O.A.0	PHASE 1H EXPANSION – ISSUED FOR DESIGN	2019/04/05	DSH	Rv	ZGA	KUL	JEG			REVISION DESCRIPTION ISSUED FOR DESIGN
													PROJECT NO. CL1H
													LSD S.E. 1/4, Sec. 17, TWP 76, RG 6, W4M
													ISSUE DATE 2019/04/05
												DRAWING NO. CL1–42–PFD–01–0163–001	REVISION NO. O.A.0



04/04/2019

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CL1-42-PFD-01-0164-001_O.A.O



PACKAGE NO.

REFERENCE NUMBER	REFERENCE TITLE	STAMPS	REV NO	REVISION	DATE	DRN	CKD	DES	LDE	PE	CONSULTANT NAME AND LOGO	TITLE	DRAWING NO.	REVISION NO.
			VB	PHASE 1H EXPANSION - REISSUED FOR REGULATORY APPROVAL	2012/07/25	IS	APC	LY	KUL	BZS		CHRISTINA LAKE COMMERCIAL PLANT PROCESS FLOW DIAGRAM ACID/CAUSTIC/NEUTRALIZATION SYSTEM PHASE 1H	CL1-42-PFD-01-0164-001	O.A.O
			O.A.O	PHASE 1H EXPANSION - ISSUED FOR DESIGN	2019/04/05	DSH	PWC	ZGA	KUL	JEG				
											REVISION DESCRIPTION ISSUED FOR DESIGN			
											PROJECT NO. CL1H			
											LSD S.E. 1/4, Sec. 17, TWP 76, RG 6, W4M			
											ISSUE DATE 2019/04/05	SCALE NONE		



04/04/2019

PERMIT TO PRACTICE
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APEGA PERMIT No.
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The Association of Professional Engineers,
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CL1-42-PFD-01-0166-001_O.A.O

T-0620
COAGULANT BULK
STORAGE TANK
NOMINAL CAPACITY: 27.8 m³

PK-0622
COAGULANT CHEMICAL
INJECTION SKID PACKAGE

P-0622 A/B
COAGULANT PUMPS
RATED FLOW: 0.042 Am³/h

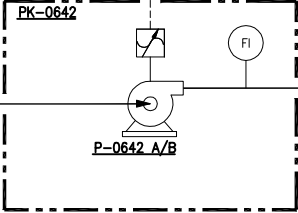
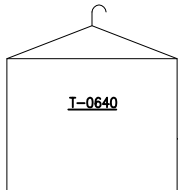
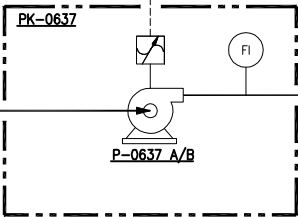
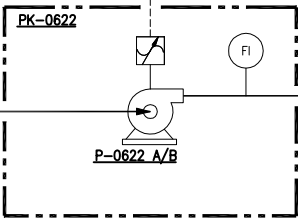
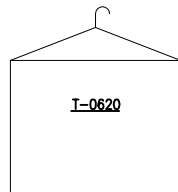
PK-0637
FILTER AID CHEMICAL
INJECTION SKID PACKAGE

P-0637 A/B
FILTER AID PUMPS
RATED FLOW: 0.042 Am³/h

T-0640
SULPHITE BULK
STORAGE TANK
NOMINAL CAPACITY: 24.8 m³

PK-0642
SULPHITE CHEMICAL
INJECTION PACKAGE

P-0642 A/B
SULPHITE PUMP
RATED FLOW: 0.1 Am³/h



FLOW SIGNAL
42-PFD-01-162-01
FROM T-0560,
WLS FLOW CONTROL

COAGULANT
NOTE 3
TO INJECTION

FLOW SIGNAL
42-PFD-01-162-01
FROM P-0575 A/B/C,
AFTER-FILTER FEED PUMPS

FILTER AID
NOTE 3
TO INJECTION

FLOW SIGNAL
42-PFD-01-0162-001
FROM P-0575A/B/C
AFTER-FILTER FEED PUMPS

SULPHITE
NOTE 3
TO INJECTION

- NOTES:
1. ALL EQUIPMENT SHOWN IS PHASE 1H, EXCEPT WHERE NOTED.
 2. ALL TAG NUMBERS TO BE PREFIXED BY "CL1-".
 3. INJECTION POINT LOCATED ON DWG. CL1H-42-PFD-01-162-01.

PACKAGE NO.

REFERENCE NUMBER	REFERENCE TITLE

STAMPS



04/04/2019

PERMIT TO PRACTICE
VISTA PROJECTS LIMITED
APEGA PERMIT No.
P 04559
The Association of Professional Engineers,
and Geoscientists of Alberta

REV NO	REVISION	DATE	DRN	CKD	DES	LDE	PE
VB	PHASE 1H EXPANSION - REISSUED FOR REGULATORY APPROVAL	2012/07/25	DI	APC	LY	KUL	BZS
O.A.O	PHASE 1H EXPANSION - ISSUED FOR DESIGN	2019/04/05	DSH	ZGA	KUL	JEG	LSD

CONSULTANT NAME AND LOGO

REVISION DESCRIPTION
ISSUED FOR DESIGN

PROJECT NO.
CL1H

LSD
S.E. 1/4, Sec. 17, TWP 76, RG 6, W4M

ISSUE DATE
2019/04/05

SCALE
NONE

TITLE
CHRISTINA LAKE COMMERCIAL PLANT
PROCESS FLOW DIAGRAM
CHEMICAL INJECTION - AREA 01
PHASE 1H

DRAWING NO.
CL1-42-PFD-01-0166-001

REVISION NO.
O.A.O

CL1-42-PFD-01-0166-002_O.A.1

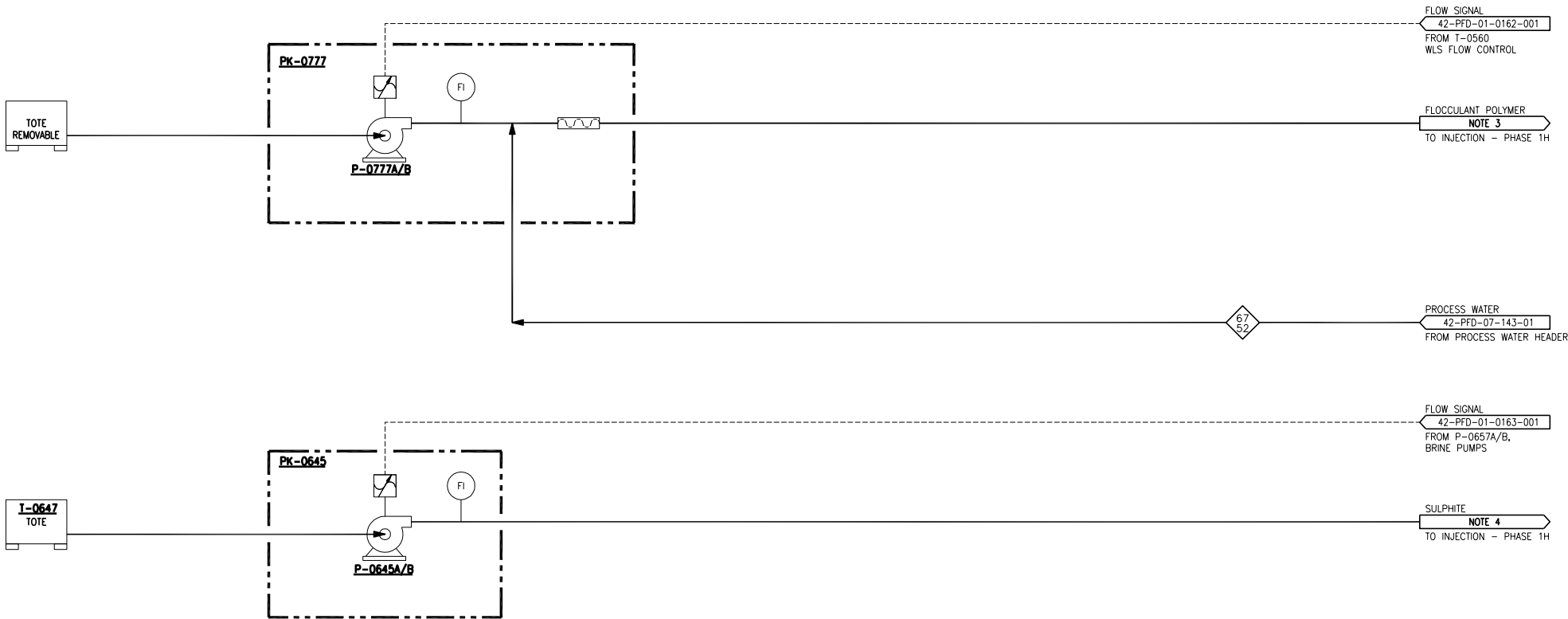
PK-0777
FLOCCULANT POLYMER
INJECTION PACKAGE

P-0777A/B
FLOCCULANT POLYMER PUMPS
RATED FLOW: 0.0044 Am3/h

T-0647
BRINE SULPHITE TOTE TANK
CAPACITY: 1 m3

PK-0645
BRINE SULPHITE CHEMICAL
INJECTION PACKAGE

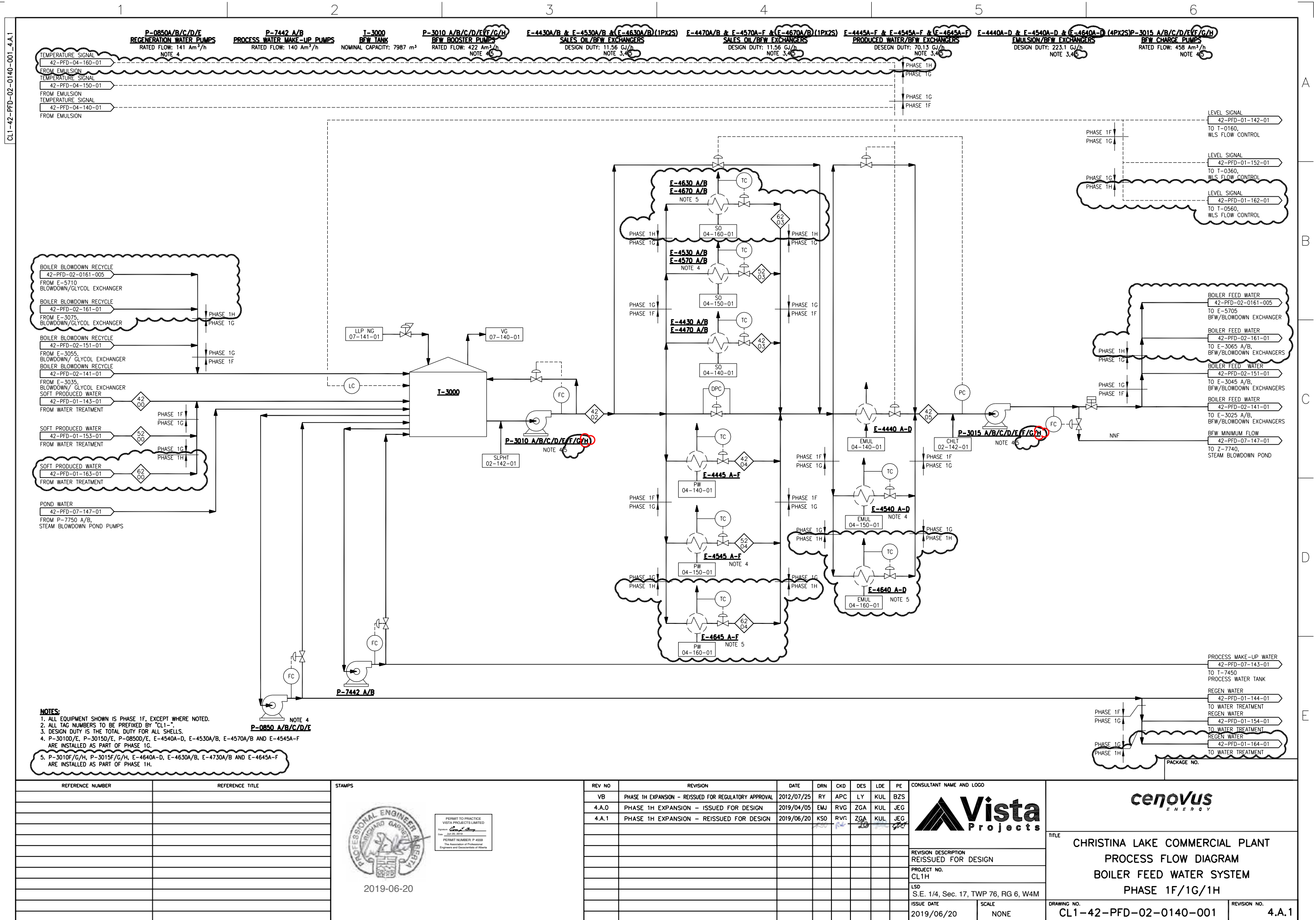
P-0645A/B
BRINE SULPHITE PUMPS
RATED FLOW: 0.02 Am3/h



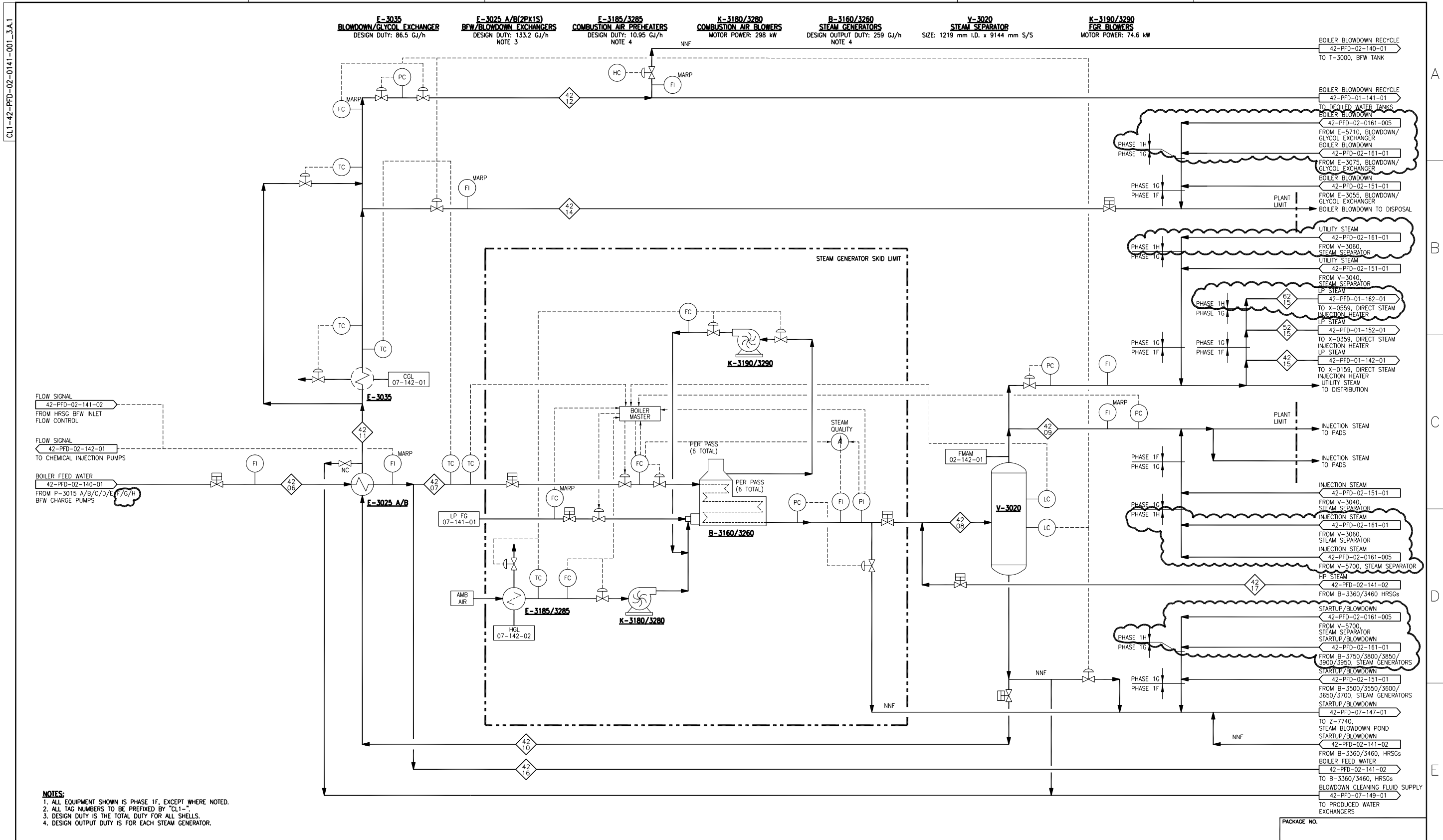
- NOTES:**
1. ALL EQUIPMENT SHOWN IS PHASE 1H, EXCEPT WHERE NOTED.
 2. ALL TAG NUMBERS TO BE PREFIXED BY "CL1-".
 3. INJECTION POINT LOCATED ON DWG. CL1G-42-PFD-01-162-01.
 4. INJECTION POINT LOCATED ON DWG. CL1G-42-PFD-01-163-01.

PACKAGE NO.

