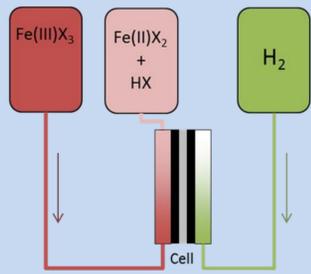
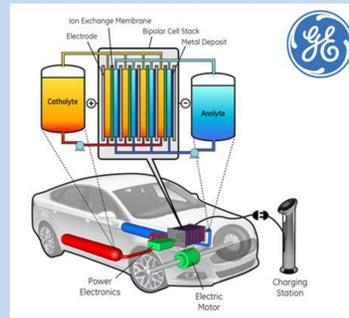


## Overview of Flow Cell Projects

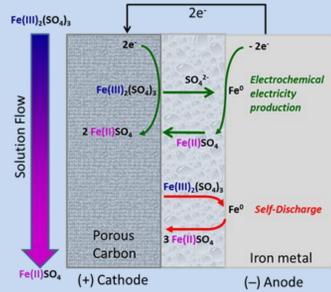
Inexpensive Fe-H<sub>2</sub>



High Capacity Aqueous Chemistry



Non-hazardous Fe-Fe

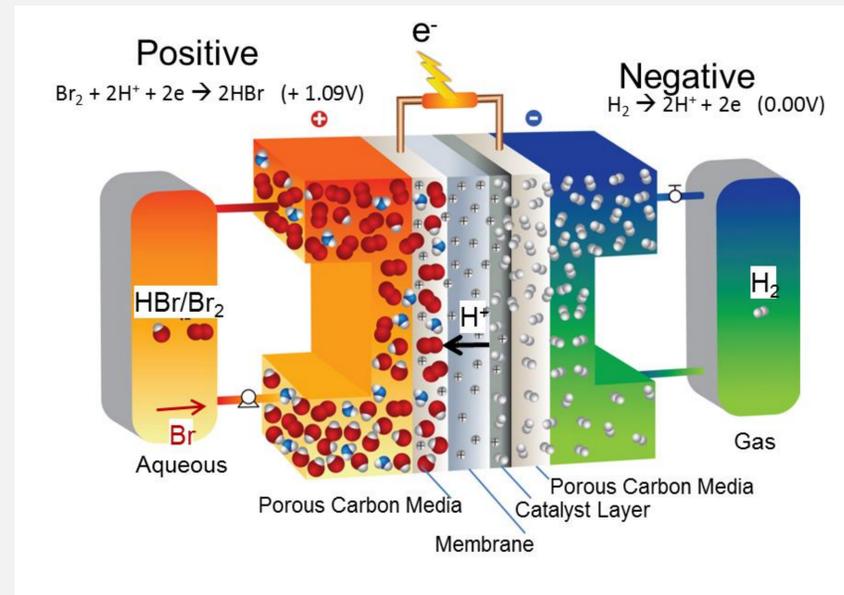


High Power Br<sub>2</sub>-H<sub>2</sub>



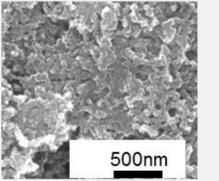
## Bromine-Hydrogen Redox Flow Cell

High-power, low-cost system

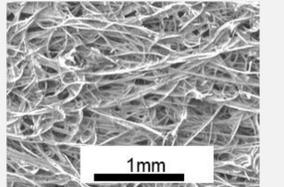


	\$/kg	Ah/\$
Vanadium (V2O5)	18	16
Hydrogen	10	2680
Bromine	1	335

Catalyst Layer (CL)

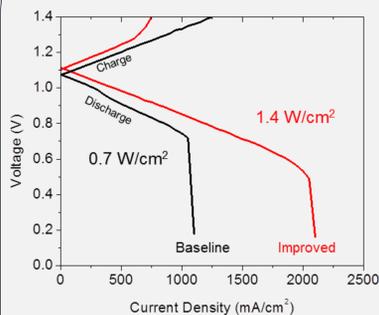


Porous Carbon Media (GDL)