REFERENCE NUMBER	REFERENCE TITLE	STAMPS	REV NO	REVISION	DATE	DRN	CKD	DES	LDE	PE	CONSULTANT NAME AND LOGO	TITLE	
		 2019-06-11 PERMIT TO PRACTICE VISTA PROJECTS LIMITED  2019-06-11 PERMIT NUMBER: P-4559 The Association of Professional Engineers and Geoscientists of Alberta	VB	PHASE 1H EXPANSION - REISSUED FOR REGULATORY APPROVAL		RY						 CHRISTINA LAKE COMMERCIAL PLANT PROCESS FLOW DIAGRAM CHEMICAL INJECTION - AREA 01 PHASE 1H	
			O.A.0	PHASE 1H EXPANSION - ISSUED FOR DESIGN	2019/04/05	DSH	RVG	ZGA	KUL	JEG			
			O.A.1	PHASE 1H EXPANSION - REISSUED FOR DESIGN	2019/06/11	KSO	RVG	ZGA	KUL	JEG			
											REVISION DESCRIPTION REISSUED FOR DESIGN	DRAWING NO. CL1-42-PFD-01-0166-002	
											PROJECT NO. CL1H		REVISION NO. O.A.1
											LSD S.E. 1/4, Sec. 17, TWP 76, RG 6, W4M		
											ISSUE DATE 2019/06/11		
											SCALE NONE		



CL1-42-PFD-02-0141-001_3.A.1



- NOTES:**
1. ALL EQUIPMENT SHOWN IS PHASE 1F, EXCEPT WHERE NOTED.
 2. ALL TAG NUMBERS TO BE PREFIXED BY "CL1-".
 3. DESIGN DUTY IS THE TOTAL DUTY FOR ALL SHELLS.
 4. DESIGN OUTPUT DUTY IS FOR EACH STEAM GENERATOR.

REFERENCE NUMBER	REFERENCE TITLE

STAMPS



2019-06-11

PERMIT TO PRACTICE
VISTA PROJECTS LIMITED

Signature: 
Date: Jan 13, 2019
PC/MT/NT NUMBER: P-4559
The Association of Professional Engineers and Geoscientists of Alberta

REV NO	REVISION	DATE	DRN	CKD	DES	LDE	PE
VB	PHASE 1H EXPANSION - REISSUED FOR REGULATORY APPROVAL	2012/07/25	RY	APC	LY	KUL	BZS
3.A.0	PHASE 1H EXPANSION - ISSUED FOR DESIGN	2019/04/05	EMJ	RVG	ZGA	KUL	JEG
3.A.1	PHASE 1H EXPANSION - REISSUED FOR DESIGN	2019/06/11	KSO	RVG	ZGA	KUL	JEG

CONSULTANT NAME AND LOGO



REVISION DESCRIPTION
REISSUED FOR DESIGN

PROJECT NO.
CL1H

LSD
S.E. 1/4, Sec. 17, TWP 76, RG 6, W4M

ISSUE DATE
2019/06/11

SCALE
NONE

cenovus
ENERGY

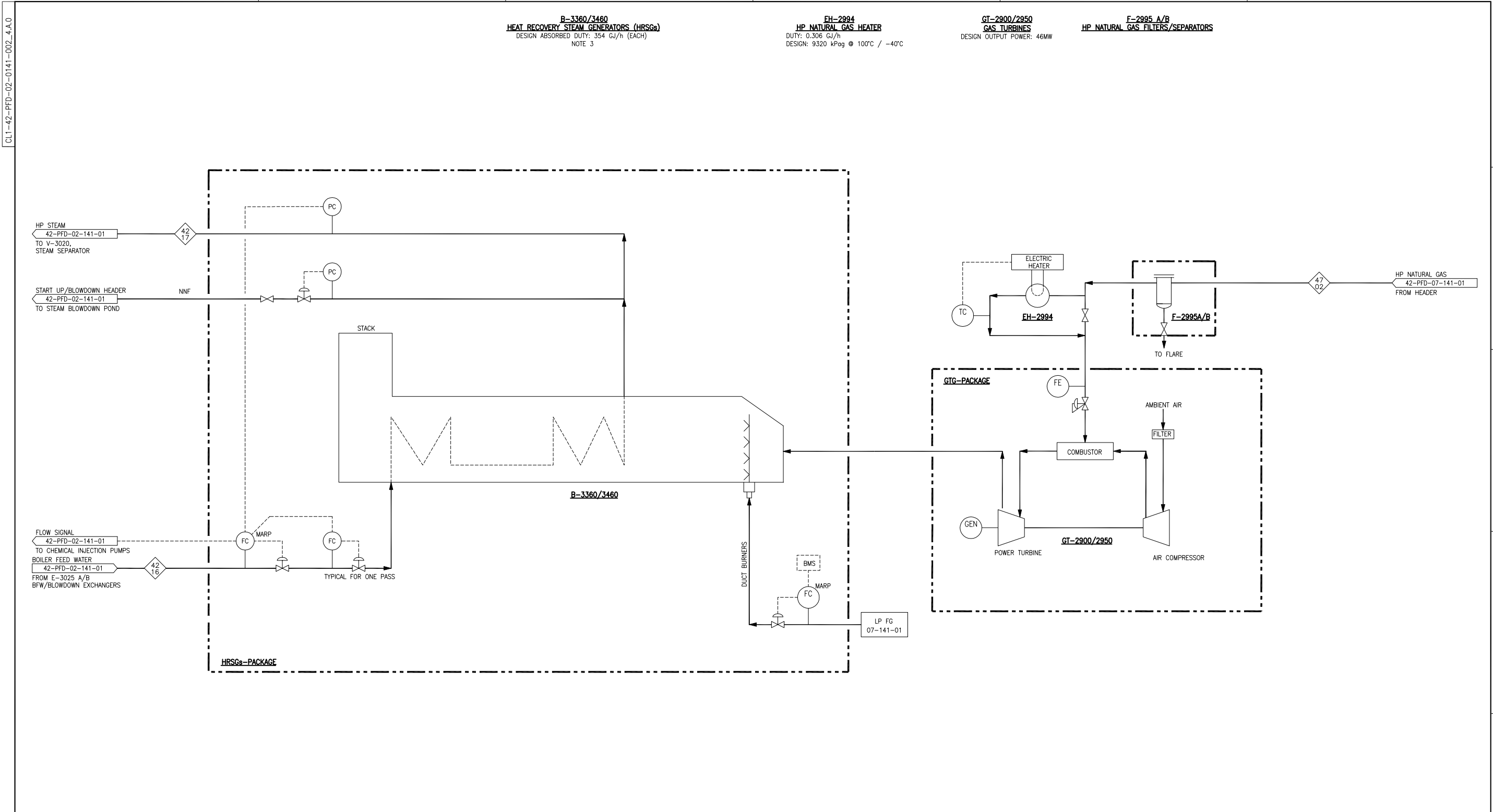
TITLE
CHRISTINA LAKE COMMERCIAL PLANT
PROCESS FLOW DIAGRAM
STEAM GENERATION SYSTEM (OTSG)
PHASE 1F/1G/1H

DRAWING NO.
CL1-42-PFD-02-0141-001

REVISION NO.
3.A.1

CL1-42-PFD-02-0141-002_4.A.0

K:\Projects\Cenovus\2195\Piping\Drafting\PFD\01 - IFR - (IN PROGRESS)\CL1-42-PFD-02-0141-002_4.A.0.dwg Ken Sorensen 4/3/2019 11:23 AM



REFERENCE NUMBER		REFERENCE TITLE		 04/04/2019 PERMIT TO PRACTICE VISTA PROJECTS LIMITED APEGA PERMIT No. P 04559 The Association of Professional Engineers, and Geoscientists of Alberta		REV NO		REVISION		DATE		DRN		CKD		DES		LDE		PE				CONSULTANT NAME AND LOGO				TITLE CHRISTINA LAKE COMMERCIAL PLANT PROCESS FLOW DIAGRAM STEAM GENERATION SYSTEM (COGENERATION) PHASE 1F		DRAWING NO. CL1-42-PFD-02-0141-002		REVISION NO. 4.A.0	
0V		PHASE 1G EXPANSION – ISSUED FOR DESIGN				2013/01/15		KJS		RVG		LY		KU		GP																	
1V		PHASE 1G EXPANSION – REISSUED FOR DESIGN				2013/07/23		JM		RVG		LY		KU		MC																	
2V		PHASE 1G EXPANSION – ISSUED FOR PROJECT TURNOVER				2015/05/08		GP		RVG		LY		RVG		FY																	
4.A.0		PHASE 1H EXPANSION – ISSUED FOR DESIGN				2019/04/05		EMJ		RVG		ZGA		KUL		JEG																	

CL1-42-PFD-02-0142-001_3.A.1

T-3084
FILMING AMINE STORAGE TANK
NOMINAL CAPACITY: 5.9 m³

PK-3085
FILMING AMINE CHEMICAL PACKAGE

P-3085
FILMING AMINE INJECTION PUMPS
RATED FLOW: 0.01 Am³/h

T-3086
SULPHITE STORAGE TANK
NOMINAL CAPACITY: 122 m³

PK-3087
SULPHITE CHEMICAL INJECTION SKID PACKAGE

P-3087A/B
SULPHITE INJECTION PUMPS
RATED FLOW: 0.125 Am³/h

T-3088
CHELANT STORAGE TANK
NOMINAL CAPACITY: 16.69 m³

PK-3089
CHELANT INJECTION PACKAGE

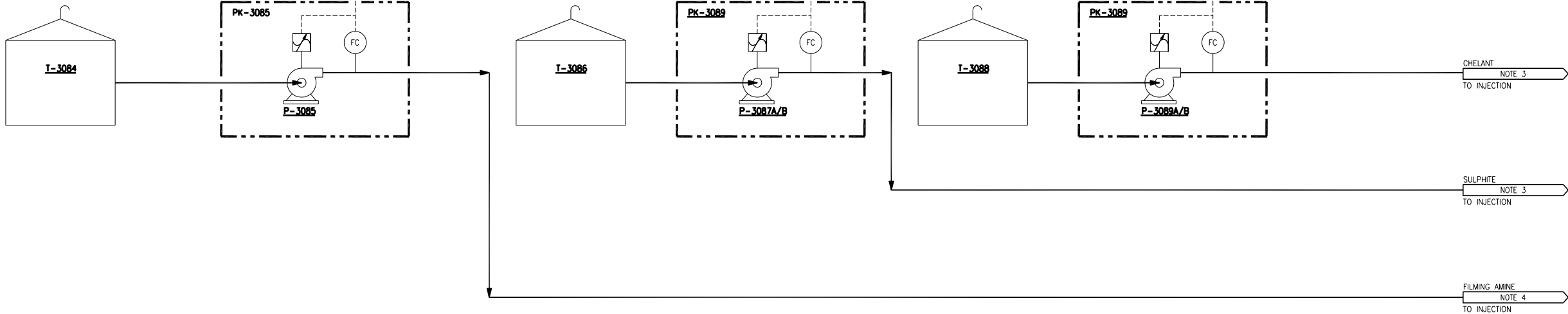
P-3089A/B
CHELANT INJECTION PUMPS
RATED FLOW: 0.02 Am³/h

FLOW SIGNAL
42-PFD-02-161-01
FROM TOTAL BFW FLOW METER

FLOW SIGNAL
42-PFD-02-151-01
FROM TOTAL BFW FLOW METER

FLOW SIGNAL
42-PFD-02-152-01
TO CHEMICAL INJECTION PUMP

FLOW SIGNAL
42-PFD-02-141-01
FROM TOTAL BFW FLOW METER



- NOTES:**
1. ALL EQUIPMENT SHOWN IS PHASE 1F EXCEPT WHERE NOTED.
 2. ALL TAG NUMBERS TO BE PREFIXED BY "CL1-".
 3. INJECTION POINT LOCATED ON DWG. CL1H-42-PFD-02-140-01.
 4. INJECTION POINT LOCATED ON DWG. CL1H-42-PFD-02-141-01.

PACKAGE NO.

REFERENCE NUMBER	REFERENCE TITLE



2019-06-11

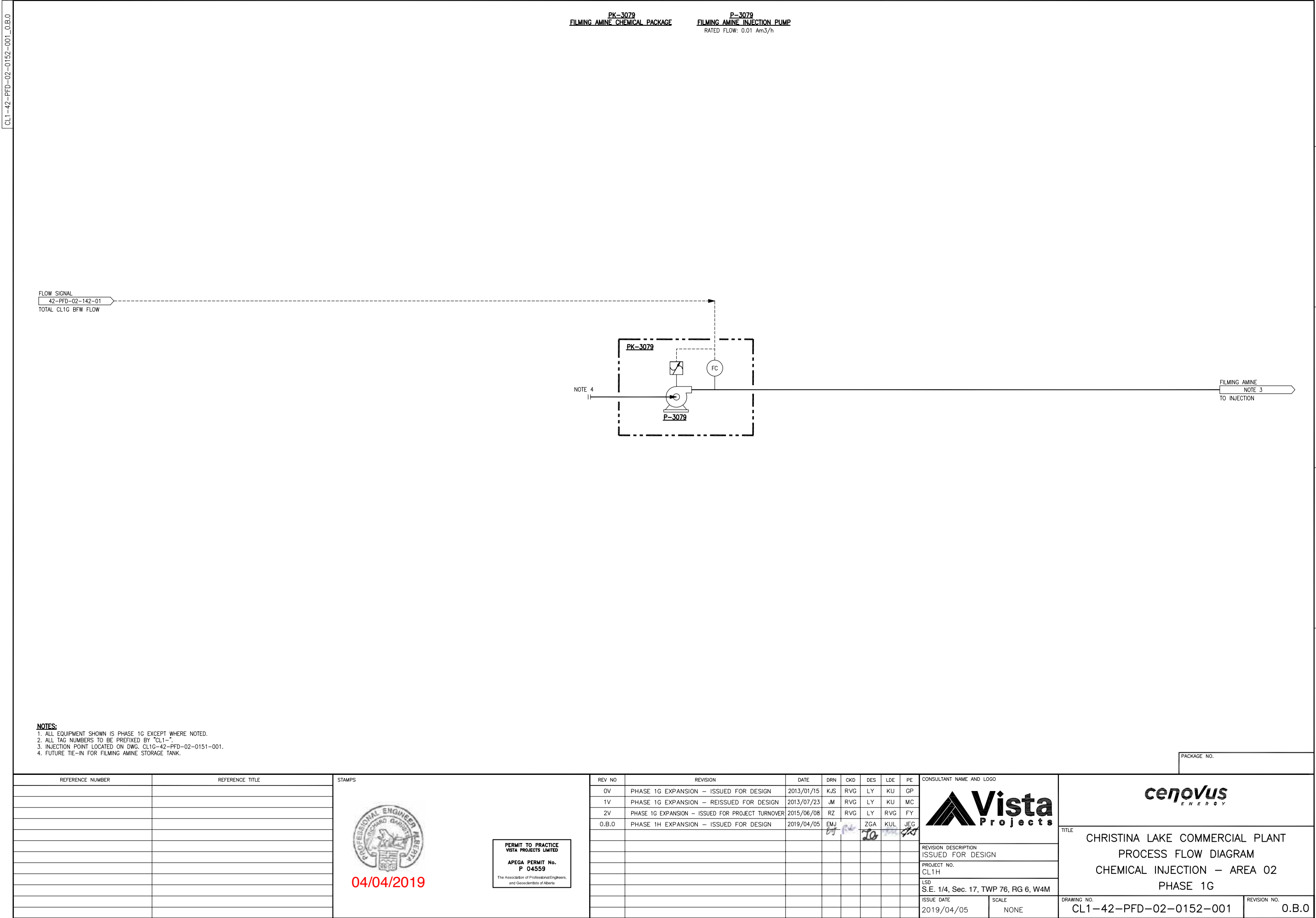
PERMIT TO PRACTICE
VISTA PROJECTS LIMITED
Signature:
Date: Jun 13, 2019
PERMIT NUMBER: P-4559
The Association of Professional
Engineers and Geoscientists of Alberta

REV NO	REVISION	DATE	DRN	CKD	DES	LDE	PE
VB	PHASE 1H EXPANSION - REISSUED FOR REGULATORY APPROVAL	2012/07/25	RY	APC	LY	KUL	BZS
3.A.0	PHASE 1H EXPANSION - ISSUED FOR DESIGN	2019/04/05	EMJ	RVG	ZGA	KUL	JEG
3.A.1	PHASE 1H EXPANSION - REISSUED FOR DESIGN	2019/06/11	KSO	RVG	ZGA	KUL	JEG

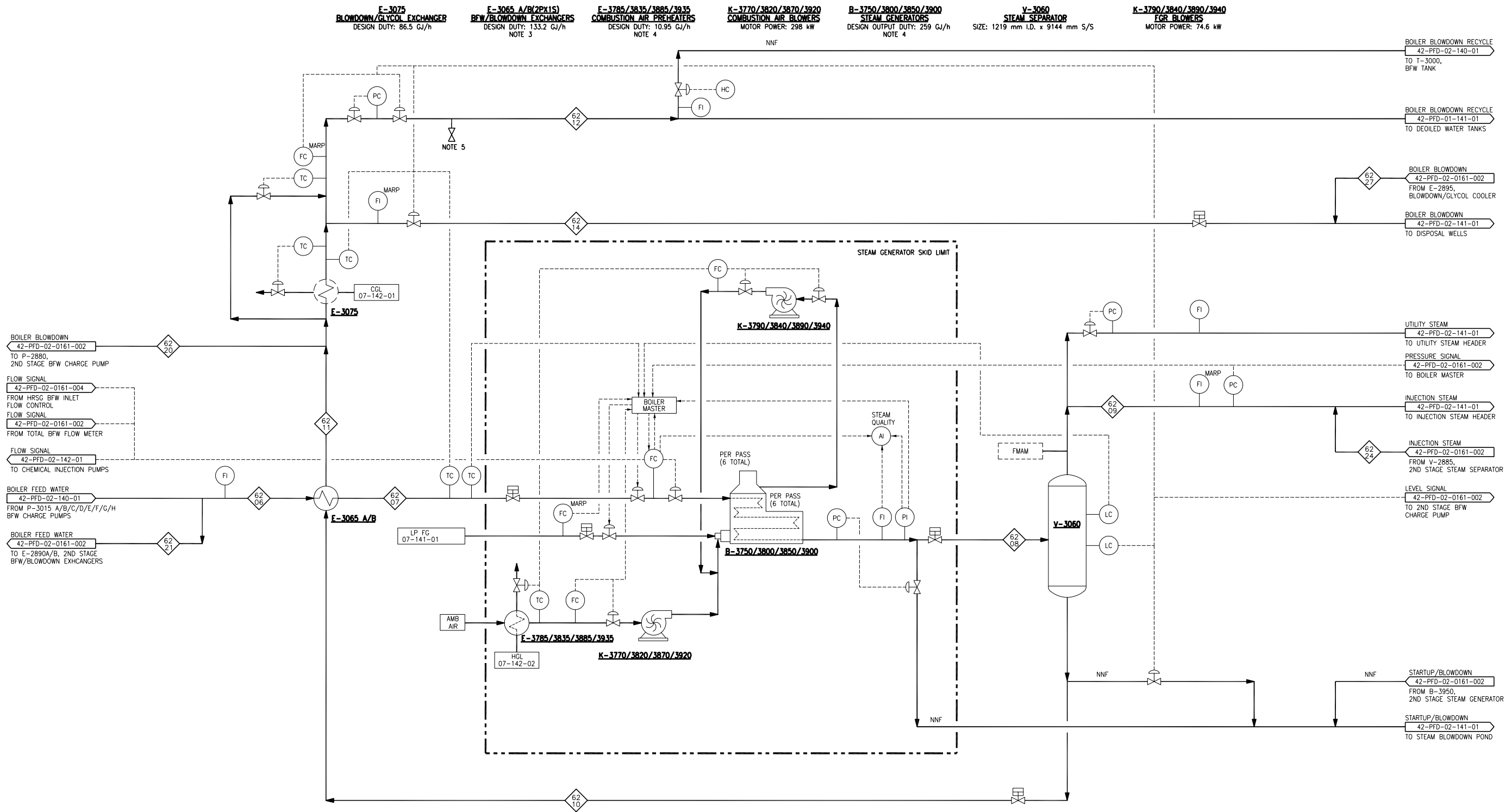
CONSULTANT NAME AND LOGO	
REVISION DESCRIPTION REISSUED FOR DESIGN	
PROJECT NO. CL1H	
LSD S.E. 1/4, Sec. 17, TWP 76, RG 6, W4M	
ISSUE DATE 2019/06/11	SCALE NONE

TITLE CHRISTINA LAKE COMMERCIAL PLANT PROCESS FLOW DIAGRAM CHEMICAL INJECTION - AREA 02 PHASE 1F/1G/1H	
DRAWING NO. CL1-42-PFD-02-0142-001	REVISION NO. 3.A.1

K:\Projects\Cenovus\2195\Piping\Drafting\PFDD\01 - IFR - (IN PROGRESS)\CL1-42-PFD-02-0152-001_O.B.O.dwg Ken Sorensen 4/3/2019 11:23 AM



CL1-42-PFD-02-0161-001_O.A.1



- NOTES:**
1. ALL EQUIPMENT SHOWN IS PHASE 1H, EXCEPT WHERE NOTED.
 2. ALL TAG NUMBERS TO BE PREFIXED BY "CL1-".
 3. DESIGN DUTY IS THE TOTAL DUTY FOR ALL SHELLS.
 4. DESIGN DUTY FOR EACH UNIT IS SHOWN.
 5. FUTURE TIE-IN POINT FOR DIVERTING 2ND STAGE BLOWDOWN TO DEOILED WATER TANKS AND/OR THE BFW TANK.

PACKAGE NO.

REFERENCE NUMBER	REFERENCE TITLE

STAMPS



2019-06-11

PERMIT TO PRACTICE
VISTA PROJECTS LIMITED
Date: Jun 10, 2019
PERMIT NUMBER: P-4539
The Association of Professional
Engineers and Geoscientists of Alberta

REV NO	REVISION	DATE	DRN	CKD	DES	LDE	PE
VB	PHASE 1H EXPANSION - ISSUED FOR REGULATORY APPROVAL		AP				
O.A.0	PHASE 1H EXPANSION - ISSUED FOR DESIGN	2019/04/05	EMJ	RVG	ZGA	KUL	JEG
O.A.1	PHASE 1H EXPANSION - REISSUED FOR DESIGN	2019/06/11	KSO	RVG	ZGA	KUL	JEG

CONSULTANT NAME AND LOGO



Vista
Projects

REVISION DESCRIPTION
REISSUED FOR DESIGN

PROJECT NO.
CL1H

LSD
S.E. 1/4, Sec. 17, TWP 76, RG 6, W4M

ISSUE DATE
2019/06/11

SCALE
NONE

TITLE



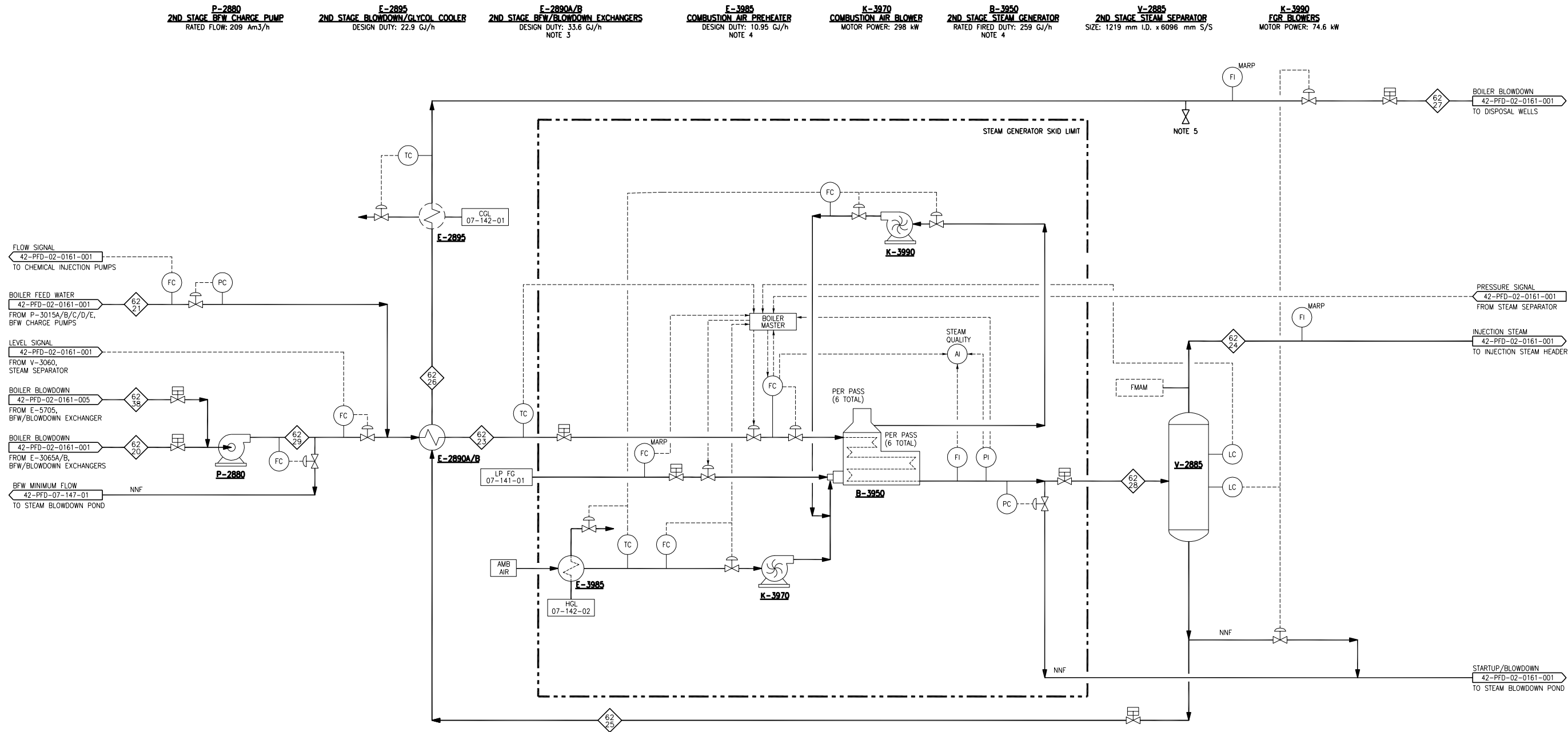
cenovus
ENERGY

CHRISTINA LAKE COMMERCIAL PLANT
PROCESS FLOW DIAGRAM
STEAM GENERATION SYSTEM (OTSG)
PHASE 1H

DRAWING NO.
CL1-42-PFD-02-0161-001

REVISION NO.
O.A.1

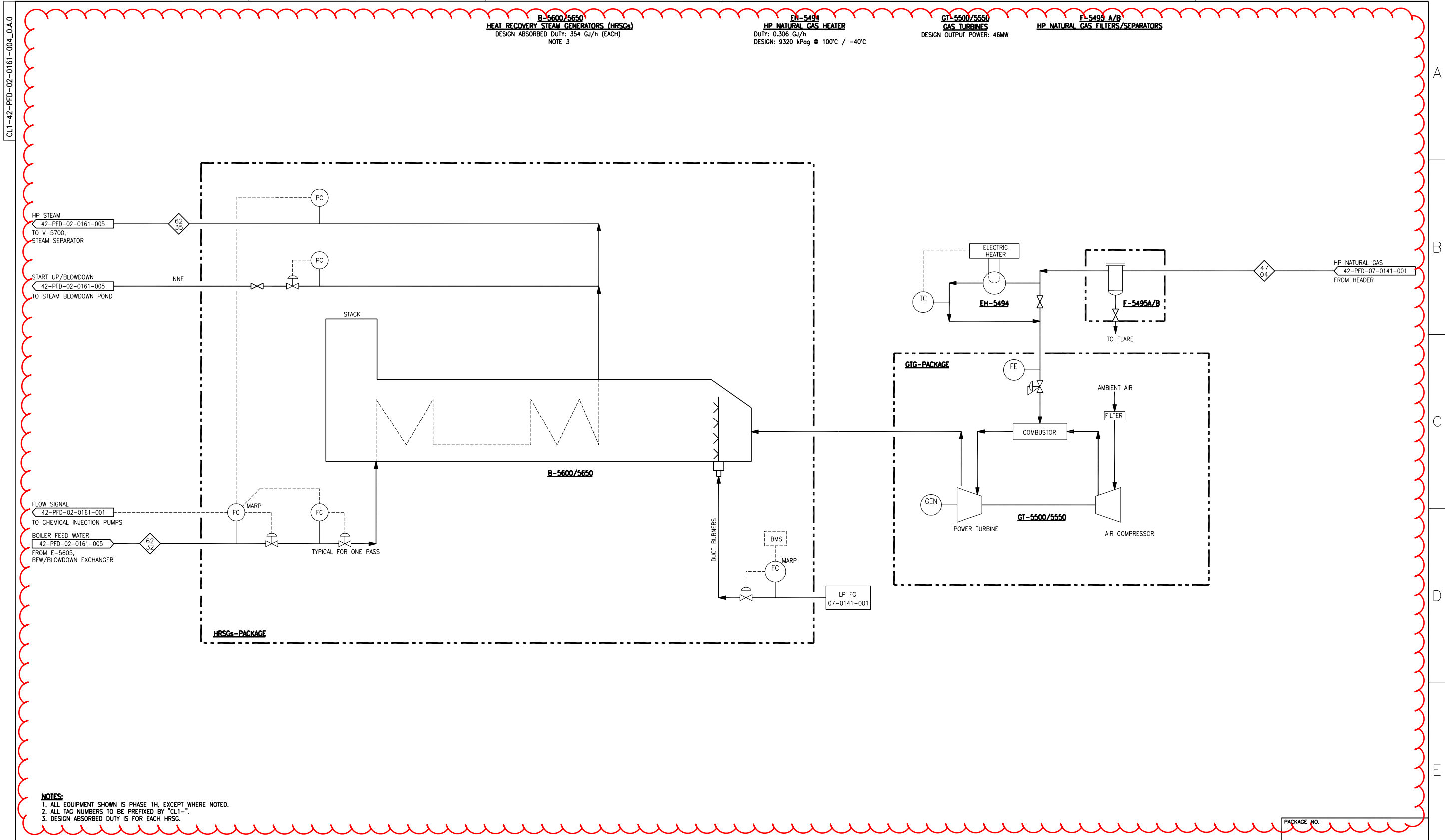
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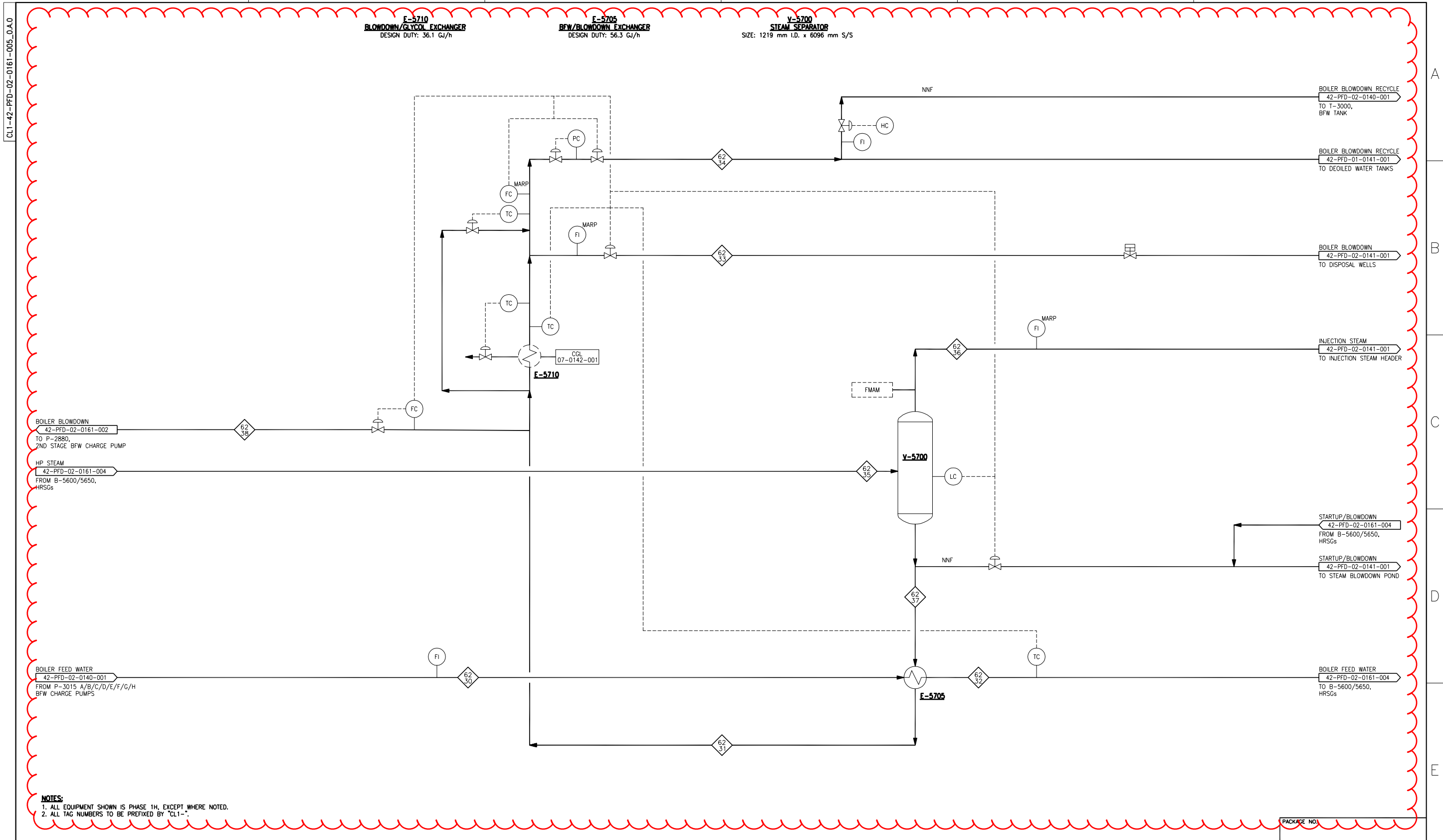
- NOTES:**
1. ALL EQUIPMENT SHOWN IS PHASE 1H EXCEPT WHERE NOTED.
 2. ALL TAG NUMBERS TO BE PREFIXED BY "CL1-".
 3. DESIGN DUTY IS THE TOTAL DUTY FOR ALL SHELLS.
 4. DESIGN DUTY FOR EACH UNIT IS SHOWN.
 5. FUTURE TIE-IN POINT FOR DIVERTING 2ND STAGE BLOWDOWN TO DEOILED WATER TANKS AND/OR THE BFW TANK.

PACKAGE NO.