## Improving Cell Metrics

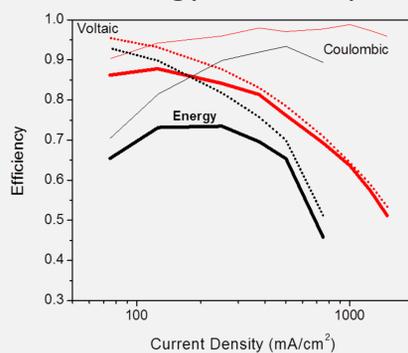
Cell Performance



Electrode and membrane optimization:

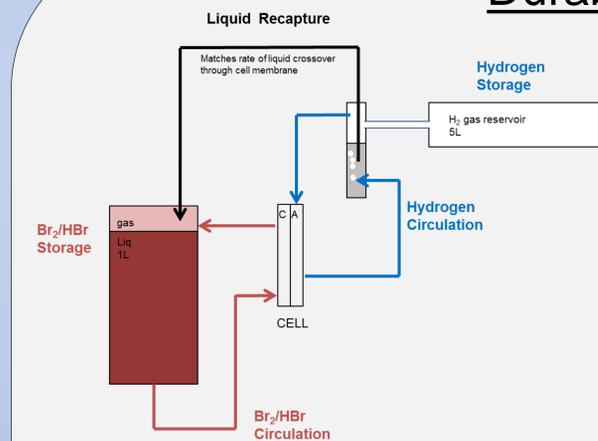
- |                             |                     |
|-----------------------------|---------------------|
| <b>Electrodes</b>           | <b>Membrane</b>     |
| - Br- adsorption on Pt (-)  | - Pretreatment      |
| - Cell compression          | - Thickness         |
| - Hydrogen pressure         | - Reinforcement     |
| - Porous media type         | - Equivalent weight |
| - Microporous media coating |                     |
| - Catalyst placement        |                     |

Energy Efficiency

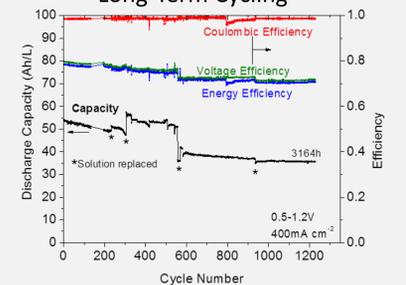


- Coulombic Efficiency**
- Self Discharge
  - Crossover
  - Thickness, equivalent weight
  - Pretreatment
  - Assembled wet/dry
- Voltaic Efficiency**
- Hydrogen Pressure
  - Optimization of (-) and (+) electrodes

## Durability Testing

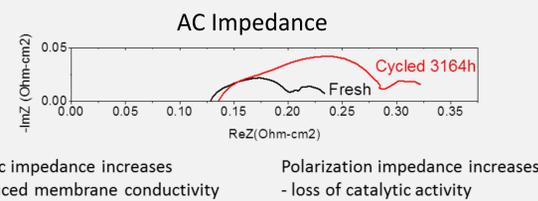
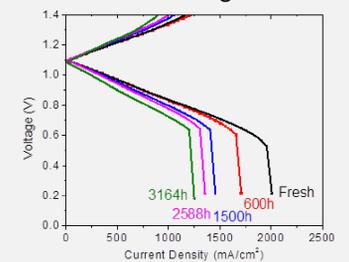


Long-Term Cycling



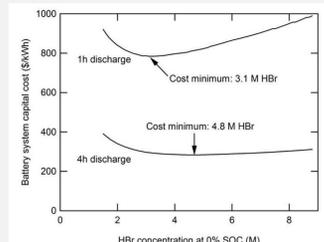
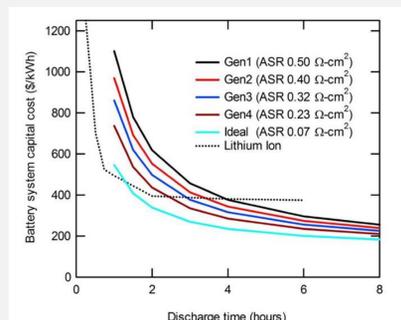
- Slow loss of capacity
- Lower utilization due to voltaic losses
  - Br<sub>2</sub> escape via leaks (minor)

Performance Degradation



- Ohmic impedance increases
- reduced membrane conductivity
- Polarization impedance increases
- loss of catalytic activity

## Cost Model



- Below minimum, tank and pump costs increase
- Above minimum, cell ASR increases