REFERENCE NUMBER	REFERENCE TITLE	STAMPS	REV NO	REVISION	DATE	DRN	CKD	DES	LDE	PE	CONSULTANT NAME AND LOGO	TITLE
			O.A.0	PHASE 1H EXPANSION - ISSUED FOR DESIGN	2019/04/05	KSO	RVG	ZGA	KUL	JEG		CHRISTINA LAKE COMMERCIAL PLANT PROCESS FLOW DIAGRAM STEAM GENERATION SYSTEM (2ND STAGE OTSG) PHASE 1H
			O.A.1	PHASE 1H EXPANSION - REISSUED FOR DESIGN	2019/06/11	KSO	RVG	ZGA	KUL	JEG		
											REVISION DESCRIPTION REISSUED FOR DESIGN	
											PROJECT NO. CL1H	
											LSD S.E. 1/4, Sec. 17, TWP 76, RG 6, W4M	
											ISSUE DATE 2019/06/11	
											SCALE NONE	
											DRAWING NO. CL1-42-PFD-02-0161-002	
											REVISION NO. O.A.1	

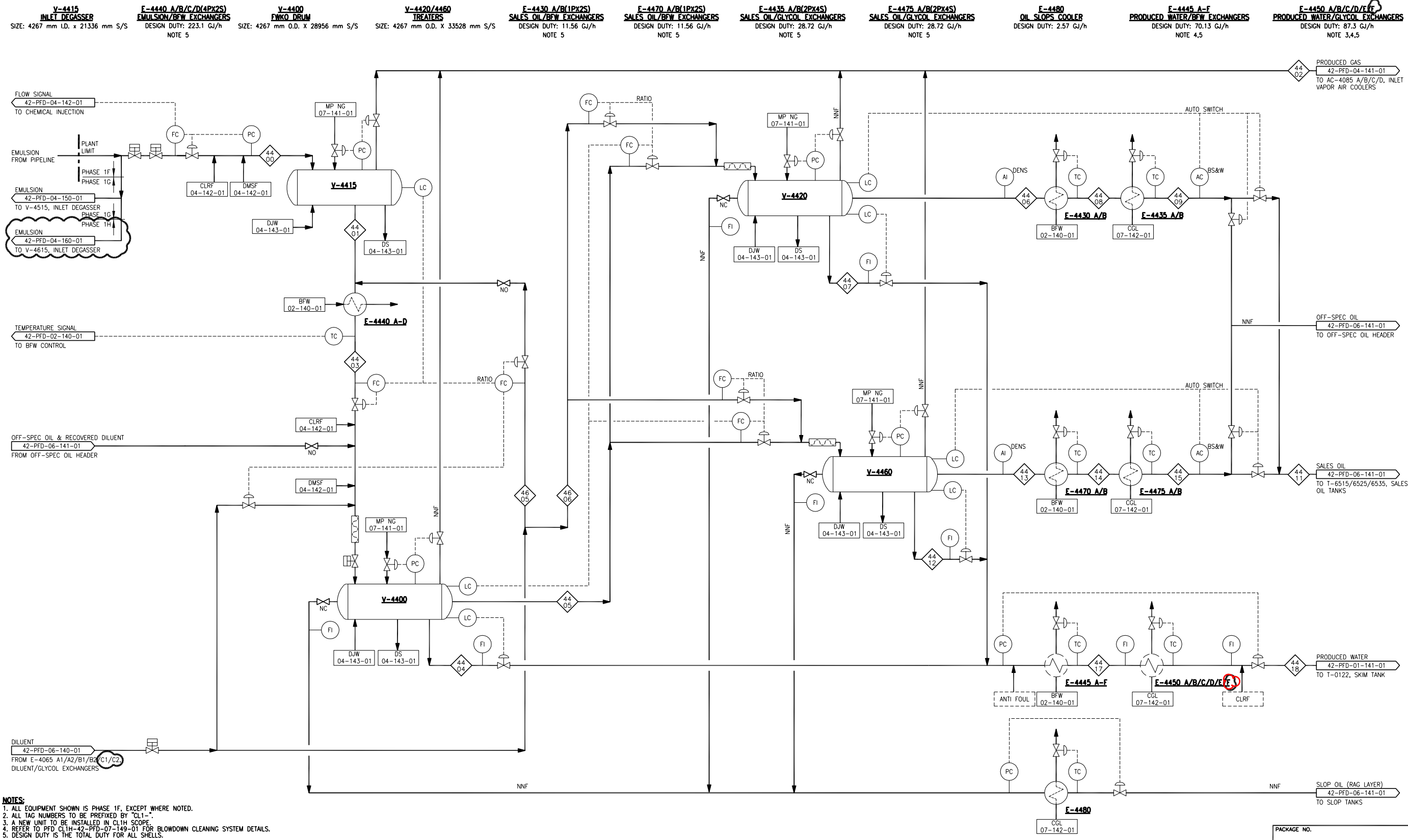


REFERENCE NUMBER	REFERENCE TITLE	STAMPS	REV NO	REVISION	DATE	DRN	CKD	DES	LDE	PE	CONSULTANT NAME AND LOGO	TITLE	DRAWING NO.	REVISION NO.
			O.A.O	PHASE 1H EXPANSION - ISSUED FOR DESIGN	2019/06/11	KSO	RVG	ZGA	KUL	JEG		CHRISTINA LAKE COMMERCIAL PLANT PROCESS FLOW DIAGRAM STEAM GENERATION SYSTEM (COGENERATION) PHASE 1H	CL1-42-PFD-02-0161-004	O.A.O
											REVISION DESCRIPTION ISSUED FOR DESIGN			
											PROJECT NO. CL1H			
											LSD S.E. 1/4, Sec. 17, TWP 76, RG 6, W4M			
											ISSUE DATE 2019/06/11	SCALE NONE		



REFERENCE NUMBER	REFERENCE TITLE	STAMPS	REV NO	REVISION	DATE	DRN	CKD	DES	LDE	PE	CONSULTANT NAME AND LOGO	TITLE	DRAWING NO.	REVISION NO.
			O.A.O	PHASE 1H EXPANSION - ISSUED FOR DESIGN	2019/06/11	KSO	RVG	ZGA	KUL	JEG		CHRISTINA LAKE COMMERCIAL PLANT PROCESS FLOW DIAGRAM STEAM GENERATION SYSTEM (COGENERATION) PHASE 1H	CL1-42-PFD-02-0161-005	O.A.O
											REVISION DESCRIPTION ISSUED FOR DESIGN			
											PROJECT NO. CL1H			
											LSD S.E. 1/4, Sec. 17, TWP 76, RG 6, W4M			
											ISSUE DATE 2019/06/11	SCALE NONE		

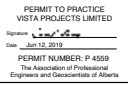
CL1-42-PFD-04-0140-001_4.A.1



NOTES:
1. ALL EQUIPMENT SHOWN IS PHASE 1F, EXCEPT WHERE NOTED.
2. ALL TAG NUMBERS TO BE PREFIXED BY "CL1-".
3. A NEW UNIT TO BE INSTALLED IN CL1H SCOPE.
4. REFER TO PFD CL1H-42-PFD-07-149-01 FOR BLOWDOWN CLEANING SYSTEM DETAILS.
5. DESIGN DUTY IS THE TOTAL DUTY FOR ALL SHELLS.

REFERENCE NUMBER	REFERENCE TITLE

STAMPS



2019-06-11

REV NO	REVISION	DATE	DRN	CKD	DES	LDE	PE
VB	PHASE 1H EXPANSION - REISSUED FOR REGULATORY APPROVAL	2012/07/25	RY	APC	LY	KUL	BZS
4.A.0	PHASE 1H EXPANSION - ISSUED FOR DESIGN	2019/04/05	EMJ	RVG	ZGA	KUL	JEG
4.A.1	PHASE 1H EXPANSION - REISSUED FOR DESIGN	2019/06/11	KSO	RVG	ZGA	KUL	JEG

CONSULTANT NAME AND LOGO



REVISION DESCRIPTION
REISSUED FOR DESIGN

PROJECT NO.
CL1H

LSD
S.E. 1/4, Sec. 17, TWP 76, RG 6, W4M

ISSUE DATE
2019/06/11

SCALE
NONE

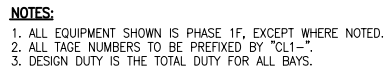
cenovus ENERGY

TITLE
CHRISTINA LAKE COMMERCIAL PLANT
PROCESS FLOW DIAGRAM
OIL TREATING SYSTEM
PHASE 1F/1G/1H

DRAWING NO.
CL1-42-PFD-04-0140-001

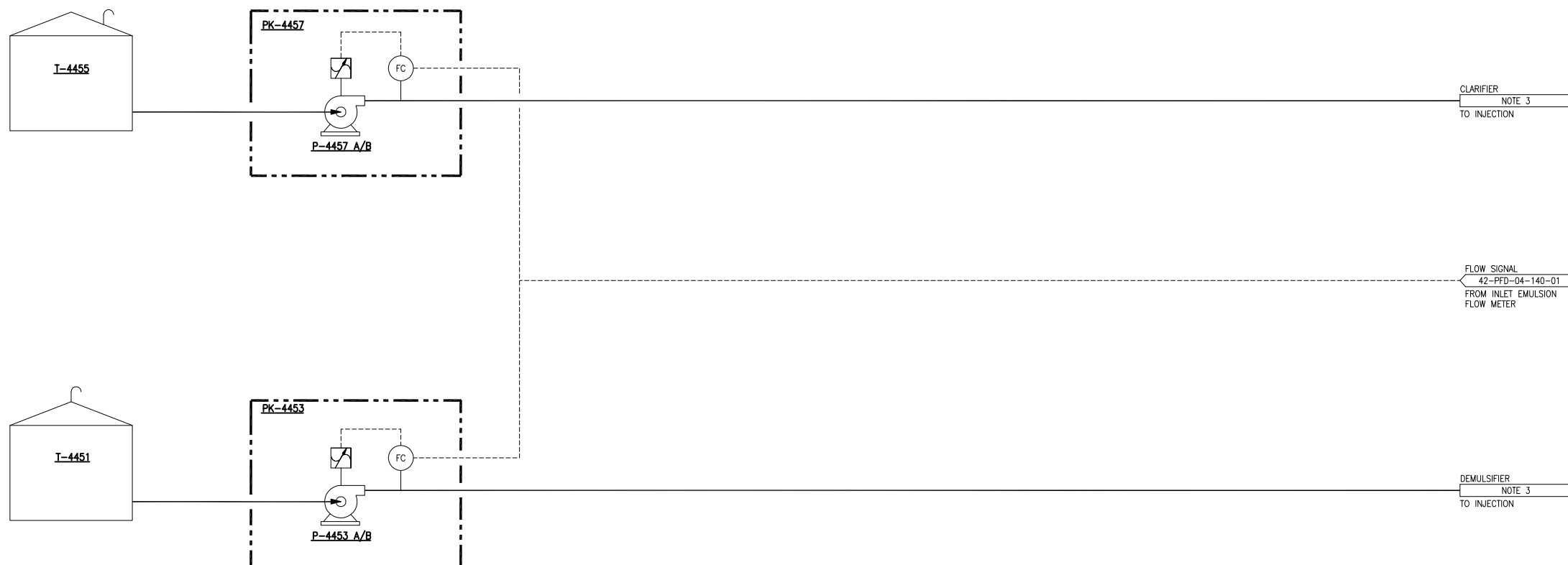
REVISION NO.
4.A.1

V-4087
PRODUCED GAS SEPARATOR
SIZE: 1829 I.D. x 7315 mm S/S



REFERENCE NUMBER	REFERENCE TITLE	STAMPS	REV. NO	REVISION	DATE	DRN	CKD	DES	LDE	PE	CONSULTANT NAME AND LOGO	TITLE
		  04/04/2019	VB	PHASE 1H EXPANSION – REISSUED FOR REGULATORY APPROVAL	2012/07/25	RY	APC	LY	KUL	BZS	 REVISION DESCRIPTION ISSUED FOR DESIGN PROJECT NO. CL1H LSD S.E. 1/4, Sec. 17, TWP 76, RG 6, W4M ISSUE DATE 2019/04/05 SCALE NONE	CHRISTINA LAKE COMMERCIAL PLANT PROCESS FLOW DIAGRAM PRODUCED GAS HANDLING PHASE 1F/1G/1H
			3.A.0	PHASE 1H EXPANSION – ISSUED FOR DESIGN	2019/04/05	EMJ	APC	ZGA	KUL	JEG		

P-4453 A/B
DEMULSIFIER INJECTION PUMPS
RATED FLOW: 0.15 Am³/h

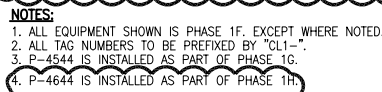


1. ALL EQUIPMENT SHOWN IS PHASE 1F, EXCEPT WHERE NOTED.
2. ALL TAG NUMBERS TO BE PREFIXED BY "CL1-".
3. INJECTION POINT LOCATED ON DWG. CL1G-42-PFD-04-140-01

PACKAGE NO.

REFERENCE NUMBER	REFERENCE TITLE	STAMPS	REV NO	REVISION	DATE	DRN	CKD	DES	LDE	PE	CONSULTANT NAME AND LOGO	cenovus ENERGY			
		 04/04/2019	0V	PHASE 1G EXPANSION – ISSUED FOR DESIGN	2013/01/15	MB	RVG	LY	KU	GP		TITLE CHRISTINA LAKE COMMERCIAL PLANT PROCESS FLOW DIAGRAM CHEMICAL INJECTION – AREA 04 PHASE 1F			
			1V	PHASE 1G EXPANSION – REISSUED FOR DESIGN	2013/07/23	JM	RVG	LY	KU	MC					
			2V	PHASE 1G EXPANSION – ISSUED FOR PROJECT TURNOVER	2015/06/08	RZ	RVG	LY	RVG	FY					
			3.A.0	PHASE 1H EXPANSION – ISSUED FOR DESIGN	2019/04/05	EMJ	ZGA	KUL	JEG						
												REVISION DESCRIPTION ISSUED FOR DESIGN	DRAWING NO. CL1-42-PFD-04-0142-001		
												PROJECT NO. CL1H			REVISION NO. 3.A.0
												LSD S.E. 1/4, Sec. 17, TWP 76, RG 6, W4M			
												ISSUE DATE 2019/04/05			SCALE NONE

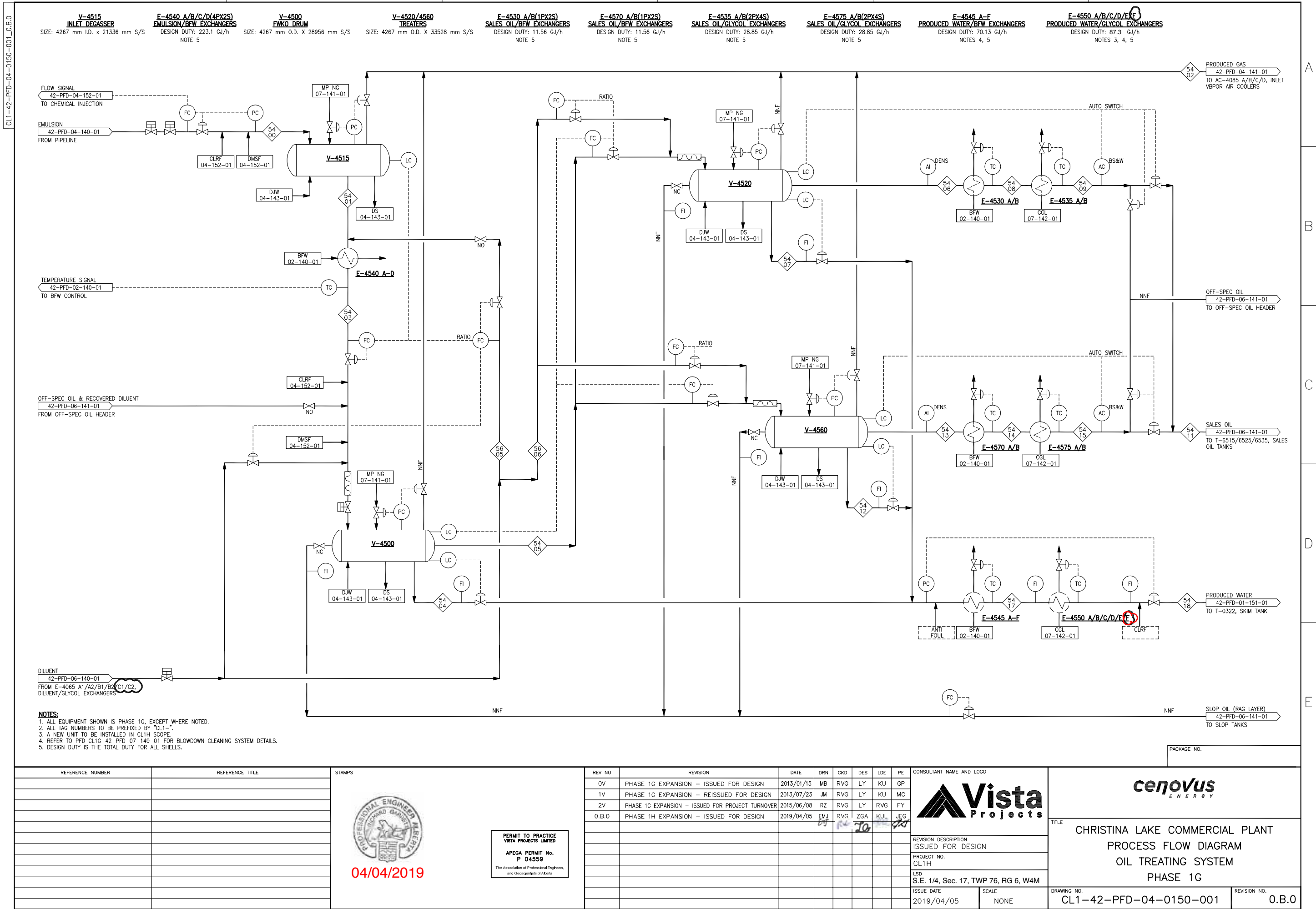
P-4042 A/B
DESAND TANK DECANT PUMPS
RATED FLOW: 10 Am³/h



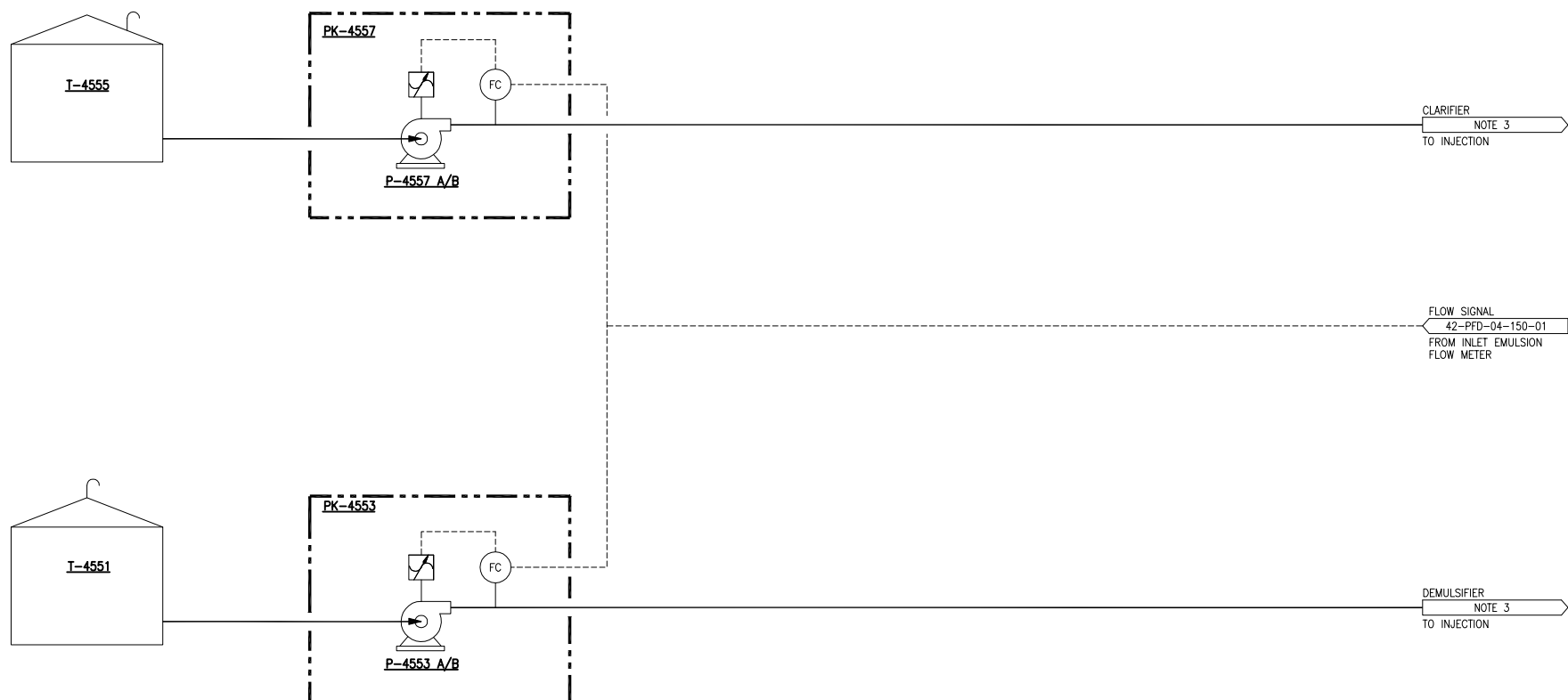
REFERENCE NUMBER		REFERENCE TITLE		STAMPS		CONSULTANT NAME AND LOGO									
				 04/04/2019											
				PERMIT TO PRACTICE VISTA PROJECTS LIMITED APEGA PERMIT No. P 04559 The Association of Professional Engineers, and Geoscientists of Alberta		cenovus ENERGY									
						TITLE									
						CHRISTINA LAKE COMMERCIAL PLANT									
						PROCESS FLOW DIAGRAM									
						DESAND SYSTEM									
						PHASE 1F/1G/1H									
						DRAWING NO.									
						CL1-42-PFD-04-0143-001									
						REVISION NO.									
						3.A.0									

REV. NO	REVISION	DATE	DRN	CKD	DES	LDE	PE
VB	PHASE 1H EXPANSION - REISSUED FOR REGULATORY APPROVAL	2012/07/25	DS	APC	LY	KUL	BZS
3.A.0	PHASE 1H EXPANSION - ISSUED FOR DESIGN	2019/04/05	EMJ	APC	ZGA	KUL	JEG

K:\Projects\Cenovus\2195\Piping\Drafting\PF01 - IFR - (IN PROGRESS)\CL1-42-PFD-04-0150-001_O.B.O.dwg Ken Sorensen 4/3/2019 11:22 AM



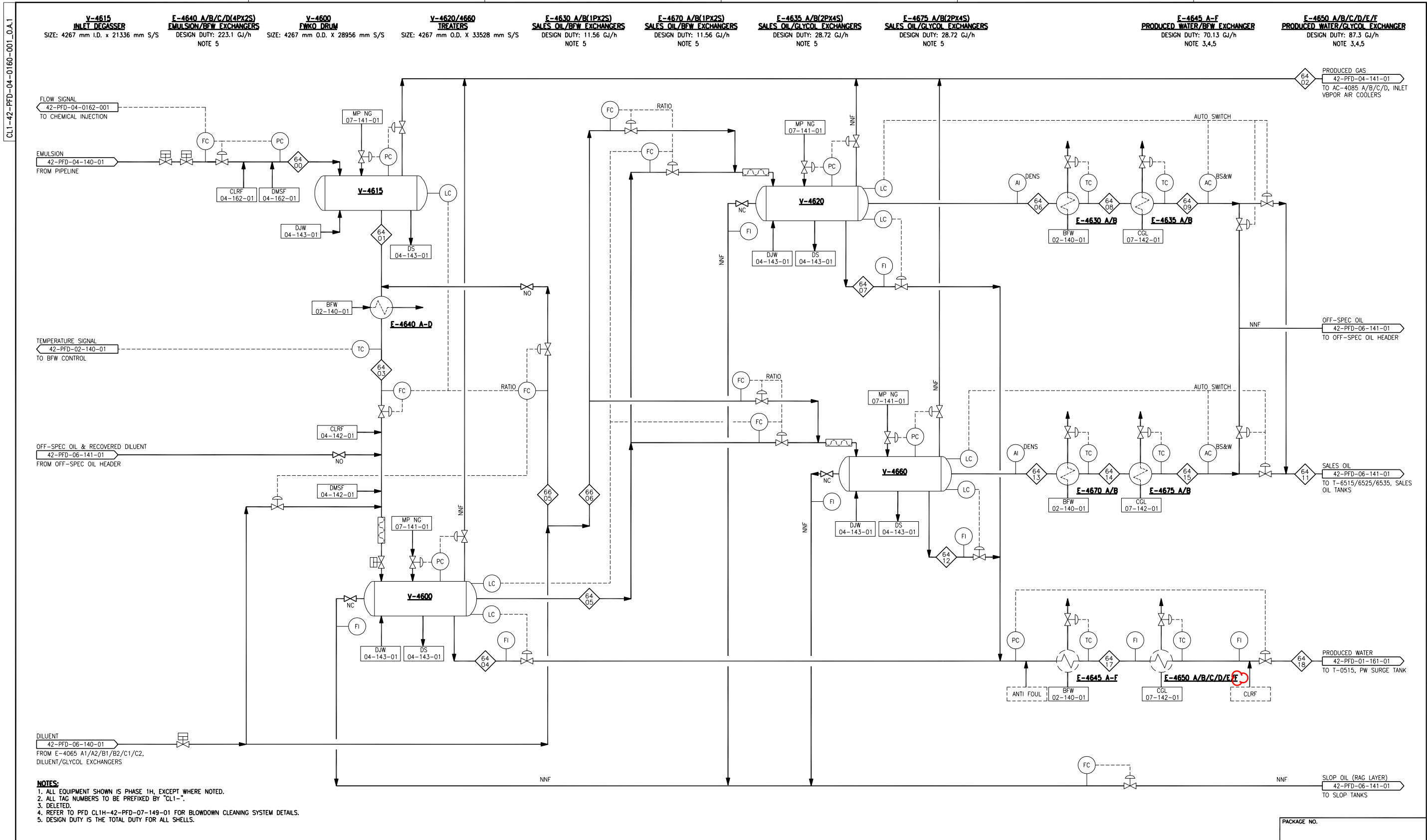
P-4553 A/B
DEMULSIFIER INJECTION PUMPS
RATED FLOW: 0.15 Am³/h



1. ALL EQUIPMENT SHOWN IS PHASE 1G, EXCEPT WHERE NOTED.
2. ALL TAG NUMBERS TO BE PREFIXED BY "CL1-".
3. INJECTION POINT LOCATED ON DWG. CL1G-42-PFD-04-150-01.

PACKAGE NO.

[illegible]



REFERENCE NUMBER	REFERENCE TITLE

STAMPS


2019-06-11


PERMIT TO PRACTICE
VISTA PROJECTS LIMITED
Date: 12-12-2019
PERMIT NUMBER: P-4559
The Association of Professional Engineers and Geoscientists of Alberta

REV NO	REVISION	DATE	DRN	CKD	DES	LDE	PE
VB	PHASE 1H EXPANSION - REISSUED FOR REGULATORY APPROVAL	2012/07/25	DS	APC	LY	KUL	BZS
O.A.0	PHASE 1H EXPANSION - ISSUED FOR DESIGN	2019/04/05	EMJ	RVG	ZGA	KUL	JEG
O.A.1	PHASE 1H EXPANSION - REISSUED FOR DESIGN	2019/06/11	KSO	RVG	ZGA	KUL	JEG

CONSULTANT NAME AND LOGO



REVISION DESCRIPTION
REISSUED FOR DESIGN

PROJECT NO.
CL1H

LSD
S.E. 1/4, Sec. 17, TWP 76, RG 6, W4M

ISSUE DATE
2019/06/11

SCALE
NONE

TITLE



CHRISTINA LAKE COMMERCIAL PLANT
PROCESS FLOW DIAGRAM
OIL TREATING SYSTEM
PHASE 1H

DRAWING NO.
CL1-42-PFD-04-0160-001

REVISION NO.
O.A.1

P-4653 A/B
DEMULSIFIER INJECTION PUMPS
RATED FLOW: 0.15 Am³/h



1. ALL EQUIPMENT SHOWN IS PHASE 1H, EXCEPT WHERE NOTED.
2. ALL TAG NUMBERS TO BE PREFIXED BY "CL1-".
3. INJECTION POINT LOCATED ON DWG. CL1-42-PFD-04-0160-001.

PACKAGE NO.

[illegible]

CL1-42-PFD-05-0140-001_3.A.0

F-5225 A/B(1PX2S)
CRUDE FLASH DRUM
FEED/EFFLUENT EXCHANGERS
DESIGN DUTY: 6.17 GJ/h
NOTE 3

V-5200
CRUDE FLASH DRUM
SIZE: 4267 mm O.D. x 12192 mm S/S

P-5215 A/B
CRUDE FLASH DRUM
OIL PUMPS
RATED FLOW: 79.5 Am3/h

P-5220 A/B
CRUDE FLASH DRUM
OIL RECYCLE PUMPS
RATED FLOW: 262.1 Am3/h

H-5270 A/B
CRUDE FLASH DRUM
REHEATERS
DESIGN DUTY: 9.35 GJ/h
NOTE 4

K-5270 A/B
CRUDE FLASH DRUM
REHEATER BLOWERS
MOTOR POWER: 22.4 kW

E-5235
CRUDE FLASH DRUM
OVERHEAD/GLYCOL EXCHANGER
DESIGN DUTY: 15.12 GJ/h

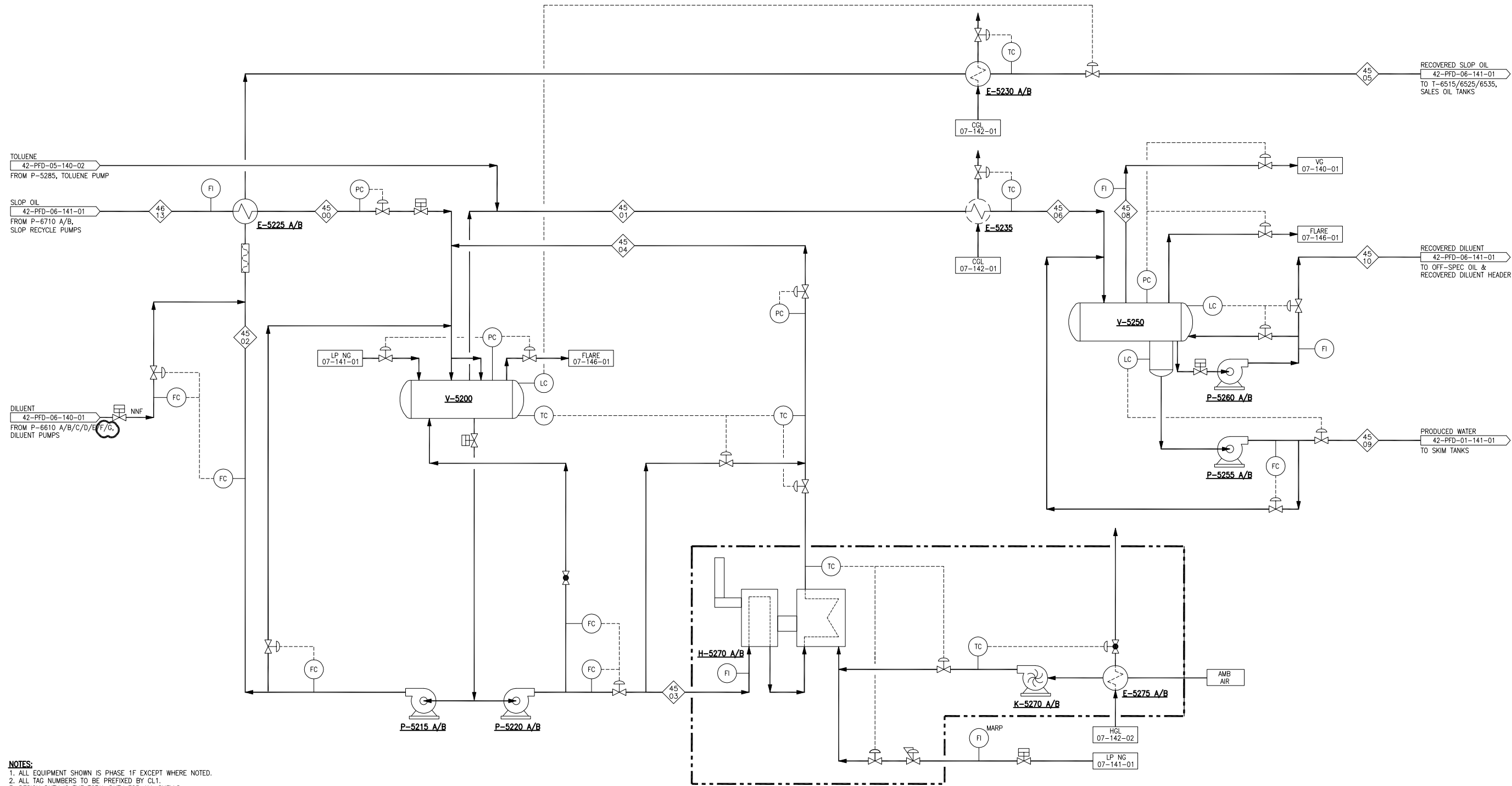
E-5275 A/B
CRUDE FLASH DRUM
REHEATER AIR PREHEATERS
DESIGN DUTY: 0.78 GJ/h
NOTE 3

E-5230 A/B(1PX2S)
CRUDE FLASH DRUM
EFFLUENT/GLYCOL EXCHANGERS
DESIGN DUTY: 7.34 GJ/h
NOTE 3

V-5250
CRUDE FLASH DRUM
OVERHEAD SEPARATOR
SIZE: 1067 mm O.D x 3658 mm S/S

P-5260 A/B
CRUDE FLASH RECYCLE
DILUENT PUMPS
RATED FLOW: 8.4 Am3/h

P-5255 A/B
CRUDE FLASH RECYCLE
WATER PUMPS
RATED FLOW: 4.3 Am3/h



- NOTES:
1. ALL EQUIPMENT SHOWN IS PHASE 1F EXCEPT WHERE NOTED.
 2. ALL TAG NUMBERS TO BE PREFIXED BY CL1.
 3. DESIGN DUTY IS THE TOTAL DUTY FOR ALL SHELLS
 4. DESIGN DUTY IS FOR EACH REHEATER

PACKAGE NO.

REFERENCE NUMBER	REFERENCE TITLE

STAMPS



04/04/2019

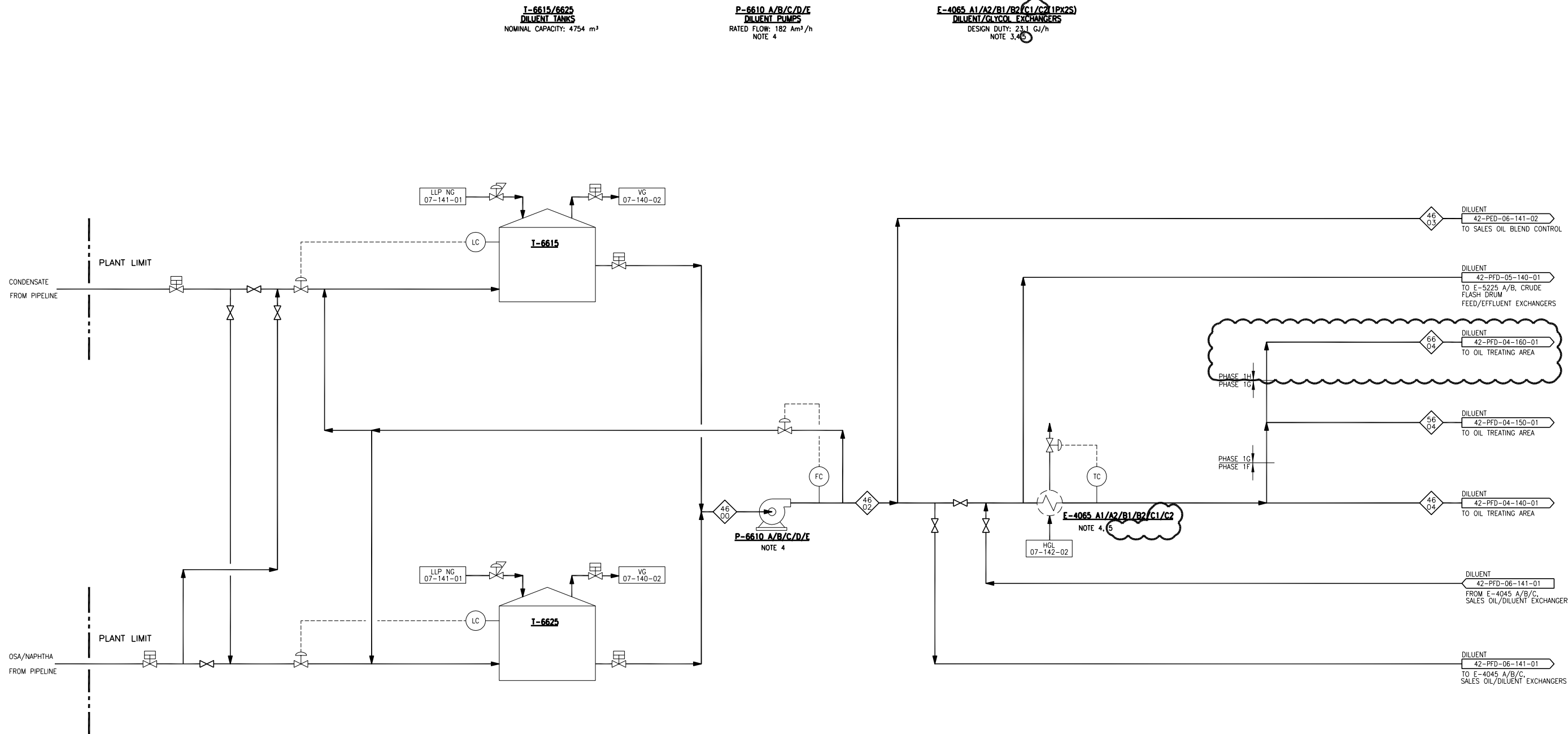
PERMIT TO PRACTICE
VISTA PROJECTS LIMITED
APEGA PERMIT No.
P 04559
The Association of Professional Engineers,
and Geoscientists of Alberta

REV NO	REVISION	DATE	DRN	CKD	DES	LDE	PE
0V	PHASE 1G EXPANSION - ISSUED FOR DESIGN	2013/01/15	MB	RVG	LY	KU	GP
1V	PHASE 1G EXPANSION - REISSUED FOR DESIGN	2013/07/23	JM	RVG	LY	KU	MC
2V	PHASE 1G EXPANSION - ISSUED FOR PROJECT TURNOVER	2015/06/08	RZ	RVG	LY	RVG	FY
3.A.0	PHASE 1H EXPANSION - ISSUED FOR DESIGN	2019/04/05	HYY	RVG	ZGA	KUL	JEG

CONSULTANT NAME AND LOGO	
REVISION DESCRIPTION ISSUED FOR DESIGN	
PROJECT NO. CL1H	
LSD S.E. 1/4, Sec. 17, TWP 76, RG 6, W4M	
ISSUE DATE 2019/04/05	SCALE NONE

cenovus ENERGY	
TITLE CHRISTINA LAKE COMMERCIAL PLANT PROCESS FLOW DIAGRAM OIL SLOPS TREATING SYSTEM PHASE 1F	
DRAWING NO. CL1-42-PFD-05-0140-001	REVISION NO. 3.A.0

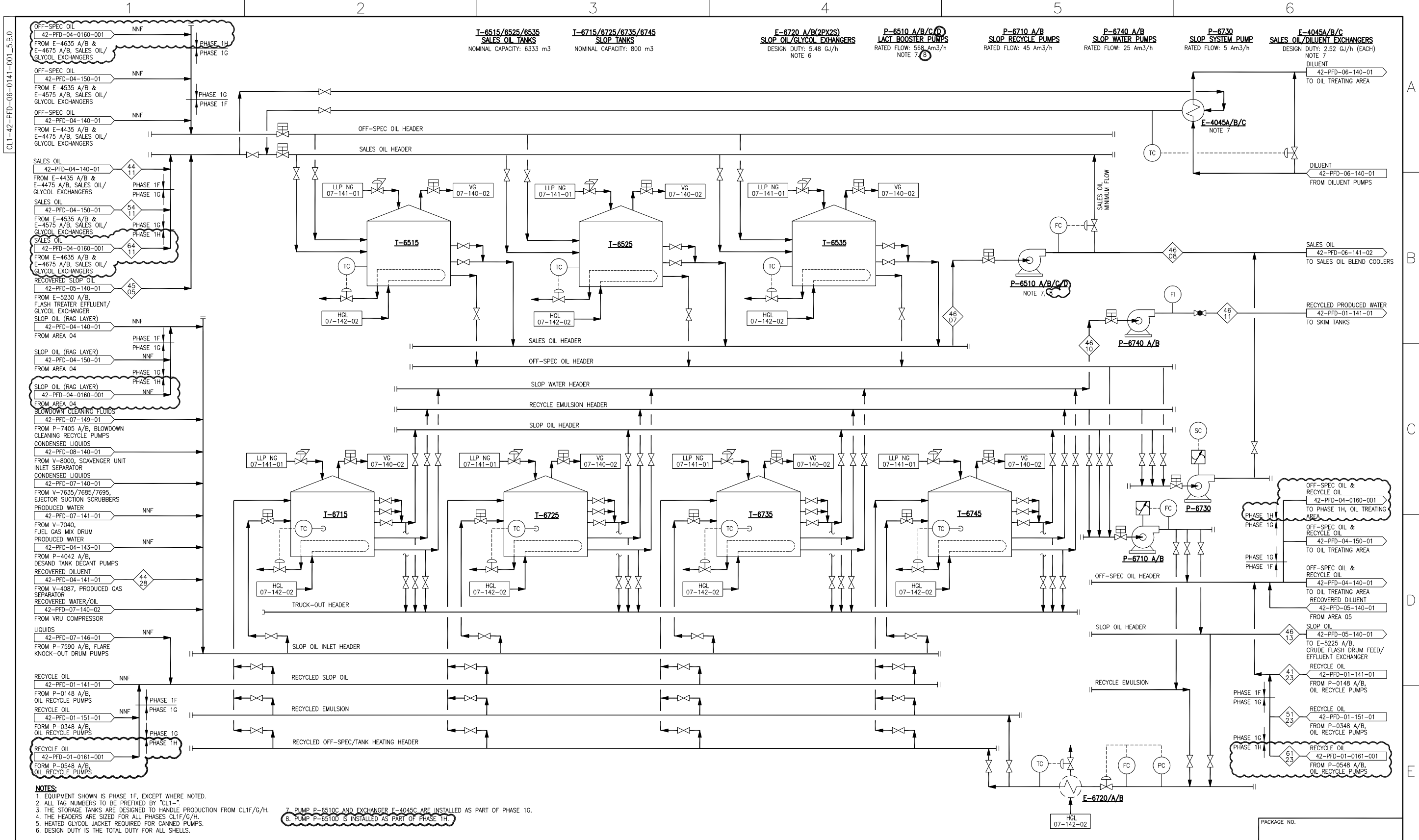
CL1-42-PFD-06-0140-001_5.A.1



- NOTES:**
1. ALL EQUIPMENT SHOWN IS PHASE 1F EXCEPT WHERE NOTED.
 2. ALL TAG NUMBERS TO BE PREFIXED BY "CL1-".
 3. DESIGN DUTY IS FOR THE TOTAL DUTY FOR ALL SHELLS.
 4. PUMPS P-6610 D/E AND EXCHANGERS E-4065 B1/B2 ARE INSTALLED AS PART OF PHASE 1G.
 5. EXCHANGERS E-4065 C1/C2 ARE INSTALLED AS PART OF PHASE 1H.

PACKAGE NO.

REFERENCE NUMBER	REFERENCE TITLE	STAMPS	REV NO	REVISION	DATE	DRN	CKD	DES	LDE	PE	CONSULTANT NAME AND LOGO	TITLE
			VA	PHASE 1H EXPANSION - ISSUED FOR REGULATORY APPROVAL	2012/07/25	DS	APC	LY	KUL	BZS		CHRISTINA LAKE COMMERCIAL PLANT PROCESS FLOW DIAGRAM DILUENT STORAGE/TRANSFER PHASE 1F/1G/1H
			5.A.0	PHASE 1H EXPANSION - ISSUED FOR DESIGN	2019/04/05	HYY	RVG	ZGA	KUL	JEG		
			5.A.1	PHASE 1H EXPANSION - REISSUED FOR DESIGN	2019/06/11	KSO	RVG	ZGA	KUL	JEG		
											REVISION DESCRIPTION REISSUED FOR DESIGN	
											PROJECT NO. CL1H	
											LSD S.E. 1/4, Sec. 17, TWP 76, RG 6, W4M	
											ISSUE DATE 2019/06/11	
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											DRAWING NO. CL1-42-PFD-06-0140-001	
											REVISION NO. 5.A.1	



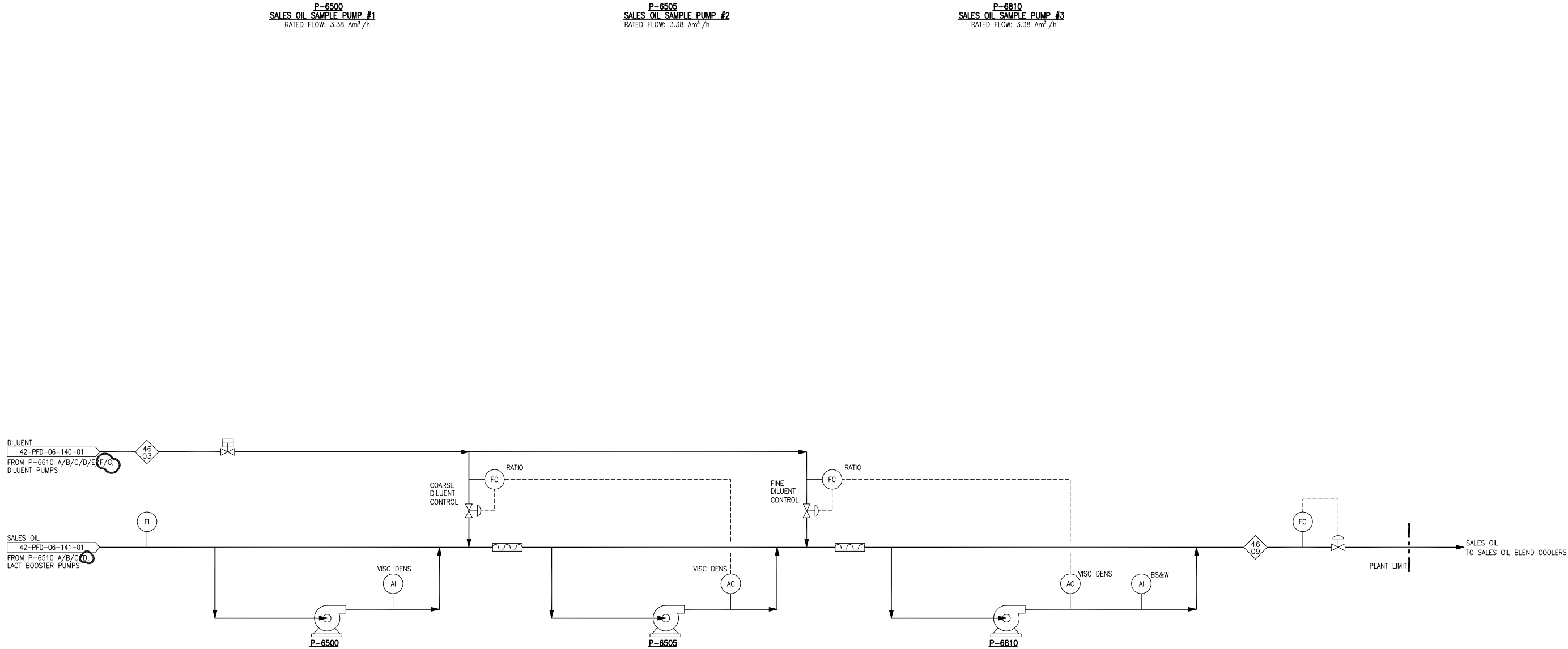
- NOTES:
- EQUIPMENT SHOWN IS PHASE 1F, EXCEPT WHERE NOTED.
 - ALL TAG NUMBERS TO BE PREFIXED BY "CL1-".
 - THE STORAGE TANKS ARE DESIGNED TO HANDLE PRODUCTION FROM CL1F/G/H.
 - THE HEADERS ARE SIZED FOR ALL PHASES CL1F/G/H.
 - HEATED GLYCOL JACKET REQUIRED FOR CANNED PUMPS.
 - DESIGN DUTY IS THE TOTAL DUTY FOR ALL SHELLS.

7. PUMP P-6510C AND EXCHANGER E-4045C ARE INSTALLED AS PART OF PHASE 1G.
8. PUMP P-6510D IS INSTALLED AS PART OF PHASE 1H.

REFERENCE NUMBER		REFERENCE TITLE	 04/04/2019	REV. NO	REVISION	DATE	DRN	CKD	DES	LDE	PE	CONSULTANT NAME AND LOGO		 TITLE CHRISTINA LAKE COMMERCIAL PLANT PROCESS FLOW DIAGRAM SALES OIL & SLOP OIL STORAGE/TRANSFER PHASE 1F/1G/1H DRAWING NO. CL1-42-PFD-06-0141-001 REVISION NO. 5.B.0	
				0V	PHASE 1G EXPANSION – ISSUED FOR DESIGN	2013/01/15	MB	RVG	LY	KU	GP	 REVISION DESCRIPTION ISSUED FOR DESIGN PROJECT NO. CL1H LSD S.E. 1/4, Sec. 17, TWP 76, RG 6, W4M ISSUE DATE 2019/04/05 SCALE NONE			
				1V	PHASE 1G EXPANSION – REISSUED FOR DESIGN	2013/07/23	JM	RVG	LY	KU	MC				
				2V	PHASE 1G EXPANSION – ISSUED FOR PROJECT TURNOVER	2015/06/08	RZ	RVG	LY	RVG	FY				
				5.B.0	PHASE 1H EXPANSION – ISSUED FOR DESIGN	2019/04/05	HY	RVG	ZGA	KUL	JEG				

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CL1-42-PFD-06-0141-002_3.B.O



NOTES:
1. ALL EQUIPMENT SHOWN IS PHASE 1F EXCEPT WHERE NOTED.
2. ALL TAG NUMBERS TO BE PREFIXED BY CL1-.

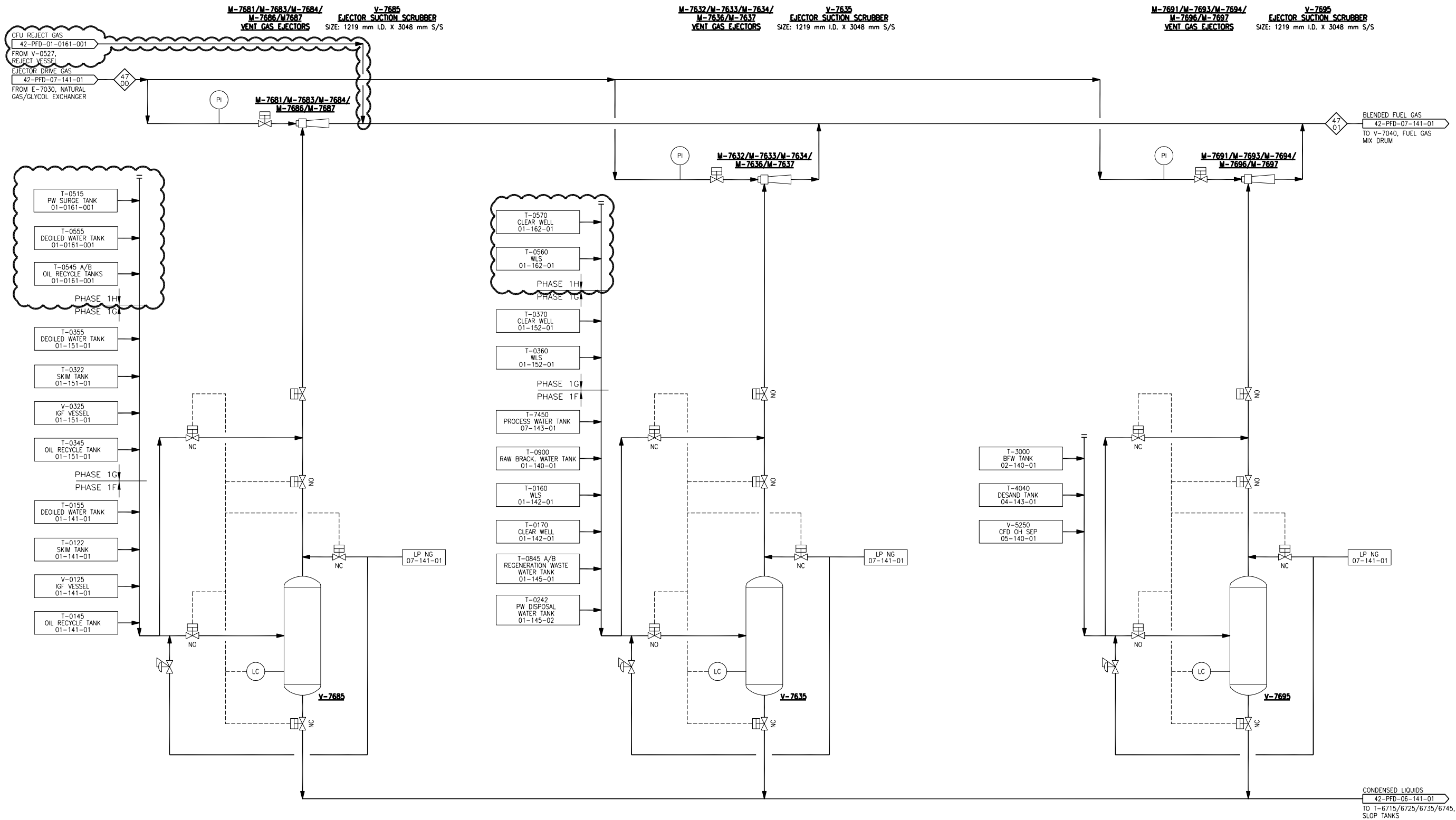
PACKAGE NO.

REFERENCE NUMBER	REFERENCE TITLE	STAMPS	REV NO	REVISION	DATE	DRN	CKD	DES	LDE	PE	CONSULTANT NAME AND LOGO	TITLE	DRAWING NO.	REVISION NO.
			VB	PHASE 1H EXPANSION - REISSUED FOR REGULATORY APPROVAL	2012/07/25	JM	APC	LY	KUL	BZS		CHRISTINA LAKE COMMERCIAL PLANT PROCESS FLOW DIAGRAM SALES OIL BLEND CONTROL PHASE 1F/1G/1H	CL1-42-PFD-06-0141-002	3.B.O
			3.B.O	PHASE 1H EXPANSION - ISSUED FOR DESIGN	2019/04/05	HYY	RVG	ZGA	KUL	JEG				
											REVISION DESCRIPTION ISSUED FOR DESIGN			
											PROJECT NO. CL1H			
											LSD S.E. 1/4, Sec. 17, TWP 76, RG 6, W4M			
											ISSUE DATE 2019/04/05	SCALE NONE		



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VISTA PROJECTS LIMITED
APEGA PERMIT No.
P 04559
The Association of Professional Engineers,
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CL1-42-PFD-07-0140-001_4.A.1



- NOTES:**
1. ALL EQUIPMENT SHOWN IS PHASE 1F, EXCEPT WHERE NOTED.
2. ALL TAG NUMBERS TO BE PREFIXED BY CL1-.

PACKAGE NO.

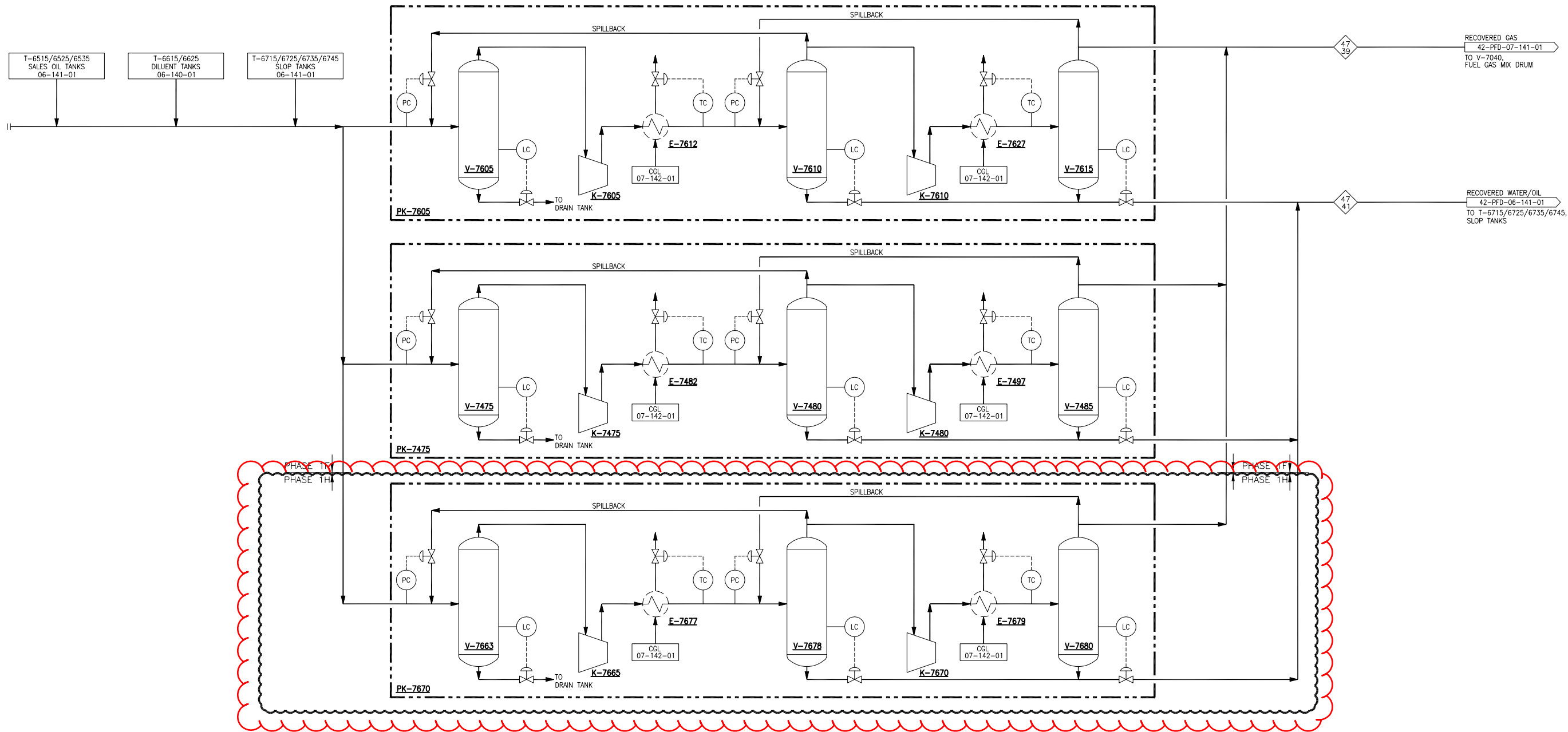
REFERENCE NUMBER	REFERENCE TITLE	STAMPS	REV NO	REVISION	DATE	DRN	CKD	DES	LDE	PE	CONSULTANT NAME AND LOGO	TITLE
			VB	PHASE 1H EXPANSION - REISSUED FOR REGULATORY APPROVAL	2012/07/25	JM	APC	LY	KUL	BZS		CHRISTINA LAKE COMMERCIAL PLANT PROCESS FLOW DIAGRAM VAPOUR RECOVERY SYSTEM (EJECTOR) PHASE 1F/1G/1H
			4.A.0	PHASE 1H EXPANSION - ISSUED FOR DESIGN	2019/04/05	HYI	RVG	ZGA	KUL	JEG		
			4.A.1	PHASE 1H EXPANSION - REISSUED FOR DESIGN	2019/06/11	KSO	RVG	ZGA	KUL	JEG		
											REVISION DESCRIPTION REISSUED FOR DESIGN	
											PROJECT NO. CL1H	
											LSD S.E. 1/4, Sec. 17, TWP 76, RG 6, W4M	
											ISSUE DATE 2019/06/11	
											SCALE NONE	
											DRAWING NO. CL1-42-PFD-07-0140-001	
											REVISION NO. 4.A.1	



PERMIT TO PRACTICE
VISTA PROJECTS LIMITED
Date: Jun 12, 2019
PERMIT NUMBER: P 4559
The Association of Professional
Engineers and Geoscientists of Alberta

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CL1-42-PFD-07-0140-002_4.C.O



- NOTES:
1. ALL EQUIPMENT SHOWN IS PHASE 1F EXCEPT WHERE NOTED.
 2. ALL TAG NUMBERS TO BE PREFIXED BY "CL1-".
 3. PK-7670 IS INSTALLED AS PART OF PHASE H.

REFERENCE NUMBER	REFERENCE TITLE

STAMPS



04/04/2019

PERMIT TO PRACTICE
VISTA PROJECTS LIMITED

APEGA PERMIT No.
P 04559

The Association of Professional Engineers,
and Geoscientists of Alberta

REV NO	REVISION	DATE	DRN	CKD	DES	LDE	PE
0V	PHASE 1G EXPANSION - ISSUED FOR DESIGN	2013/01/15	MB	RVG	LY	KU	GP
1V	PHASE 1G EXPANSION - REISSUED FOR DESIGN	2013/07/23	JM	RVG	LY	KU	MC
2V	PHASE 1G EXPANSION - ISSUED FOR PROJECT TURNOVER	2015/06/08	VW	RVG	LY	RVG	FY
4.C.O	PHASE 1H EXPANSION - ISSUED FOR DESIGN	2019/04/05	HYY	RVG	ZGA	KUL	JEG

CONSULTANT NAME AND LOGO



Vista
Projects

REVISION DESCRIPTION
ISSUED FOR DESIGN

PROJECT NO.
CL1H

LSD
S.E. 1/4, Sec. 17, TWP 76, RG 6, W4M

ISSUE DATE
2019/04/05

SCALE
NONE

PACKAGE NO.

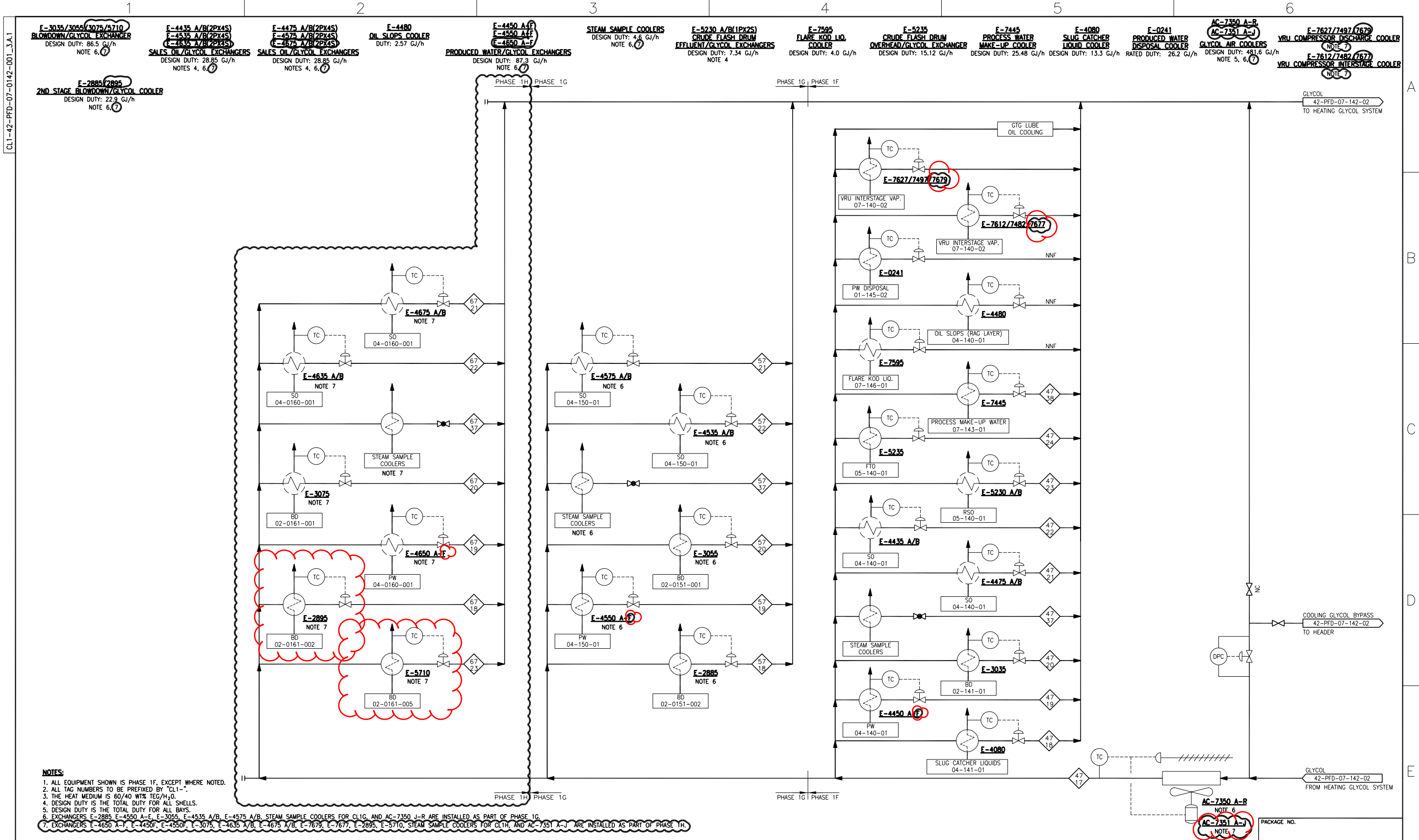


cenovus
ENERGY

TITLE
CHRISTINA LAKE COMMERCIAL PLANT
PROCESS FLOW DIAGRAM
VAPOUR RECOVERY SYSTEM (COMPRESSOR)
PHASE 1F/1G/1H

DRAWING NO.
CL1-42-PFD-07-0140-002

REVISION NO.
4.C.O



REFERENCE NUMBER	REFERENCE TITLE	STAMPS	REV NO	REVISION	DATE	DRN	CKD	DES	LDE	PE	CONSULTANT NAME AND LOGO	TITLE	PROJECT NO.	ISSUE DATE	SCALE	DRAWING NO.	REVISION NO.
			0V	PHASE 1G EXPANSION - ISSUED FOR DESIGN	2013/01/15	MB	RVG	LY	KU	GP	Vista Projects	CHRISTINA LAKE COMMERCIAL PLANT PROCESS FLOW DIAGRAM COOLING GLYCOL SYSTEM PHASE 1F/1G/1H	CL1H	2019/06/11	NONE	CL1-42-PFD-07-0142-001	3.A.1
			1V	PHASE 1G EXPANSION - REISSUED FOR DESIGN	2013/07/23	JM	RVG	LY	KU	MC							
			2V	PHASE 1G EXPANSION - ISSUED FOR PROJECT TURNOVER	2015/06/08	VW	RVG	LY	RVG	FY							
			3.A.0	PHASE 1H EXPANSION - ISSUED FOR DESIGN	2019/04/05	HY	RVG	ZGA	KUL	JEG	REVISION DESCRIPTION REISSUED FOR DESIGN						
			3.A.1	PHASE 1H EXPANSION - REISSUED FOR DESIGN	2019/06/11	KSO	RVG	ZGA	KUL	JEG	PROJECT NO. CL1H						
											LSD S.E. 1/4, Sec. 17, TWP 76, RG 6, W4M						
											ISSUE DATE						
											SCALE						

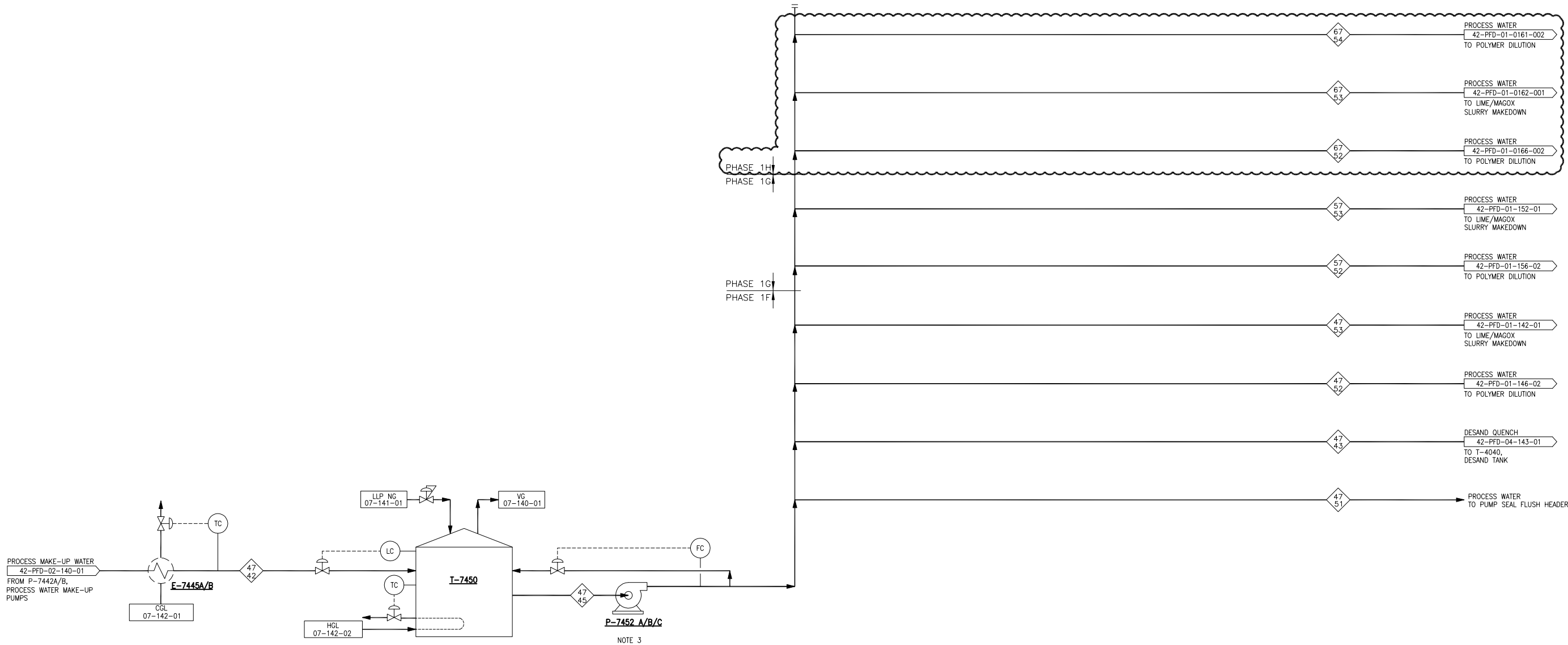
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CL1-42-PFD-07-0143-001_3.A.0

E-7445A/B
PROCESS WATER MAKE-UP COOLERS
DESIGN DUTY: 25.48 GJ/h

T-7450
PROCESS WATER TANK
NOMINAL CAPACITY: 323 m3

P-7452 A/B/C
PROCESS WATER SUPPLY PUMPS
RATED FLOW: 110 Am3/h
NOTE 3



- NOTES:**
1. ALL EQUIPMENT SHOWN IS PHASE 1F, EXCEPT WHERE NOTED.
 2. ALL TAG NUMBERS TO BE PREFIXED BY "CL1-".
 3. P-7452C IS INSTALLED AS PART OF PHASE 1G.

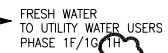
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REFERENCE NUMBER	REFERENCE TITLE	STAMPS	REV NO	REVISION	DATE	DRN	CKD	DES	LDE	PE	CONSULTANT NAME AND LOGO	TITLE	DRAWING NO.	REVISION NO.
			0V	PHASE 1G EXPANSION - ISSUED FOR DESIGN	2013/01/15	MB	RVG	LY	KU	GP		CHRISTINA LAKE COMMERCIAL PLANT PROCESS FLOW DIAGRAM PROCESS WATER SYSTEM PHASE 1F/1G/1H	CL1-42-PFD-07-0143-001	3.A.0
			1V	PHASE 1G EXPANSION - REISSUED FOR DESIGN	2013/07/23	JM	RVG	LY	KU	MC				
			2V	PHASE 1G EXPANSION - ISSUED FOR PROJECT TURNOVER	2015/06/08	RZ	RVG	LY	RVG	FY				
			3.A.0	PHASE 1H EXPANSION - ISSUED FOR DESIGN	2019/04/05	HYY	RVG	ZGA	KUL	JEG				
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											PROJECT NO. CL1H			
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											ISSUE DATE 2019/04/05	SCALE NONE		



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APEGA PERMIT No.
P 04559
The Association of Professional Engineers
and Geoscientists of Alberta

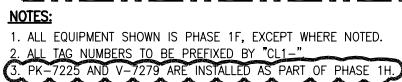
FRESH WATER MAKE-UP
42-PFD-07-148-01
TO T-7065,
FIRE WATER STORAGE TANK

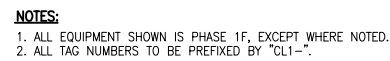


PACKAGE NO.

REFERENCE NUMBER	REFERENCE TITLE	STAMPS	REV. NO	REVISION	DATE	DRN	CKD	DES	LDE	PE	CONSULTANT NAME AND LOGO	TITLE
		 04/04/2019 PERMIT TO PRACTICE VISTA PROJECTS LIMITED APEGA PERMIT No. P 04559 The Association of Professional Engineers, and Geoscientists of Alberta	0V	PHASE 1G EXPANSION – ISSUED FOR DESIGN	2013/01/15	MB	RVG	LY	KU	GP	 REVISION DESCRIPTION ISSUED FOR DESIGN PROJECT NO. CL1H LSD S.E. 1/4, Sec. 17, TWP 76, RG 6, W4M ISSUE DATE 2019/04/05 SCALE NONE	CHRISTINA LAKE COMMERCIAL PLANT PROCESS FLOW DIAGRAM FRESH WATER SYSTEM PHASE 1F/1G/1H
	1V		PHASE 1G EXPANSION – REISSUED FOR DESIGN	2013/07/23	JM	RVG	LY	KU	MC			
	2V		PHASE 1G EXPANSION – ISSUED FOR PROJECT TURNOVER	2015/06/08	RZ	RVG	LY	RVG	FY			
	4.A.0		PHASE 1H EXPANSION – ISSUED FOR DESIGN	2019/04/05	HYH	RVG	ZGA	KUL	JEG			

V-7275/7277/7279
INSTRUMENT AIR
DRY AIR RECEIVER
SIZE: 1829 mm O.D. x 6096 mm S/S
NOTE 3

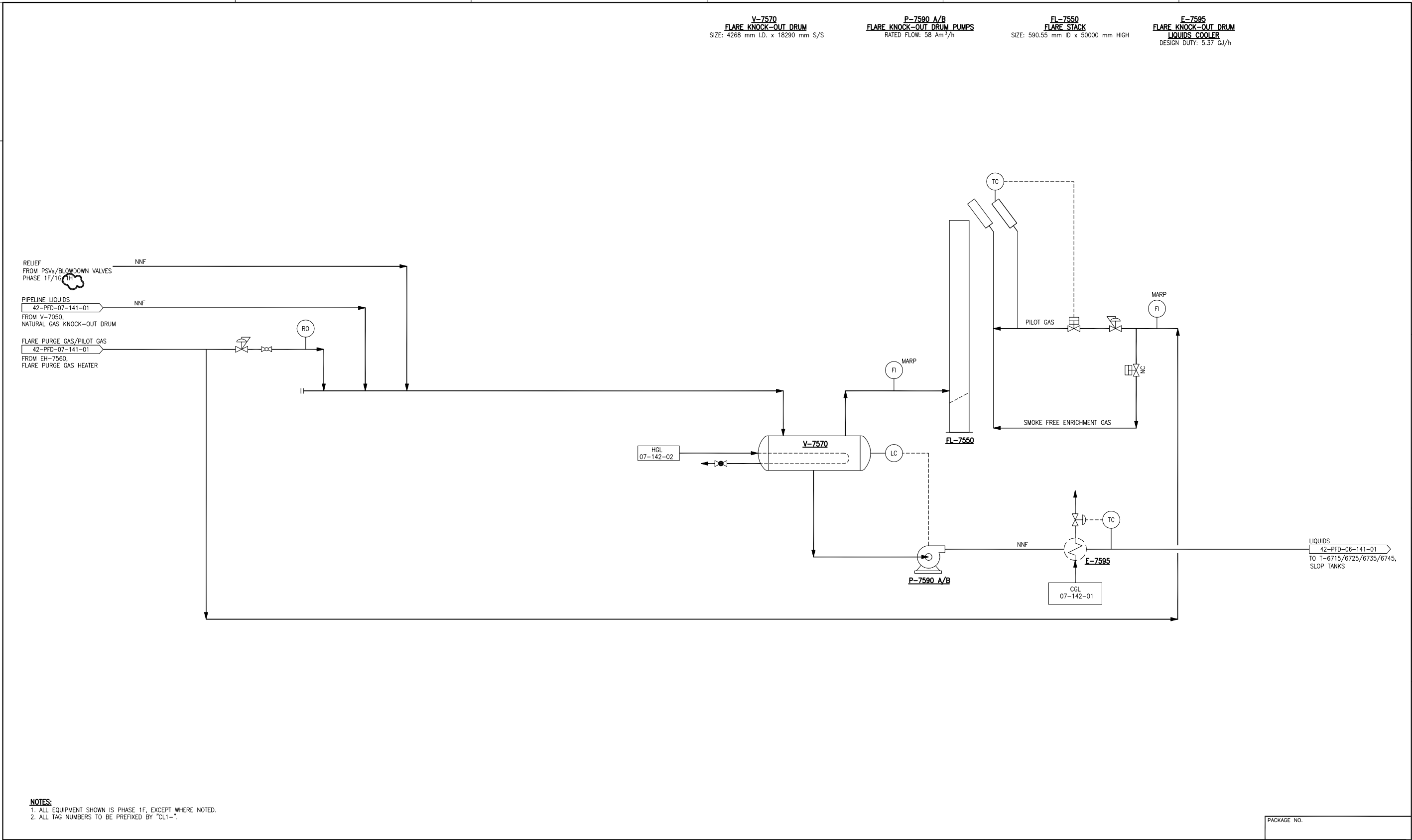
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REFERENCE NUMBER	REFERENCE TITLE	STAMPS		REV NO	REVISION	DATE	DRN	CKD	DES	LDE	PE	CONSULTANT NAME AND LOGO		
		 04/04/2019	PERMIT TO PRACTICE VISTA PROJECTS LIMITED APEGA PERMIT No. P 04559 The Association of Professional Engineers and Geoscientists of Alberta	0V	PHASE 1G EXPANSION – ISSUED FOR DESIGN	2013/01/15	MB	RVG	LY	KU	GP		TITLE CHRISTINA LAKE COMMERCIAL PLANT PROCESS FLOW DIAGRAM NITROGEN SYSTEM PHASE 1F/1G/1H	
				1V	PHASE 1G EXPANSION – REISSUED FOR DESIGN	2013/07/23	JM	RVG	LY	KU	MC			
				2V	PHASE 1G EXPANSION – ISSUED FOR PROJECT TURNOVER	2015/06/08	RZ	RVG	LY	RVG	FY			
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												REVISION DESCRIPTION ISSUED FOR DESIGN	DRAWING NO. CL1-42-PFD-07-0145-003 REVISION NO. 3.A.0	
											PROJECT NO. CL1H			
											LSD S.E. 1/4, Sec. 17, TWP 76, RG 6, W4M			
											ISSUE DATE 2019/04/05			
											SCALE NONE			

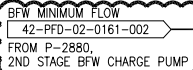
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CL1-42-PFD-07-0146-001_3.A.0



REFERENCE NUMBER	REFERENCE TITLE	STAMPS	REV NO	REVISION	DATE	DRN	CKD	DES	LDE	PE	CONSULTANT NAME AND LOGO	cenovus ENERGY		
		 04/04/2019	VC	PHASE 1H EXPANSION – REISSUED FOR REGULATORY APPROVAL	2012/08/22	IS	APC	LY	KUL	BZS		TITLE CHRISTINA LAKE COMMERCIAL PLANT PROCESS FLOW DIAGRAM FLARE SYSTEM PHASE 1F/1G/1H		
			3.A.0	PHASE 1H EXPANSION – ISSUED FOR DESIGN	2019/04/05	HYY	RVG	ZGA	KUL	JEG				
		PERMIT TO PRACTICE VISTA PROJECTS LIMITED APEGA PERMIT No. P 04559 The Association of Professional Engineers, and Geoscientists of Alberta									REVISION DESCRIPTION ISSUED FOR DESIGN	DRAWING NO. CL1–42–PFD–07–0146–001		
											PROJECT NO. CL1H			REVISION NO. 3.A.0
											LSD S.E. 1/4, Sec. 17, TWP 76, RG 6, W4M			
												ISSUE DATE 2019/04/05	SCALE NONE	

F-7785 A/B
BLOWDOWN POND
RETURN FILTERS
SIZE: 324 mm I.D. X 1029 mm S/FF

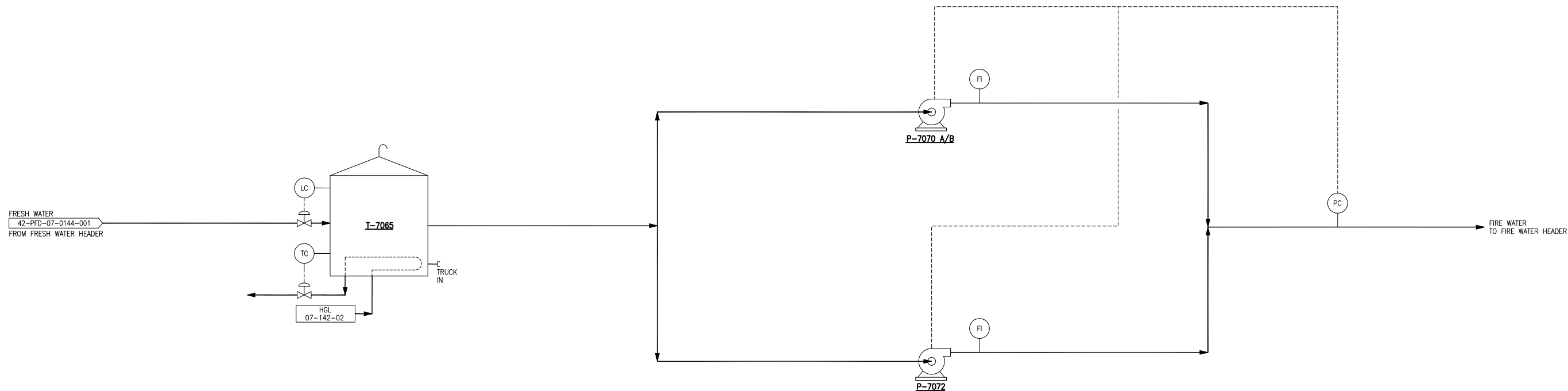


NOTES:

1. ALL EQUIPMENT SHOWN IS PHASE 1F EXCEPT WHERE NOTED.
2. ALL TAG NUMBERS TO BE PREFIXED BY "CL1-".

REFERENCE NUMBER	REFERENCE TITLE	STAMPS	REV. NO	REVISION	DATE	DRN	CKD	DES	LDE	PE	CONSULTANT NAME AND LOGO	TITLE	DRAWING NO.	REVISION NO.	
		 04/04/2019	0V	PHASE 1G EXPANSION – ISSUED FOR DESIGN	2013/01/15	KJS	RVG	LY	KU	GP		CHRISTINA LAKE COMMERCIAL PLANT PROCESS FLOW DIAGRAM STORM WATER/STEAM BLOWDOWN PONDS PHASE 1F/1G/1H	CL1-42-PFD-07-0147-001	4.A.0	
			1V	PHASE 1G EXPANSION – REISSUED FOR DESIGN	2013/07/23	JM	RVG	LY	KU	MC					REVISION DESCRIPTION ISSUED FOR DESIGN
			2V	PHASE 1G EXPANSION – ISSUED FOR PROJECT TURNOVER	2015/06/08	RZ	RVG	LY	RVG	FY					PROJECT NO. CL1H
			4.A.0	PHASE 1H EXPANSION – ISSUED FOR DESIGN	2019/04/05	HYT	RVG	ZGA	KUL	JEG					LSD S.E. 1/4, Sec. 17, TWP 76, RG 6, W4M

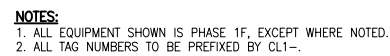
P-7072
FIRE WATER JOCKEY PUMP
RATED FLOW: 22.7 Am3/h



1. ALL EQUIPMENT SHOWN IS PHASE 1F EXCEPT WHERE NOTED
2. ALL TAG NUMBERS TO BE PREFIXED BY "CL1-".

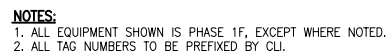
REFERENCE NUMBER	REFERENCE TITLE	STAMPS	REV. NO	REVISION	DATE	DRN	OKD	DES	LDE	PE	CONSULTANT NAME AND LOGO	TITLE	DRAWING NO.	REVISION NO.
		 04/04/2019 PERMIT TO PRACTICE VISTA PROJECTS LIMITED APEGA PERMIT No. P 04559 The Association of Professional Engineers, and Geoscientists of Alberta	0V	PHASE 1G EXPANSION – ISSUED FOR DESIGN	2013/01/15	KJS	RVG	LY	KU	GP	 REVISION DESCRIPTION ISSUED FOR DESIGN PROJECT NO. CL1H LSD S.E. 1/4, Sec. 17, TWP 76, RG 6, W4M ISSUE DATE 2019/04/05 SCALE NONE	CHRISTINA LAKE COMMERCIAL PLANT PROCESS FLOW DIAGRAM FIRE WATER SYSTEM PHASE 1F	CL1–42–PFD–07–0148–001	3.A.0
	1V		PHASE 1G EXPANSION – REISSUED FOR DESIGN	2013/07/23	JM	RVG	LY	KU	MC					
	2V		PHASE 1G EXPANSION – ISSUED FOR PROJECT TURNOVER	2015/06/08	RZ	RVG	LY	RVG	FY					
	3.A.0		PHASE 1H EXPANSION – ISSUED FOR DESIGN	2019/04/05	HYV	PVC	ZGA	KUL	JEG					

P-7405 A/B
BLOWDOWN CLEANING
RECYCLE PUMPS
RATED FLOW: 30 Am³/h



	
TITLE CHRISTINA LAKE COMMERCIAL PLANT PROCESS FLOW DIAGRAM BLOWDOWN CLEANING SYSTEM PHASE 1F/1G/1H	
DRAWING NO. CL1-42-PFD-07-0149-001	REVISION NO. 3.A.0

T-8025
SPENT CHEMICAL
STORAGE TANK



PACKAGE NO.

REFERENCE NUMBER		REFERENCE TITLE		STAMPS		CONSULTANT NAME AND LOGO										cenovus ENERGY	
					PERMIT TO PRACTICE VISTA PROJECTS LIMITED APEGA PERMIT No. P 04559 The Association of Professional Engineers, and Geoscientists of Alberta	REV NO	REVISION	DATE	DRN	CKD	DES	LDE	PE		TITLE CHRISTINA LAKE COMMERCIAL PLANT PROCESS FLOW DIAGRAM H2S SCAVENGER UNIT PHASE 1F		
		0V	PHASE 1G EXPANSION – ISSUED FOR DESIGN			2013/01/15	KJS	RVG	LY	KU	GP						
		1V	PHASE 1G EXPANSION – REISSUED FOR DESIGN			2013/07/23	JM	RVG	LY	KU	MC						
		2V	PHASE 1G EXPANSION – ISSUED FOR PROJECT TURNOVER			2015/06/08	RZ	RVG	LY	RVG	FY						
		4.A.0	PHASE 1H EXPANSION – ISSUED FOR DESIGN			2019/04/05	HYY	RVG	ZGA	KUL	JEG						